

# Rheology Principles and Applications

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OVERVIEW	<a href="#">ROTATIONAL ASSAYS</a>	<a href="#">OSCILLATORY ASSAYS</a>	<a href="#">VERTICAL ASSAYS</a>	OTHER
<ul style="list-style-type: none"><li>• <a href="#">Applications</a></li><li>• <a href="#">Rheometer Mechanics</a></li><li>• <a href="#">Q3 for IP &amp; Regulatory</a></li></ul>	<ul style="list-style-type: none"><li>• <a href="#">Basic Principles</a></li><li>• <a href="#">Shear Stress Ramp</a></li><li>• <a href="#">Shear Rate Ramp</a></li><li>• <a href="#">Thixotropy</a></li><li>• <a href="#">Time Sweep (stability)</a></li><li>• <a href="#">Temperature Sweep (stability, melting)</a></li><li>• <a href="#">Creep-Recovery</a></li><li>• <a href="#">Tribology (friction)</a></li></ul>	<ul style="list-style-type: none"><li>• <a href="#">Basic Principles</a></li><li>• <a href="#">Amplitude Sweep</a></li><li>• <a href="#">Frequency Sweep</a></li><li>• <a href="#">Time Sweep (stability)</a></li><li>• <a href="#">Temperature Sweep (stability, melting)</a></li></ul>	<ul style="list-style-type: none"><li>• <a href="#">Squeeze-Pull Away (stickiness)</a></li><li>• <a href="#">Model Chewing</a></li><li>• <a href="#">Surface Tension</a></li></ul>	<ul style="list-style-type: none"><li>• <a href="#">General Experimental Considerations</a></li><li>• <a href="#">Plate &amp; Cone Considerations</a></li><li>• <a href="#">Optimizing Dispersion, Colloidal &amp; Emulsion Stability</a></li><li>• <a href="#">Literature Example: Influence of Processing Variables on Rheological &amp; Textural Properties of Lupin Protein-Stabilized Emulsions</a></li><li>• <a href="#">Conclusions</a></li></ul>



01-Sept 2025

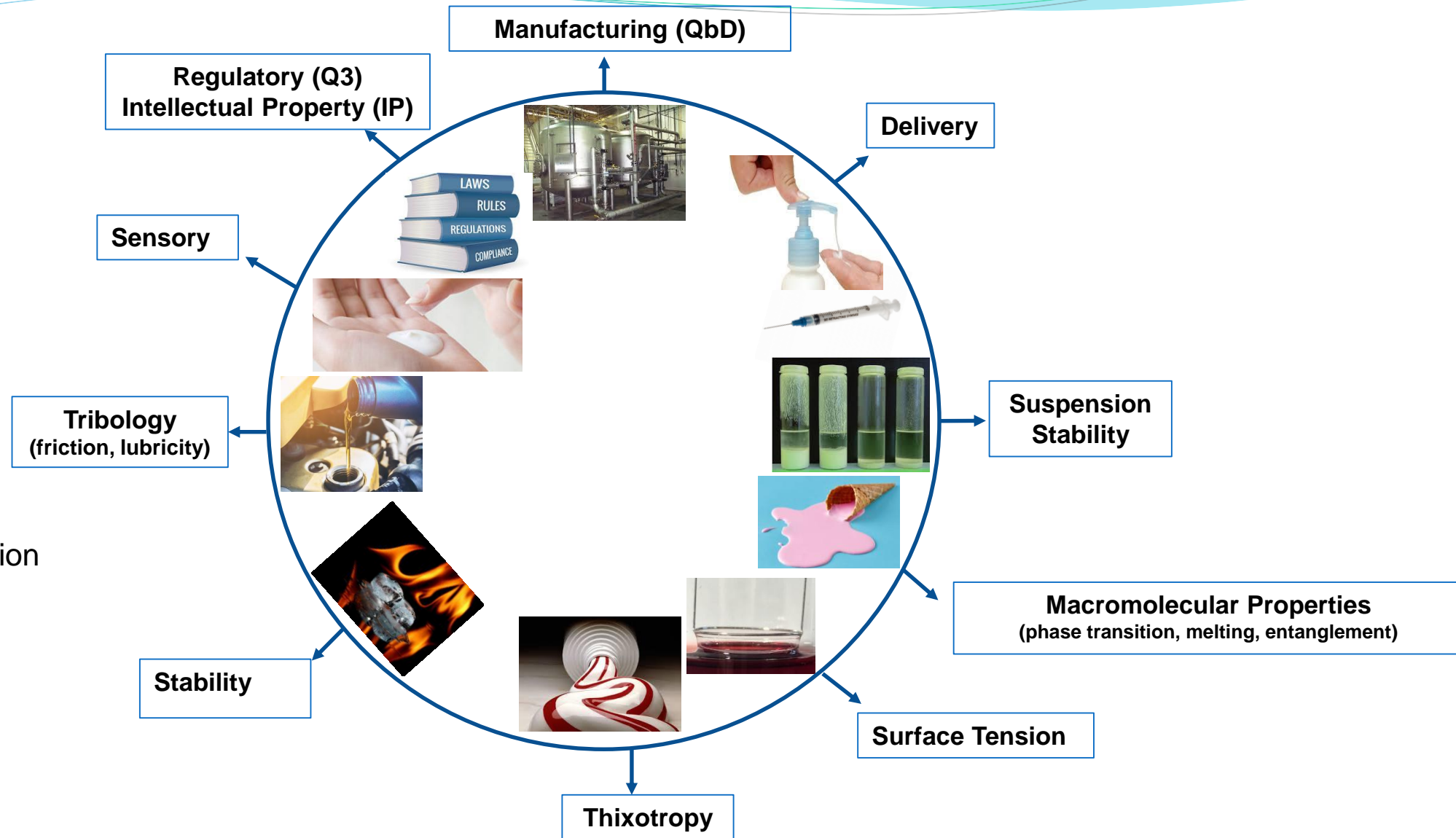
# Rheology Applications - R&D to Manufacturing

## Industries

- Pharmaceutical
- Biopharmaceutical
- Bioengineering
- Food
- Cosmetic
- Plastics
- Many others

## Materials

- Polymer
- Cream
- Emulsion/Suspension
- Gel
- Lotion
- Oil
- Ointment
- Solution
- Many others



# Rheology Applications - R&D to Manufacturing (CON'T)

- **Product development, optimization & in-process control (Quality by Design (QbD))**
  - batch consistency
  - addition order & rate
  - mixing time & speed
  - temperature (heating/cooling range & rate)
  - bulk transfer (shear thinning, rebuilding)
  - equipment type & size (scale-up, pumps, pipes)
  - transport (sedimentation, phase separation)
  - stability



# Regulatory & Intellectual Property (IP)

## Confirm Product (Dis)Similarity to RLD (Reference Listed Drug) for ANDA

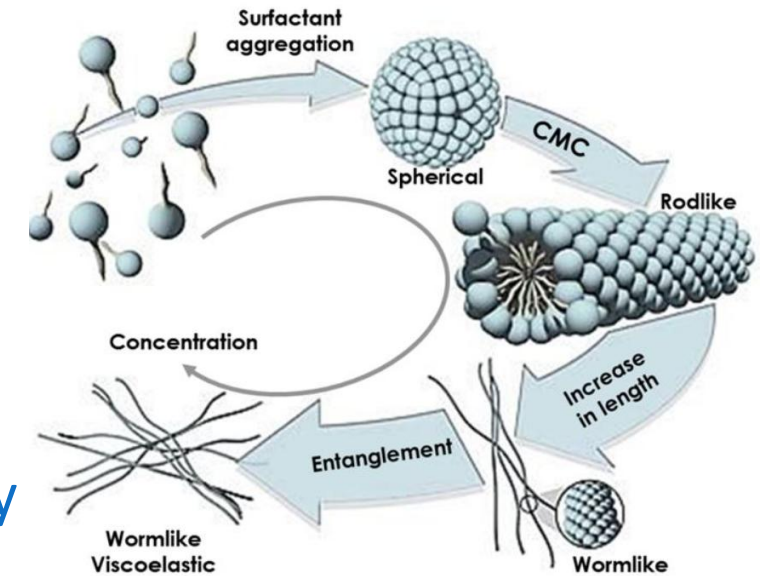
**Q1: Qualitative**  $\Rightarrow$  Same components

**Q2: Quantitative**  $\Rightarrow$  Q1 & same amount

**Q3\*: Microstructure**

$\Rightarrow$  **Q1 + Q2 + same arrangement of matter**

$\Rightarrow$  Performance, efficacy, stability, batch-to-batch consistency



$\rightarrow$  Rheometer may discern among arrangements based on association (entanglements) and their relaxation time

$\rightarrow$  Rheological properties may affect biological activity

- Fulfilling the FDA's Rheology Testing Requirements for Abbreviated New Drug Applications (ANDA) for Topical Creams – Netzsch (<https://analyzing-testing.netzsch.com/en-US/application-literature/fulfilling-the-fdas-rheology-testing-requirements-for-abbreviated-new-drug-applications-anda-for-topical-creams>)

- \* "Draft Guideline on Quality and Equivalence of Topical Products" European Medicines Agency (18Oct2018) (<https://www.ema.europa.eu/en/quality-equivalence-topical-products#current-version-section>)

- \* "Generic Development of Topical Dermatologic Products: Formulation Development, Process Development, and Testing of Topical Dermatological Products" AAPS J. 2013 Jan; 15(1): 41-52 (<https://www.ncbi.nlm.nih.gov/pmc/articles/PMC3535108/>)

- \* "Testing Topicals: Analytical Strategies for the In-Vitro Demonstration of Bioequivalence" Pharm Tech Sept 2018 (<http://www.pharmtech.com/testing-topicals-analytical-strategies-vitro-demonstration-bioequivalence?pageID=1>)



# Rheometer Overview

## Upper Plate

- only moving part contacting sample
- different surfaces
  - smooth
  - rough
  - serrated
- many other attachments

## Lower Plate

- does not move
- same surface options as upper plate
- controls temperature (-5 to 200°C)\*



## Movements → torque

- **Rotational (1 direction)**
- **Oscillational (bi-directional)**
- **Vertical**



\*Options to extend temperature ranges are available.

Images from Netzsch

# By end of presentation.....

- What assay should I use?
- What experimental parameters should I consider?
- Appreciate which is more viscous – honey or mayonnaise? What are these?  $\tau$ ,  $\sigma$ ,  $\gamma$ ,  $\eta$
- Is silly putty viscoelastic solid or liquid? What are these?  $G'$ ,  $G''$ ,  $G^*$ ,  $\delta$ ,  $\eta^*$ ,  $\tan \delta$





## SOME BASIC RHEOLOGY ASSAYS ENTRÉES

*...many side options available*

### ⇒ **ROTATIONAL** → measure flow

- Shear Rate Ramp (shear thinning)
- Shear Stress Ramp (yield stress, start of flow)
- *Thixotropy (rebuilding after shear thinning)*
- *Time Sweep (stability)*
- *Temperature Ramp (stability, phase transitions, melting)*
- *Creep-Recovery (yield stress, rebuilding)*
- Tribology (friction, lubricity)

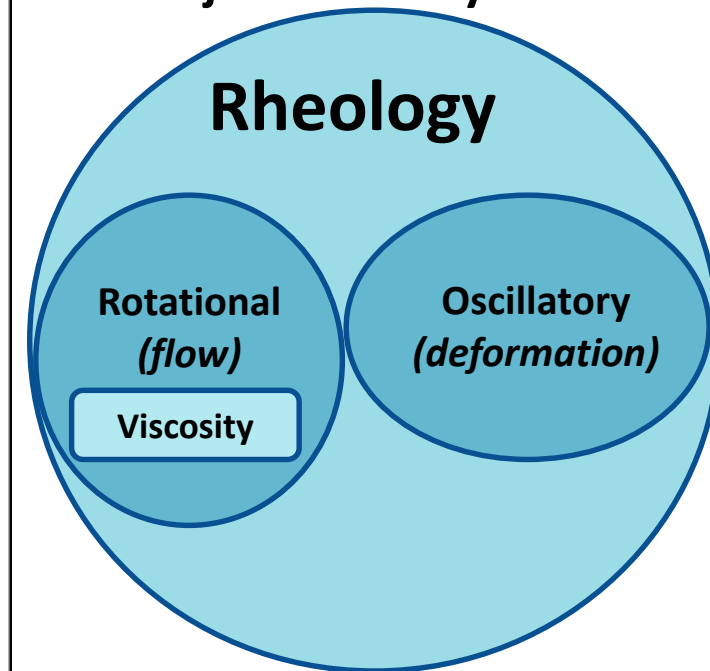
### ⇒ **OSCILLATORY** → measure deformation

- Amplitude Sweep (LVER, stability)
- Frequency Sweep (viscoelasticity)
- *Thixotropy (rebuilding after thinning)*
- *Time Sweep (stability)*
- *Temperature Ramp (stability, phase transitions, melting)*
- *Creep-Recovery (yield stress, rebuilding)*

### ⇒ **VERTICAL**

- Squeeze-Pull Away (stickiness, model chewing)
- Surface Tension

Rheology is much more than just viscosity!



# Viscosity → Resistance to Flow

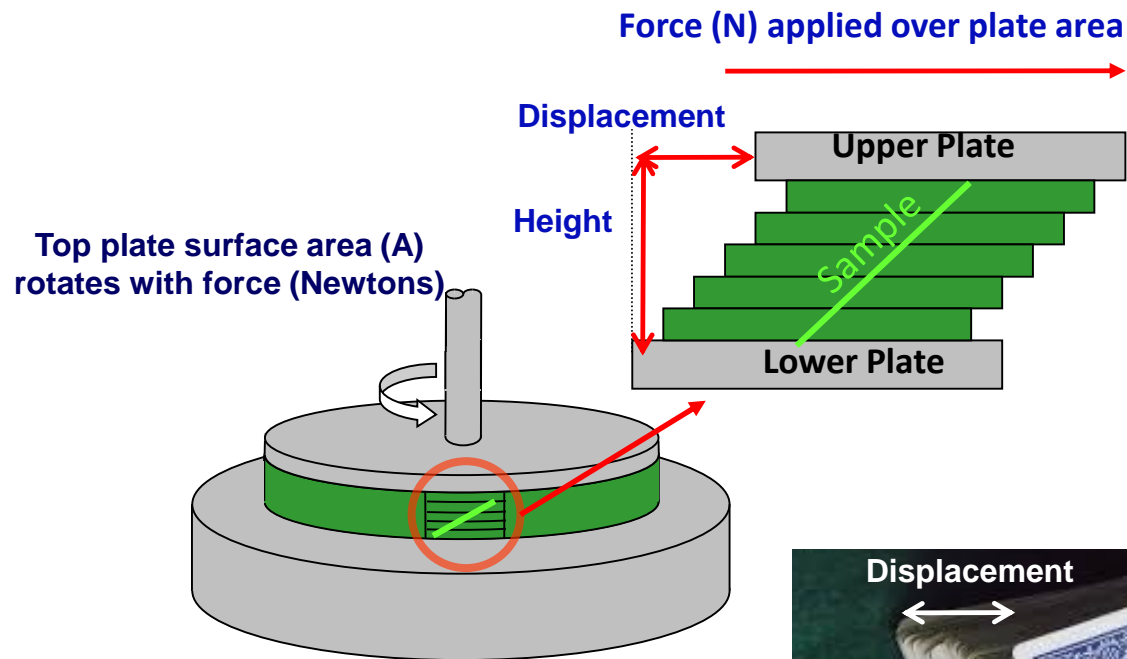


Image from Netzsch

$$\text{Viscosity}(\eta; \text{cP or Pa-sec}) = \frac{\text{Shear Stress}}{\text{Shear Rate}} = \frac{\sigma \text{ (Pa or N/m}^2\text{)}}{\gamma \text{ (sec}^{-1}\text{)}}$$

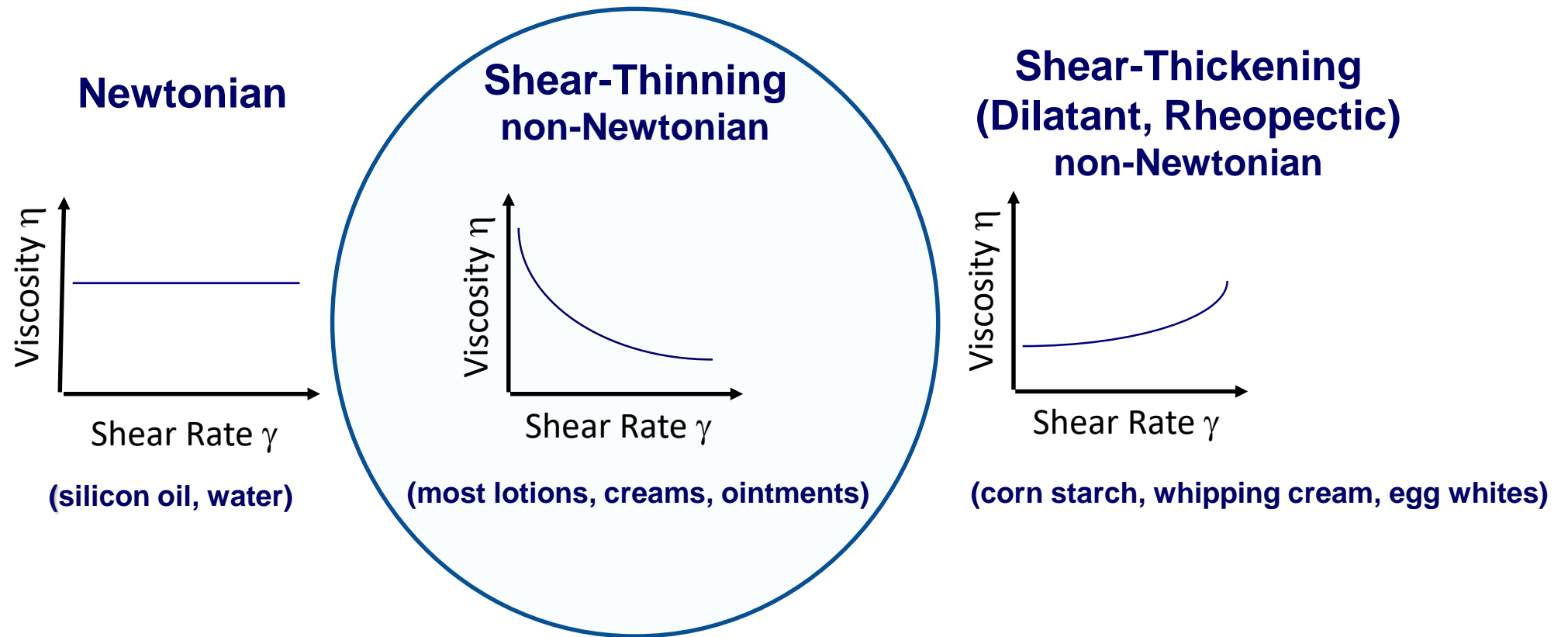
1000cP=1Pa-sec

$$= \frac{\text{Force (N)} / \text{Area (m}^2\text{)}}{\text{Strain (unitless)} / \text{Time (sec)}}$$

$$= \frac{\text{Force (N)} / \text{Area (m}^2\text{)}}{(\text{Displacement (m)} / \text{Height (m)}) / \text{Time (sec)}}$$



# Rotational - Measure flow (*as torque*) with applied force & movement



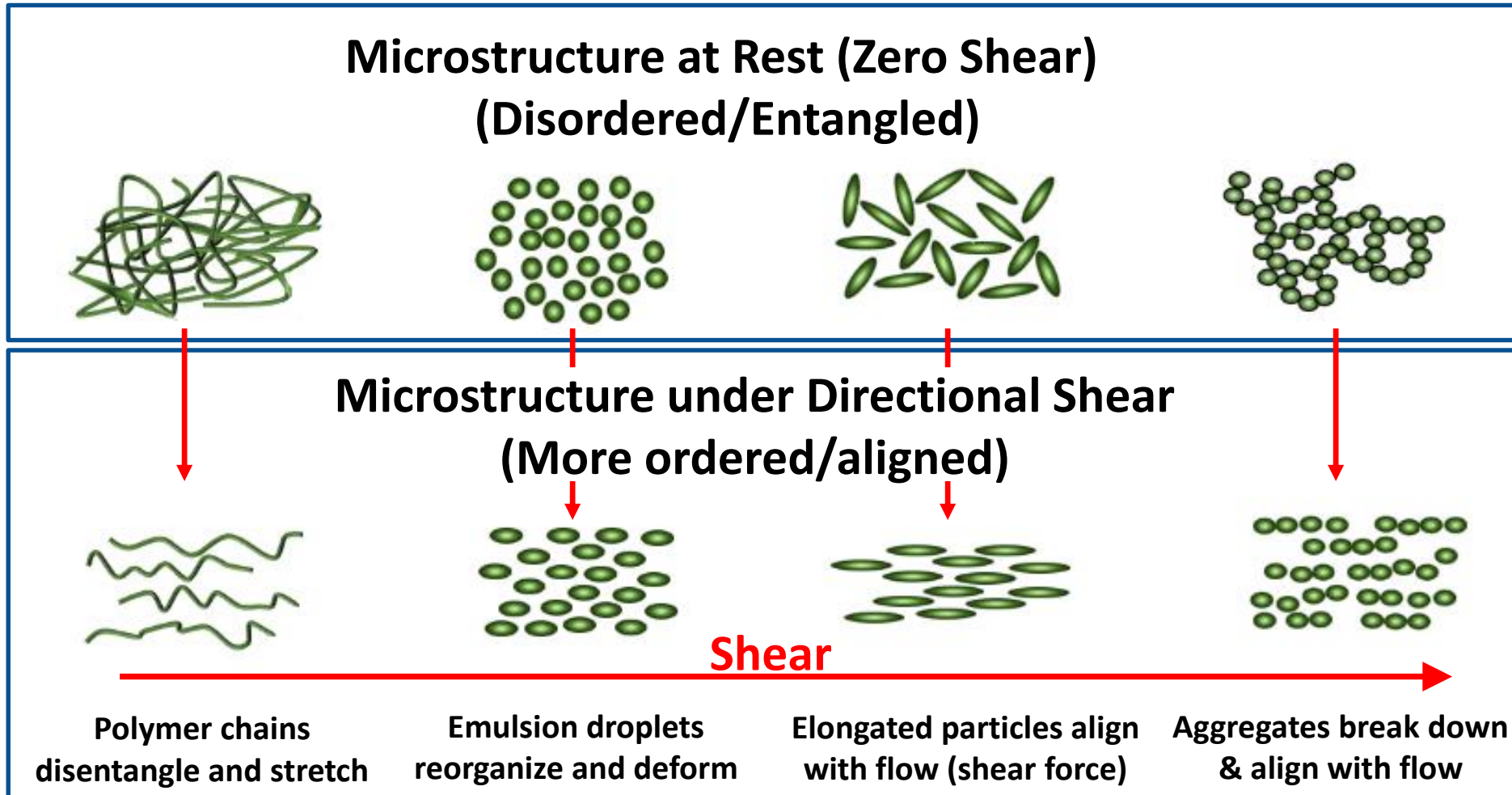
- Most semisolids shear thin (non-Newtonian)
- Helpful to model processes (spreading, pumping, syringability, feel)

Shear rate = strain/time  
(Strain=displacement/height)

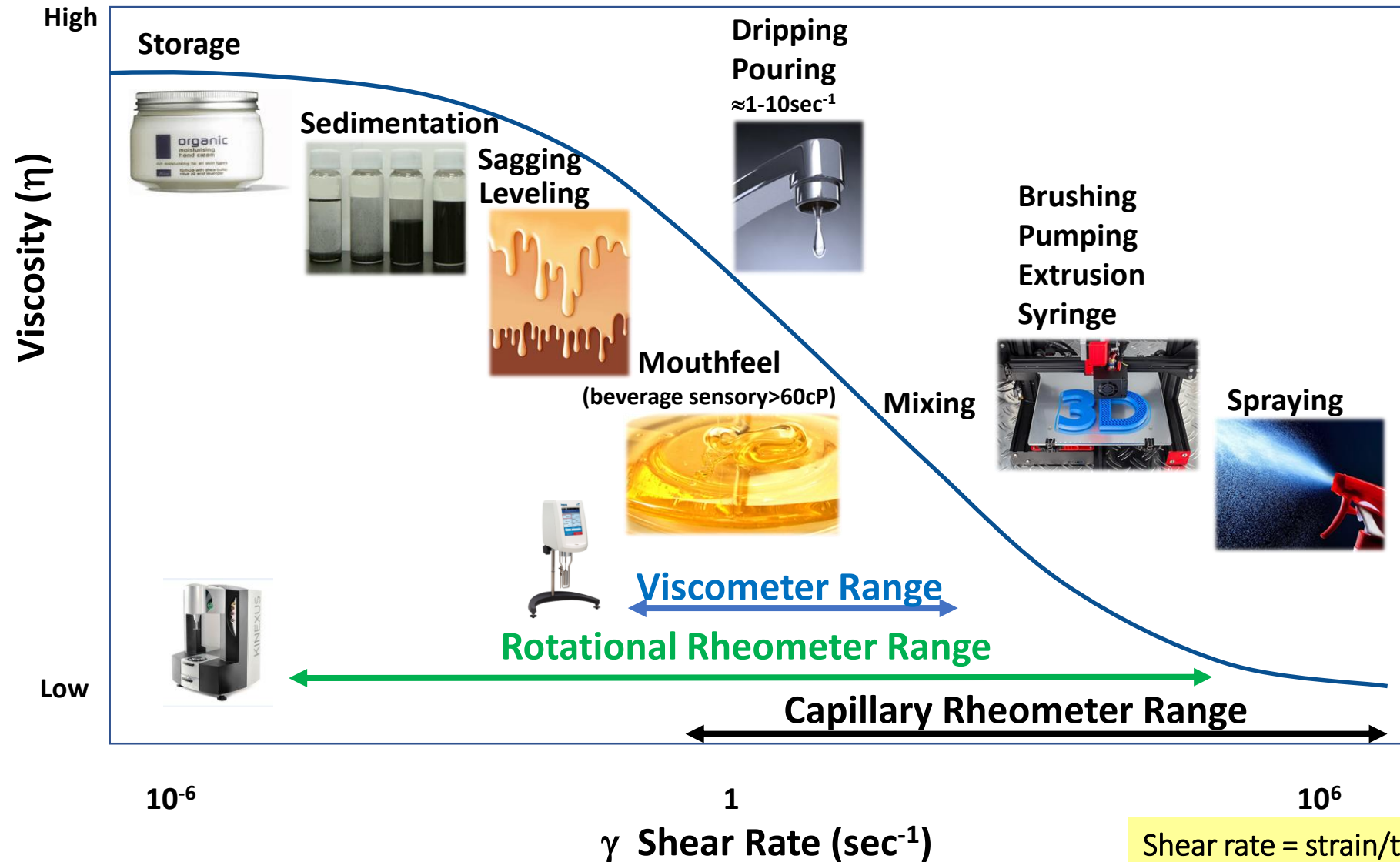


# Effect of Shear on Microstructure.. “go with the flow”

- ⇒ Biologicals, polymers, emulsions
- ⇒ Larger & irregular particles tend to increase viscosity
- ⇒ Mixtures having more polydisperse particles tend to have lower viscosity



# Shear Rate of Processes - range $10^{10}$ (10 billion)



Shear rate = strain/time  
(Strain=displacement/height)

# Shear Rates of Common Processes



→ **SAMPLE STORAGE**  
Very low shear rates:  $\leq 0.001 \text{ s}^{-1}$   
Stability (sedimentation, phase separation)



→ **SAMPLE DELIVERY**  
Medium shear rates:  $\sim 10 \text{ s}^{-1}$   
Pumpability? Scoopability?



→ **SAMPLE APPLICATION**  
Low shear rates:  $\sim 1 \text{ s}^{-1}$   
Too thin? Flows off hand?



→ **SAMPLE APPLICATION**  
Higher shear rates:  $\sim 100 \text{ s}^{-1}$   
Too thick to spread? Nice feel?

# Calculations: Shear Rate Calculations of Common Processes

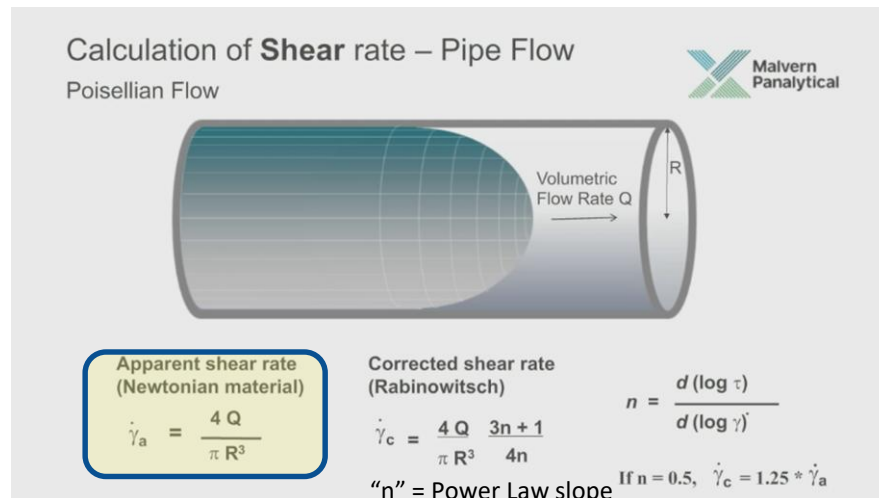
## #1 Painting



$$\begin{aligned}\text{Shear rate } \gamma &= \text{velocity} / \text{height} \\ &= 0.1\text{m/sec} / 0.0002\text{m} \\ &= \mathbf{500\text{sec}^{-1}}\end{aligned}$$

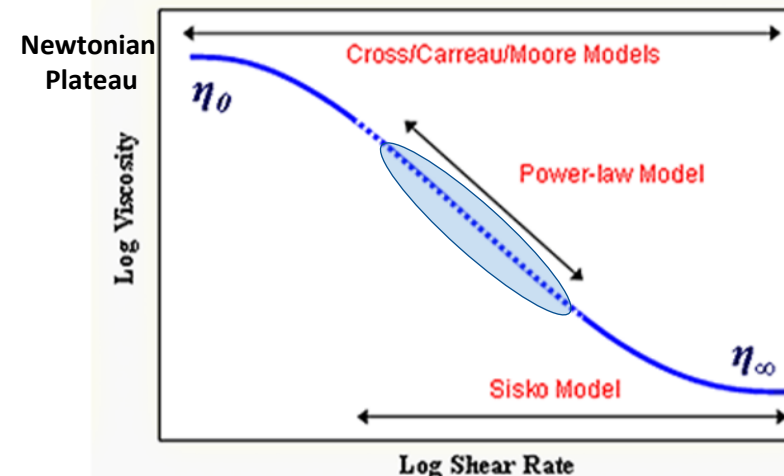
Brush velocity = 0.1 m/sec ( $\approx 4$  in/sec)  
Paint thickness =  $200\mu\text{m} = 0.0002\text{m}$  ( $\approx 0.008\text{in}$ )

## #2 Flow in capillaries, tube, pipe, syringe & needle - Poiseuille's Law



\*water is Newtonian

\*\* toothpaste is non-Newtonian



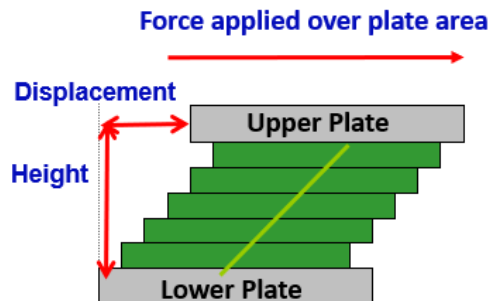
Many more curve fitting models available

# Switching gears $\Rightarrow$ Rotational Methods

## **SHEAR STRESS RAMP ASSAY**

### Analogous to moving revolving door

- **Start Applying Force:** Initially door does not move
  - $\rightarrow$  **Yield Stress:** Force required to start moving door (yield point  $\rightarrow$  flow)
  - $\rightarrow$  **Yield Viscosity:** Viscosity at yield point
- **Note:** *Very small initial movement (shear rate) at yield point can give very high yield viscosity.*



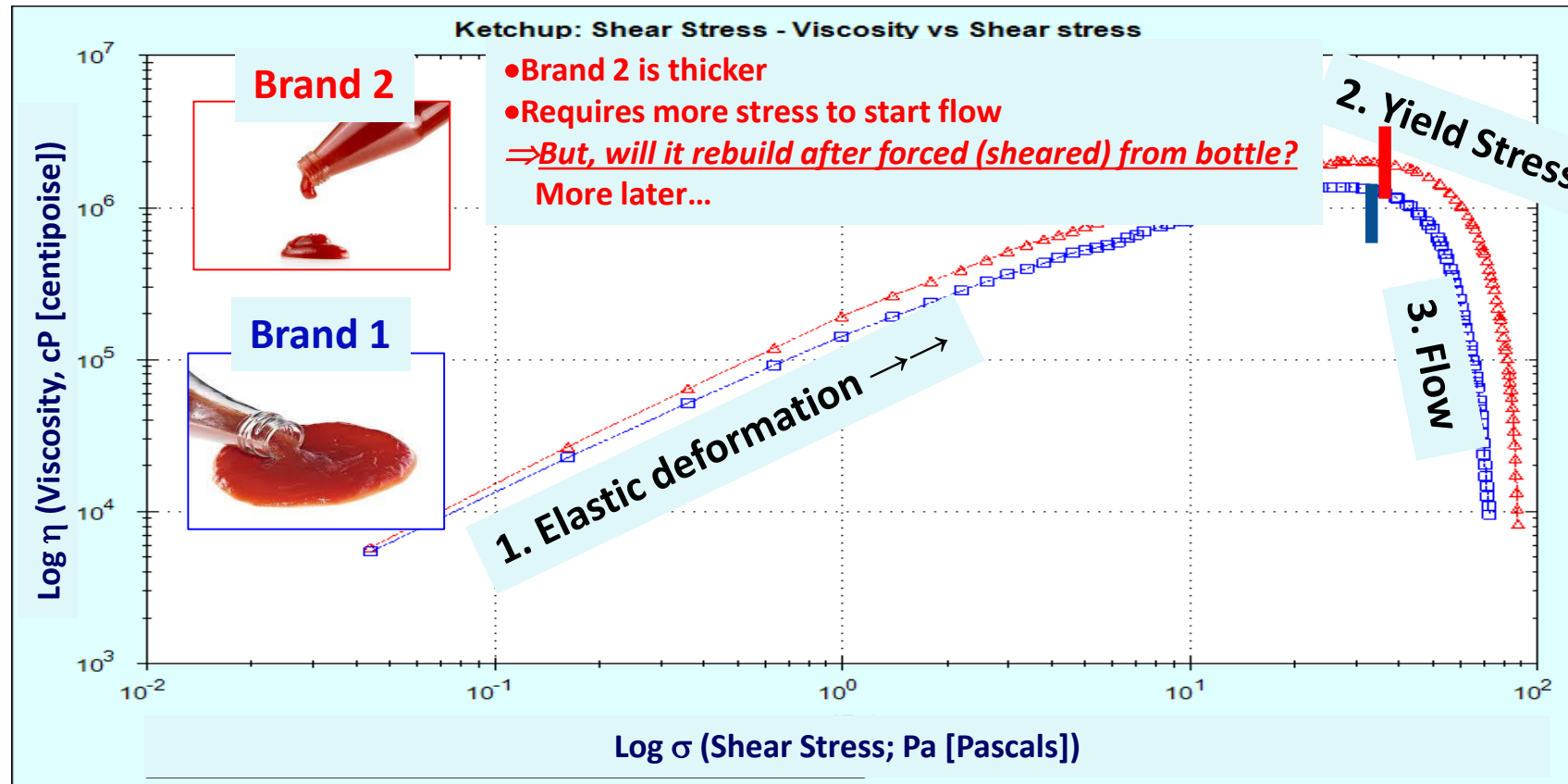
$$\begin{aligned}\text{Viscosity}(\eta) &= \frac{\text{Shear Stress}}{\text{Shear Rate}} = \frac{\sigma}{\gamma} \\ &= \frac{\text{Force/Area}}{(\text{Displacement/Height})/\text{Time}}\end{aligned}$$





# Application: Yield Stress Ramp “Flow Curve” - Ketchup

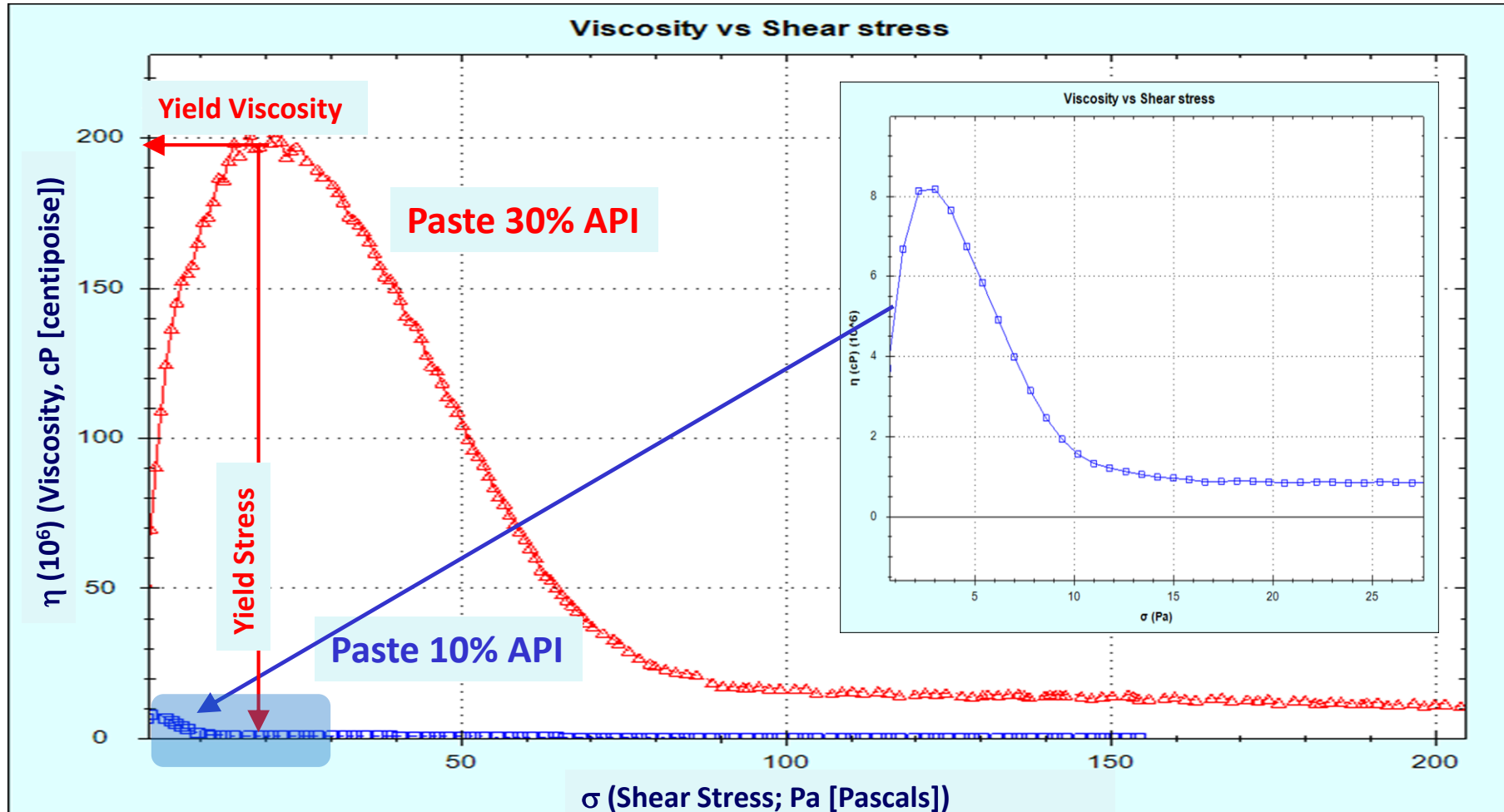
► **Purpose:** Client (engineers) needed data for process modelling



- Helpful model for difficult to pump or stir materials → start up force >> maintain flow force due to shear thinning
- Formulation optimization - type and amount of thickeners, excipients
- Insight for manufacturing optimization – pump capacity, transfer pipe dimensions, temperature
- Refine customer experience – thicker, creamier
- Model if sample is likely to settle. Stokes Law → is downward force on particles > media yield stress?

# Application: Yield Stress Ramp - Pharmaceutical Paste

- **Purpose:** Client needed to quantify impact of % API on processing & application
- **Result:** 30% API paste has much higher yield stress & yield viscosity → difficult to initiate movement

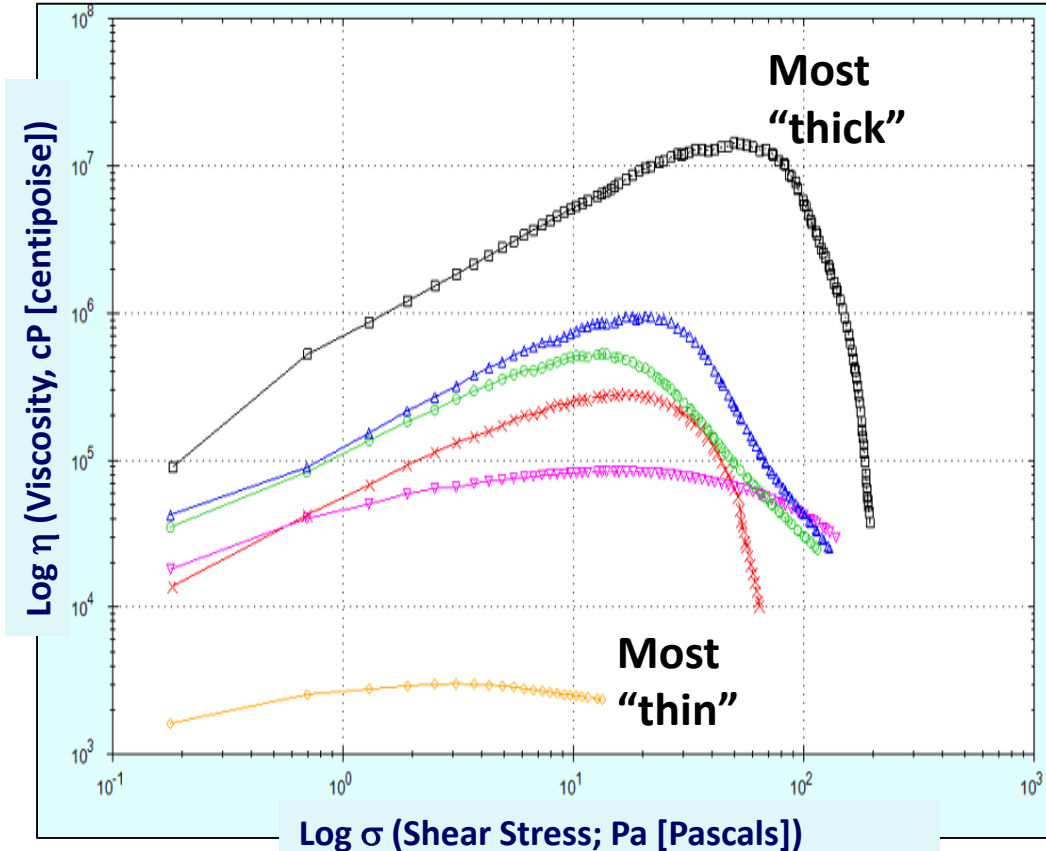


Stress = Force/Area

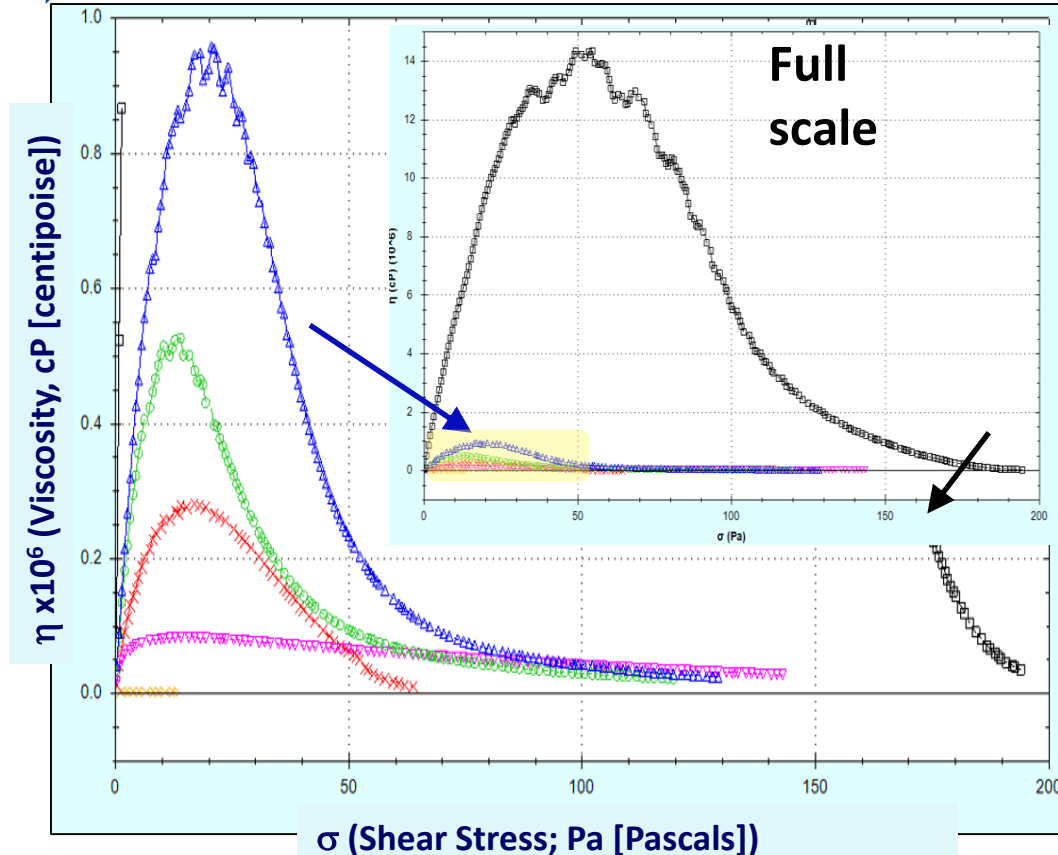
# Application: Yield Stress Ramp - Arthritis products

- **Purpose:** Client requested side-by-side rheological profiles for 6 products
- **Results:** Orders of magnitude difference!
  - **Experimental:** 25mm rough parallel plate, 200um gap (100uL sample), 0 to 300Pa over 300sec
  - **Note:** Yield response is rate dependent. Values vary with experimental parameters. *Example: Pull rubber band slow vs fast.*

## Log-Log Plot



## Linear-Linear Plot



# Application: Using Yield Stress to Screen Sedimentation

Downward stress from gravity on a spherical particle in dilute suspension is estimated by Stokes' Law

$$\sigma_s = r * g * \frac{d - \rho}{3}$$

Stress  
Particle radius  
Gravitational acceleration  
Particle density  
Fluid density

$$V_s = 2 r^2 * g * \frac{(d - \rho)}{9 \eta_0}$$

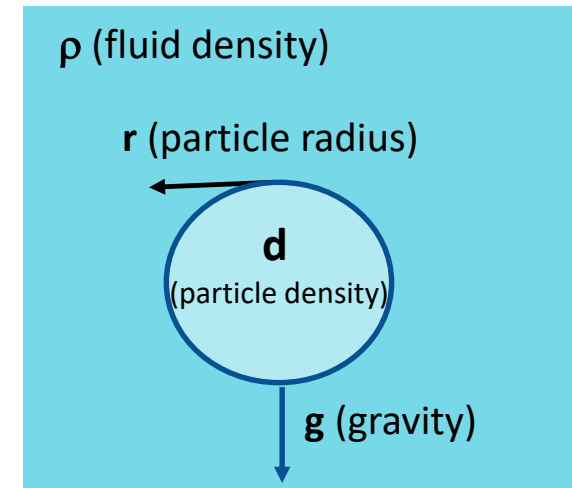
Sedimentation velocity  
Zero shear viscosity



Vodka with suspended gold flakes  
(non-Newtonian)

- If sample yield stress  $> \sigma_s$ , then sedimentation less likely assuming suspending media doesn't shear thin during transport and handling.
- Can also determine with amplitude sweep (cohesion energy density).

Ref: [azom.com/article.aspx?ArticleID=2885](http://azom.com/article.aspx?ArticleID=2885)



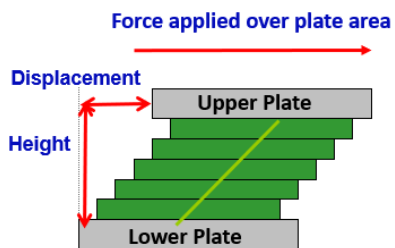


# Switching gears $\Rightarrow$ Rotational methods

## SHEAR RATE RAMP ASSAY

- Continuous ramp (most requested)
- Stepwise ramp

$$\begin{aligned}\text{Viscosity}(\eta) &= \frac{\text{Shear Stress}}{\text{Shear Rate}} = \frac{\sigma}{\gamma} \\ &= \frac{\text{Force/Area}}{\text{Strain/Time}} \\ &= \frac{\text{Force/Area}}{(\text{Displacement/Height})/\text{Time}}\end{aligned}$$





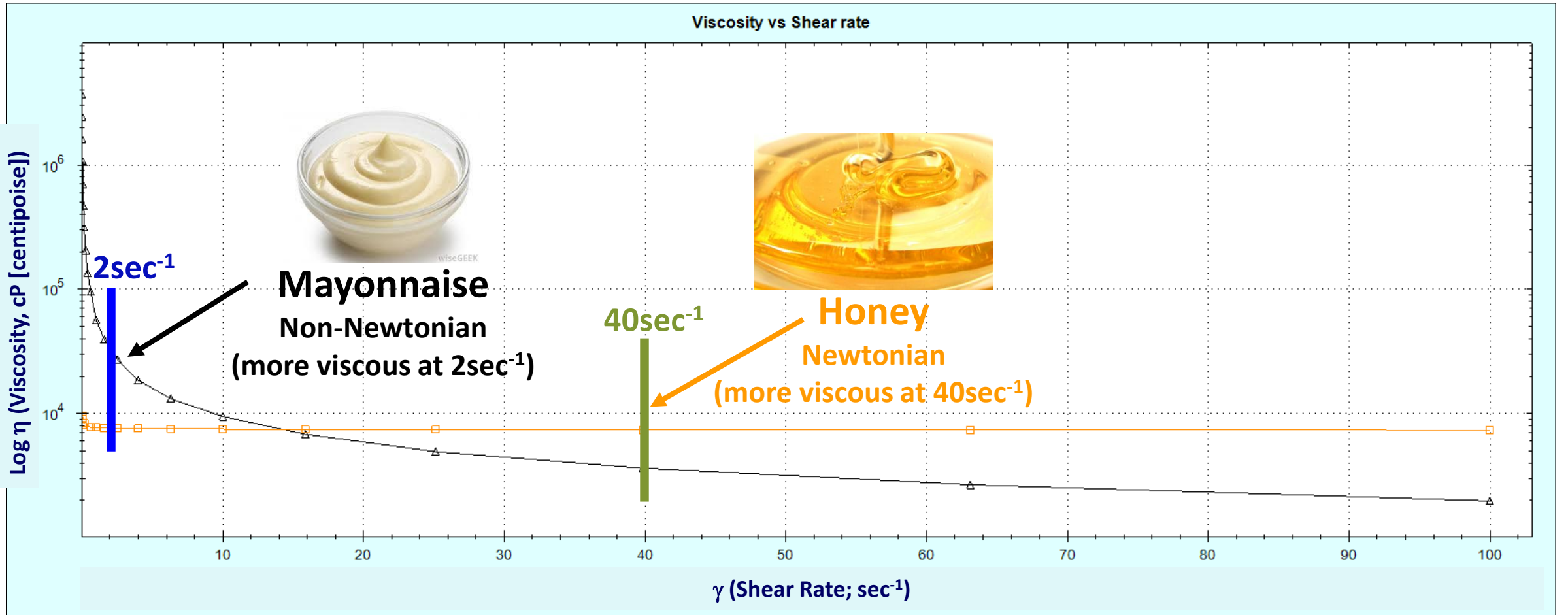
# Shear Rate Ramp (Continuous)

Which is more viscous – honey or mayonnaise?

Depends on shear rate..... CRITICAL CONSIDERATION WHEN COMPARING VISCOSITIES

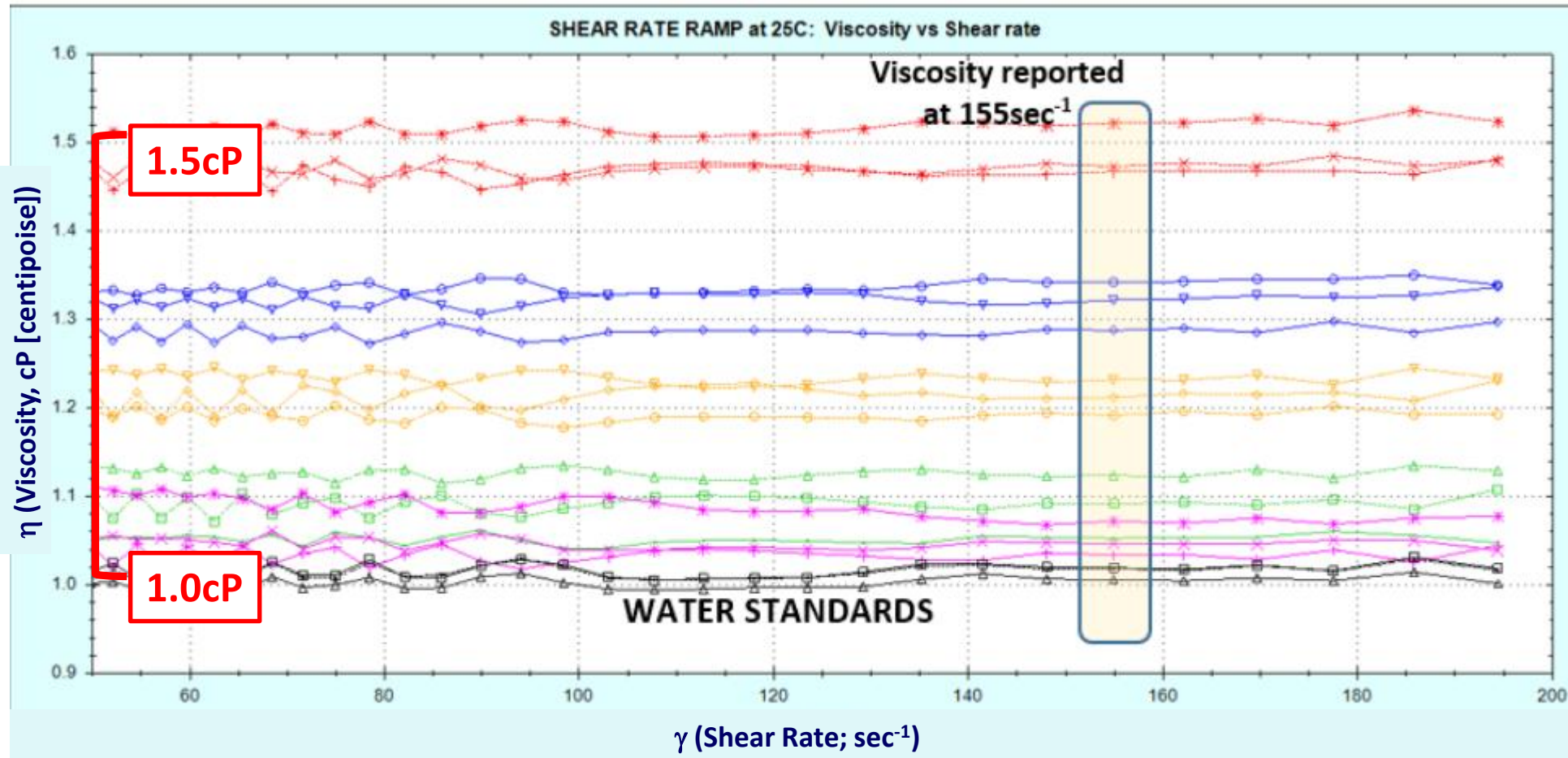
→ At  $2\text{sec}^{-1}$   $\eta_{\text{Mayonnaise}} > \eta_{\text{Honey}}$

→ At  $40\text{sec}^{-1}$   $\eta_{\text{Honey}} > \eta_{\text{Mayonnaise}}$



# Shear Rate Ramp (Continuous) – Low Viscosity Samples → Sensitivity

- **Purpose:** Client needed to compare viscosity for 5 aqueous formulations vs water
- **Result:** Resolved water stds & 5 very low viscosity samples within 0.5cP range with good reproducibility
  - Experimental: 40mm smooth upper parallel plate, 300uL gap (380uL sample) at 25°C over 50-200sec<sup>-1</sup>



Sample 1 (RSD 1.6%)

Sample 2 (RSD 2.3%)

Sample 3 (RSD 1.4%)

Sample 4 (RSD 2.7%)

Sample 5 (RSD 1.5%)

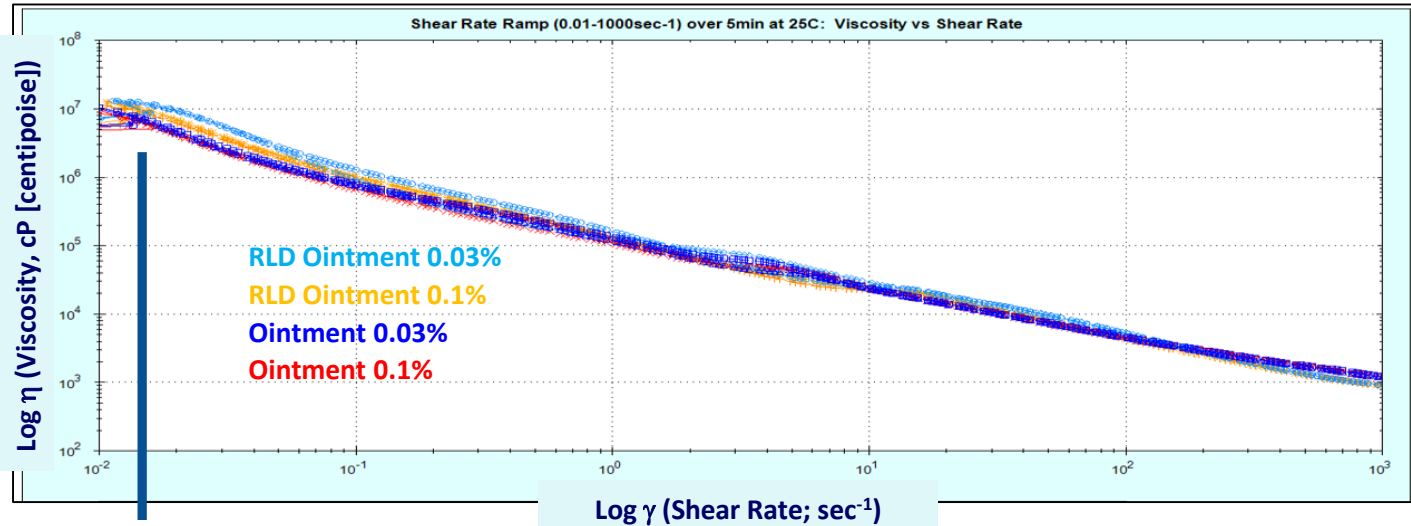
Water Std (RSD 1.1%)

# Shear Rate Ramp (Continuous) – 2 RLD vs 2 Generic Ointments

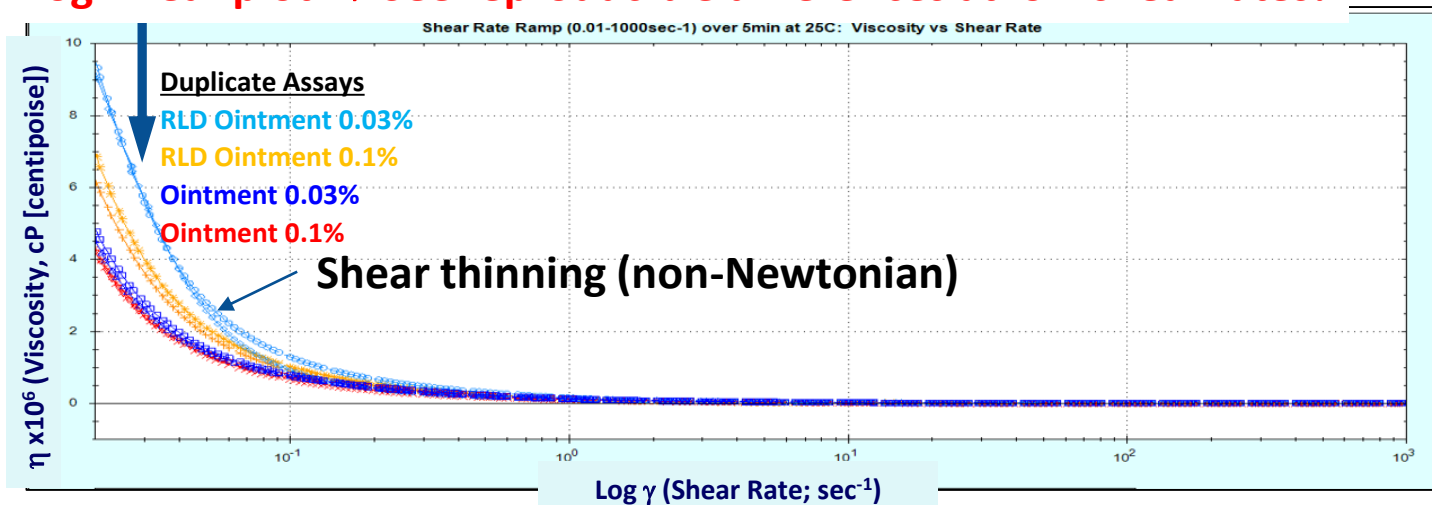
**Experimental:** Shear rate ramp ( $0.01\text{-}1000\text{sec}^{-1}$ ) over 5min at  $25^{\circ}\text{C}$ , 25mm rough upper plate

**Conclusion:**  $0.03\% > 0.01\%$  for both RLD and Generic ointments with good reproducibility ( $n=2$ )

**log-log plot → Samples look reasonably similar**



**log-linear plot → See reproducible differences at low shear rates!**



(RLD = Reference Listed Drug)

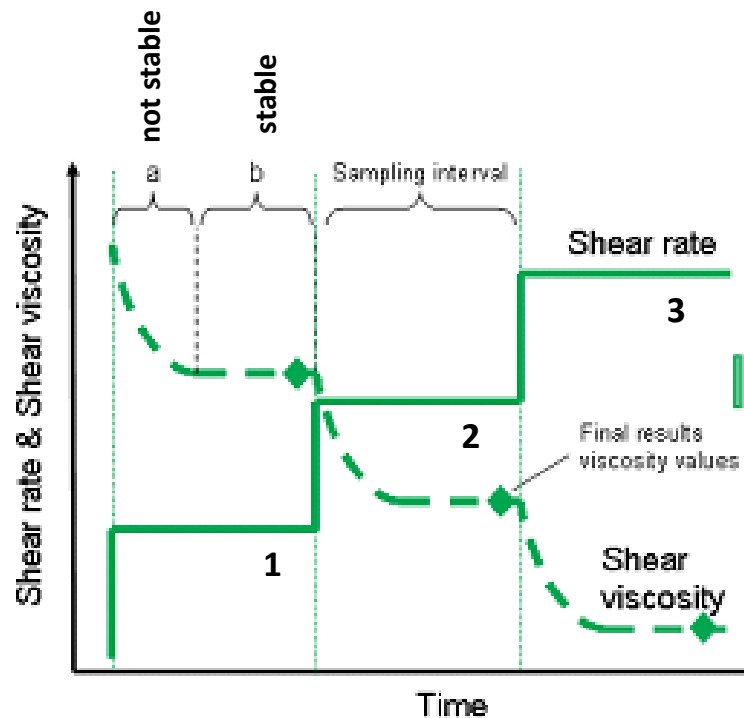
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# Viscosity – Stepwise Shear Rate Ramp

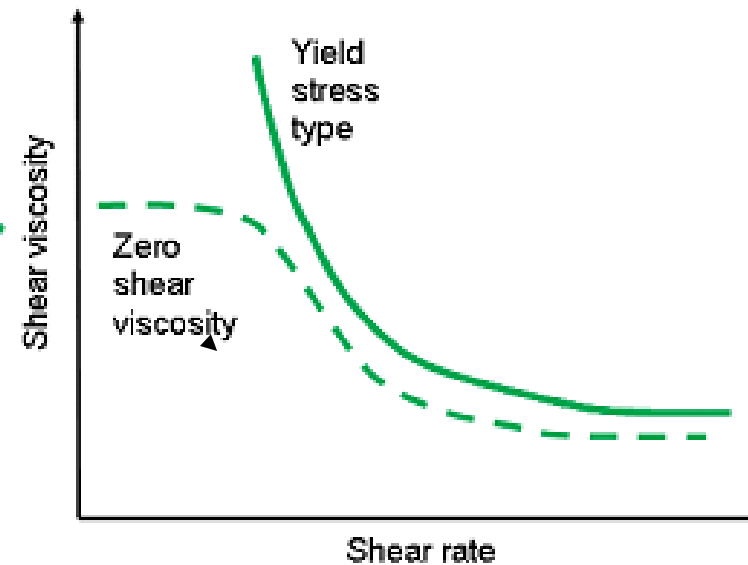
- Incrementally step shear rates up/down.
- Can define viscosity stabilization criteria (i.e. 5% change/5sec) or timeout (i.e. 30sec) before next step.
- Helpful to model manufacturing processes, quantify post-shear thinning (ir)reversibility (hysteresis).

## APPLIED MOVEMENTS

(for 3 increments)



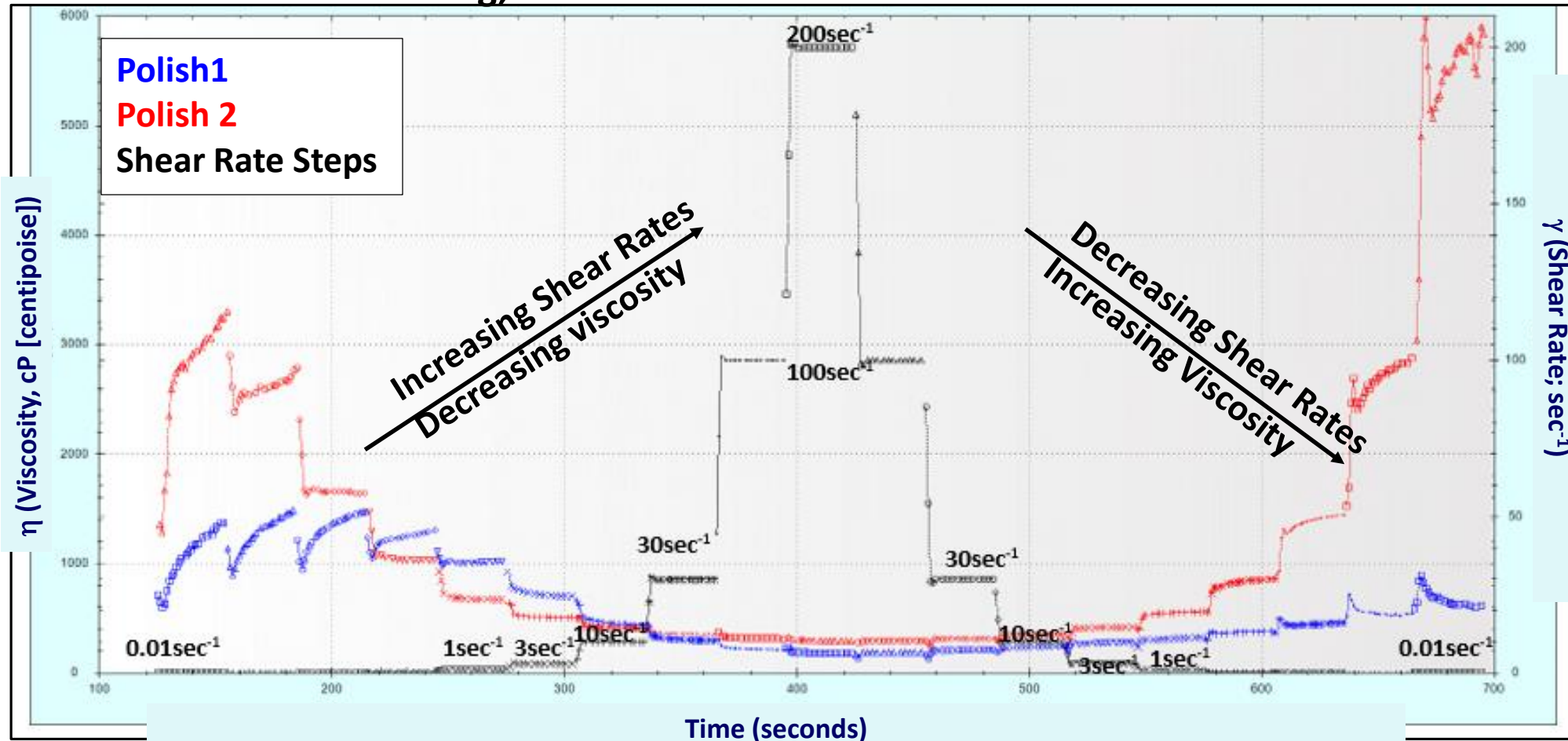
## OUTPUT PLOT



# Stepwise Shear Rate with Increasing/Decreasing Ramps for 2 Polishes

- Experimental: 25mm rough plate, 300um gap (150uL),  $0.01 \rightarrow 200 \rightarrow 0.01 \text{sec}^{-1}$
- 30 seconds hold at each step (10 steps up / 9 steps down)

**Results:** -Samples thinned with increasing shear rate, then differed extent of rebuilding with decreasing shear.  
-After shear thinning, Polish 1 *under-rebuilt* 0.53-fold & Polish 2 *over-rebuilt* 1.86-fold vs initial.

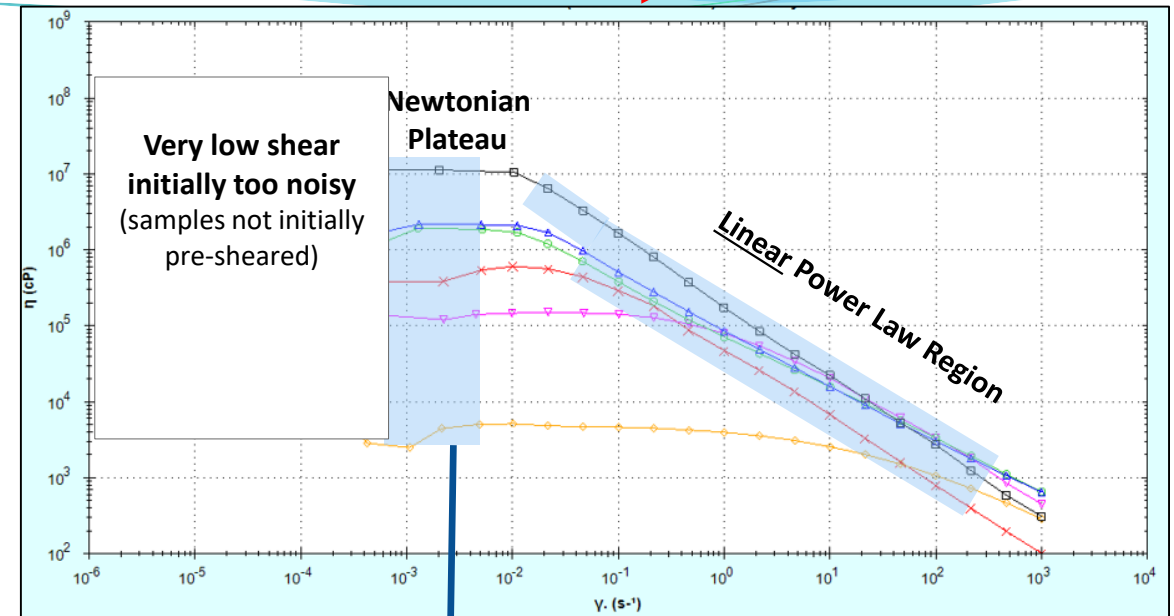




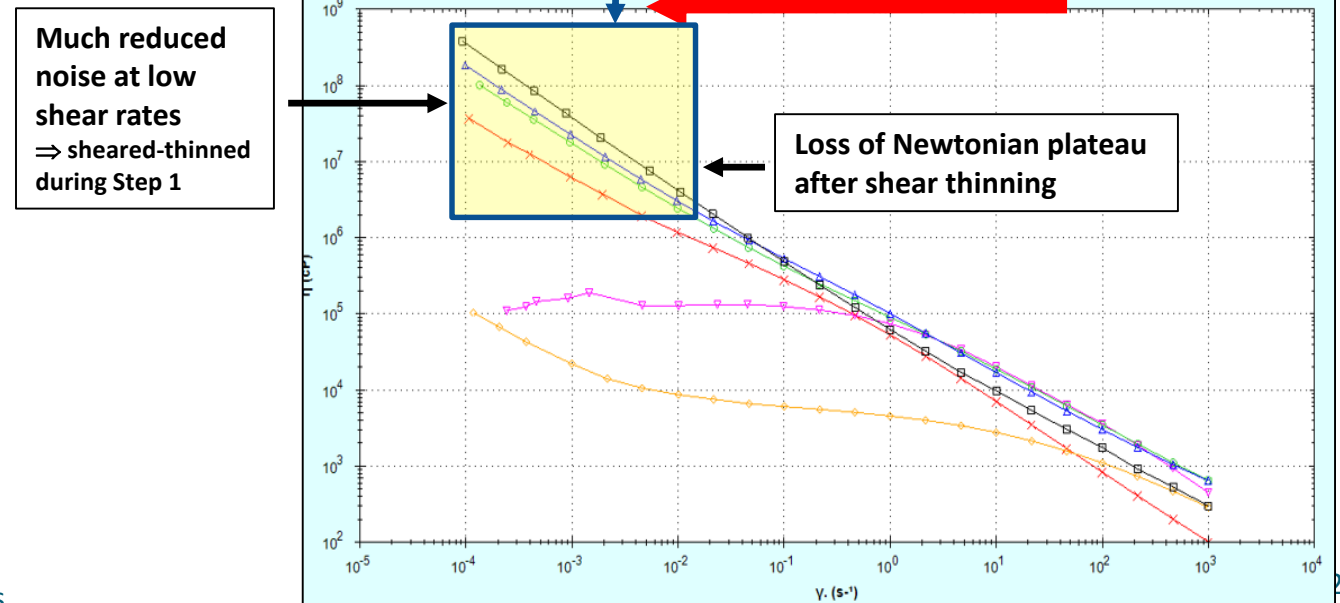
# Application: Stepwise Shear Rate for Arthritis Products

- Move to next step after stability criteria met (5%)
- **Purpose:** Client requested side-by-side comparison.
- **Results**
  - Very different among samples.
  - Increasing vs decreasing shear rate results different showing loss of Newtonian plateau
- **Experimental:** 25mm rough plate, 200um gap (100uL), 0.0001-1000sec<sup>-1</sup>

## STEP 1 - Increasing Shear Rate



## STEP 2 - Decreasing Shear Rate



# Application: Stepwise Shear Rate - Rank order macromolecule MW $\propto$ “zero” shear rate

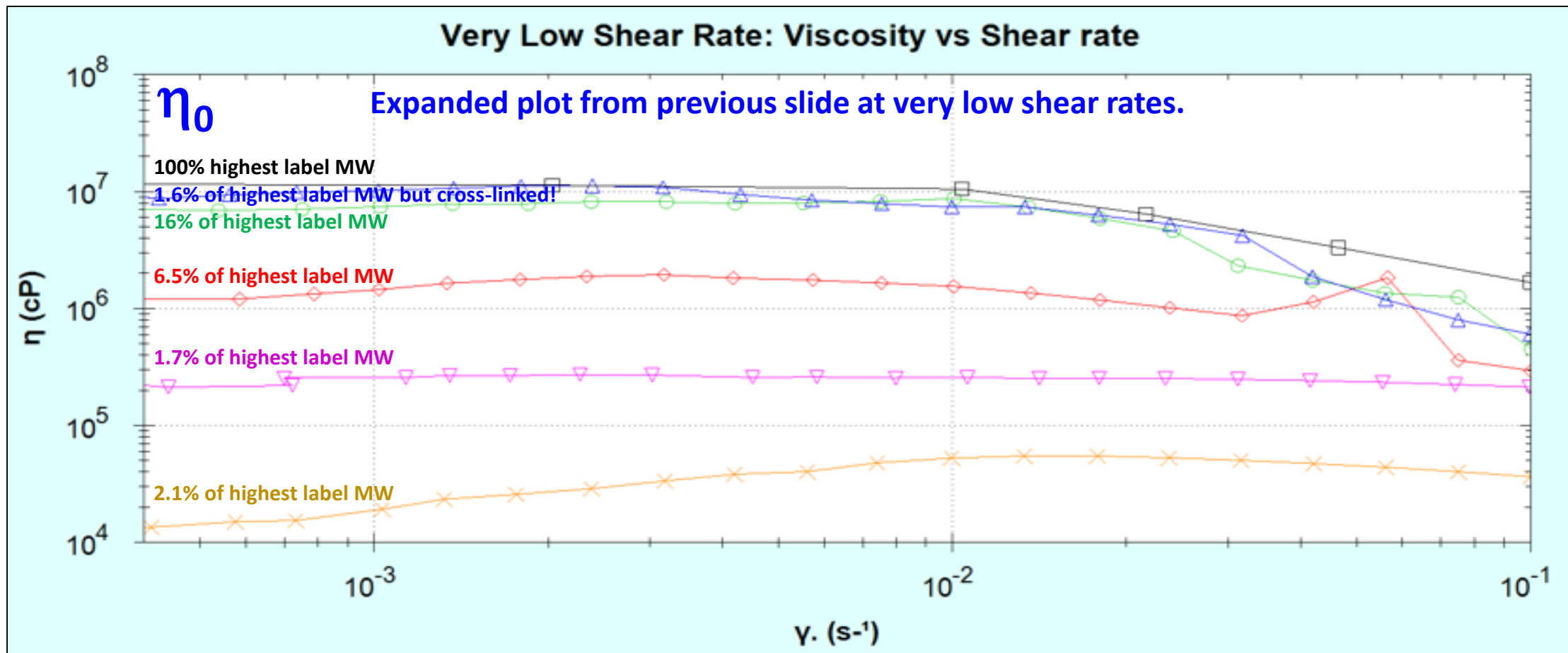
► **Purpose:** Client requested side-by-side rheological profile for several products.

► **Results:** Viscosity at Newtonian Plateau correlate with molecular weight (MW).

→ **General Rule of Thumb:** Polymer having same  $\eta_0$  with broad MW distribution (less ordered) starts shear thinning at lower shear vs narrow MWD (more ordered).

→ **General Rule of Thumb:** Correlation with  $\eta^*$  (complex viscosity) can also determined with low frequency (oscillatory) assay.

$G'$  &  $G''$  shift to  $\downarrow$ freq with  $\uparrow$ MW.  $\uparrow G'G''$  crossover frequency  $\rightarrow \downarrow$  MW.  $\uparrow G'G''$  crossover modulus  $\rightarrow$  more narrow MWD....*MORE LATER.*



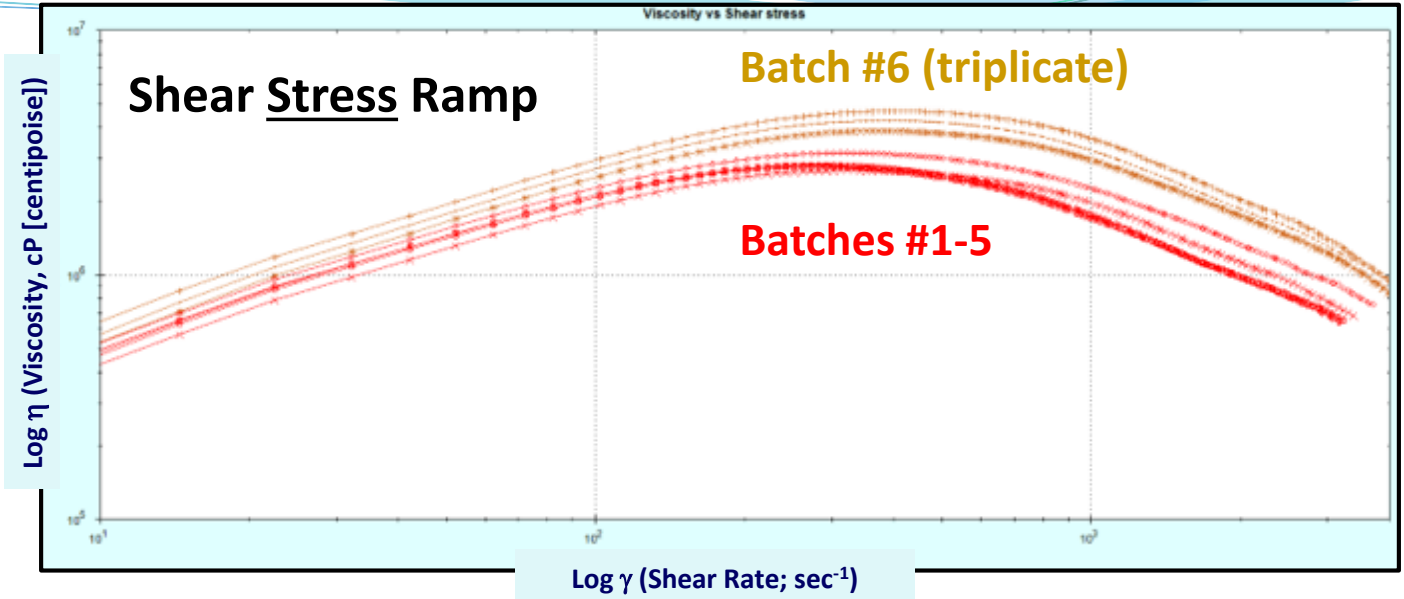
# Application: Batch (In)Consistency using Shear Stress & Shear Rate Ramp Assays

**Conclusion:** Both shear stress ramp & shear rate ramp assays confirm Batch #6 differs.

## SHEAR STRESS RAMP

**Batches #1-5 → Similar**

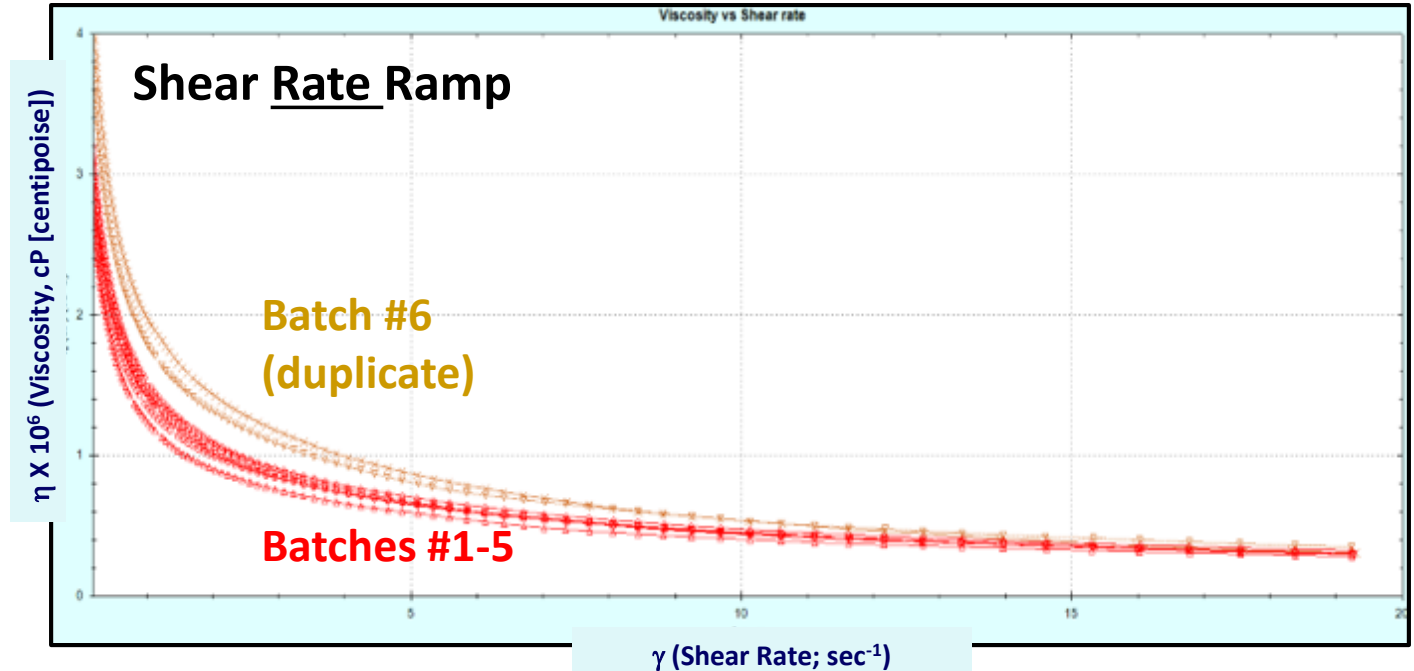
**Batch #6 (triplicate) → Higher yield stress & yield viscosity → more stiff**



## SHEAR RATE RAMP

**Batches #1-5 → Similar**

**Batch #6 (duplicate) → Higher viscosity at low shear rate (1-10sec<sup>-1</sup>)**

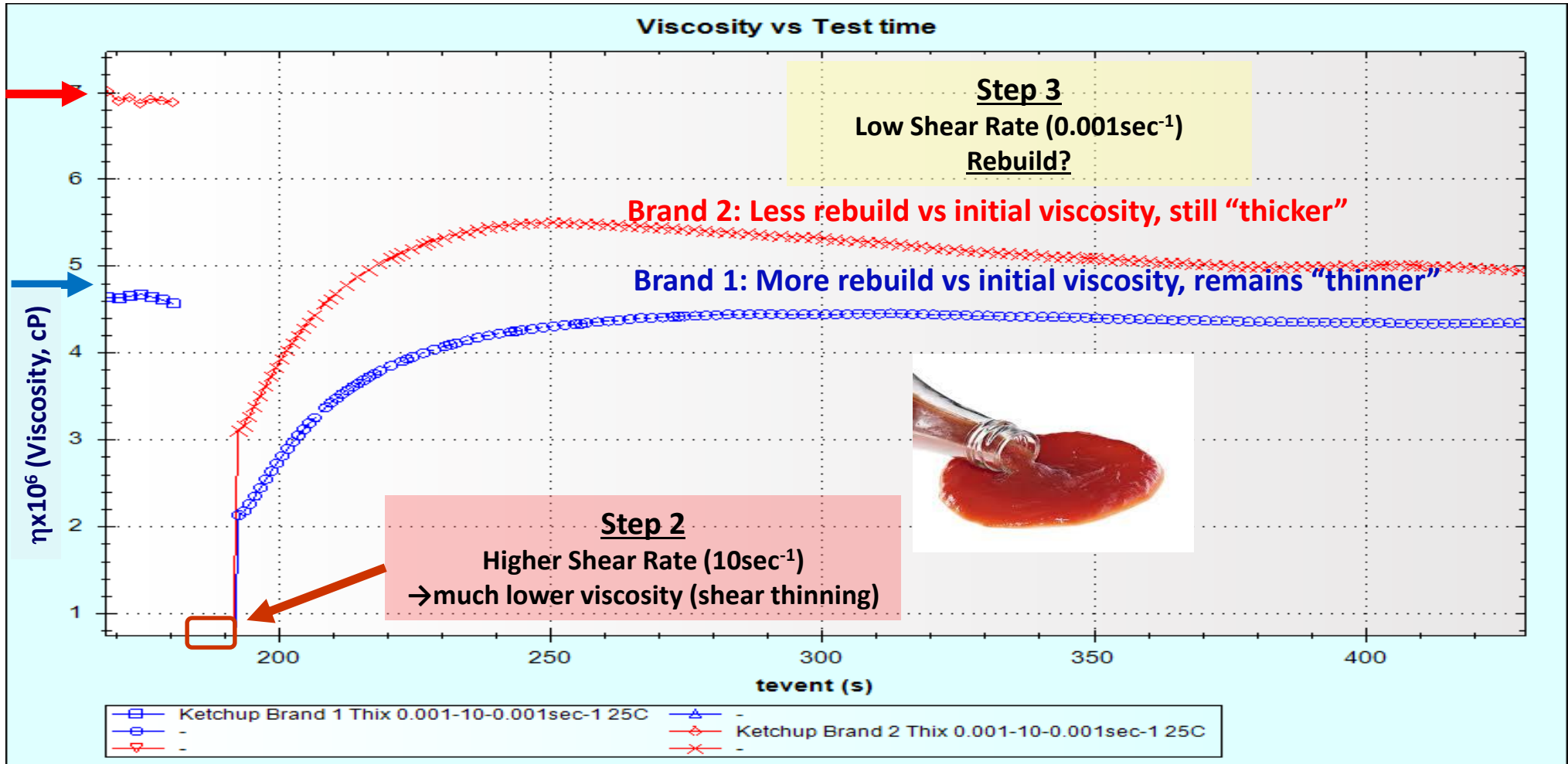


# Application: Thixotropy (3-Step) – Ketchup...again

► **Purpose:** Client (engineers) requested ketchup data for process modelling.

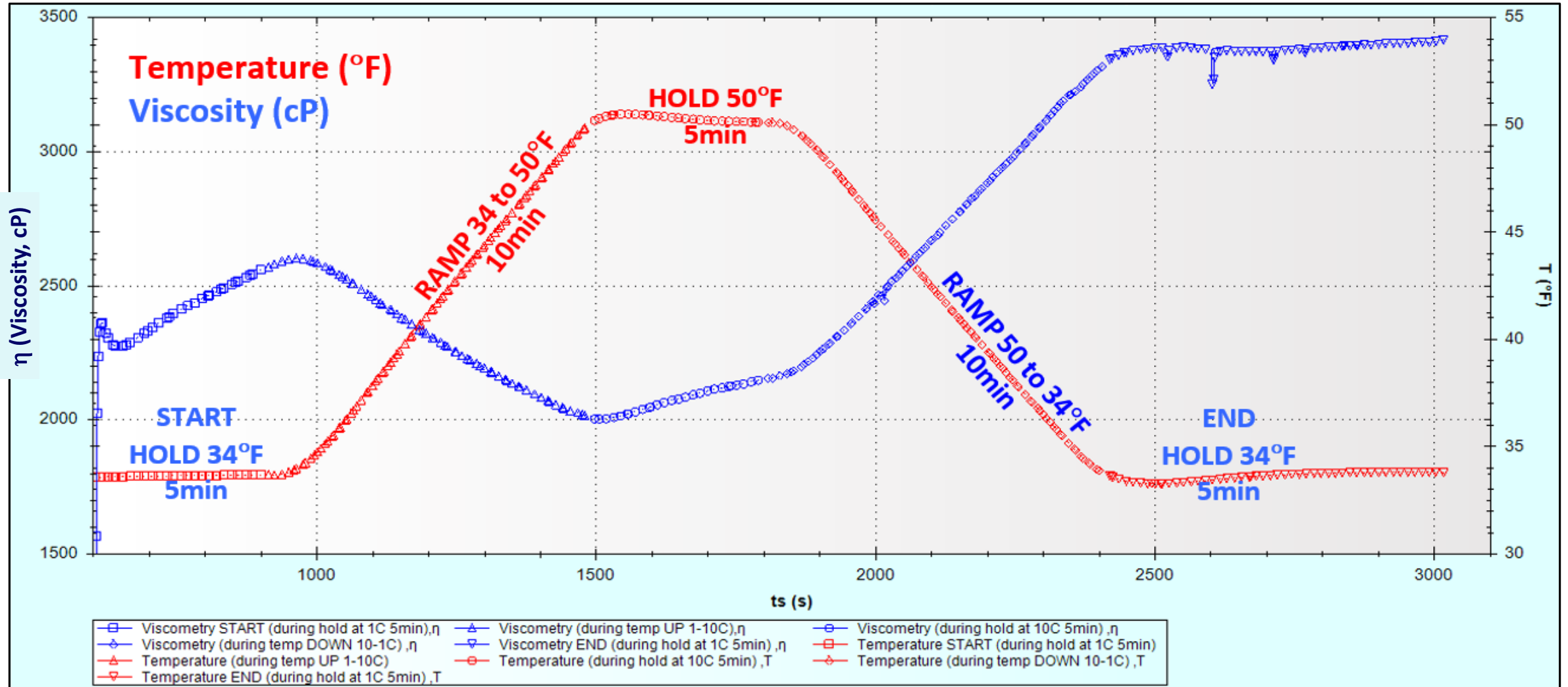
Determine rebuild extent and rate after exposure to higher shear (i.e. shear thinning).

→→**CAREFUL!** Assay parameters, esp Step 2 depend on question seeking to answer.....



# Application: Temperature Cycling with Single Shear RATE - Food

- Investigate irreversibility of food product **viscosity** with **temperature** cycles  $34 \rightarrow 50 \rightarrow 34^\circ\text{F}$
- Used solvent trap to increase humidity in assay chamber to reduce moisture loss
- Sample assayed at low shear rate of  $0.1\text{sec}^{-1}$

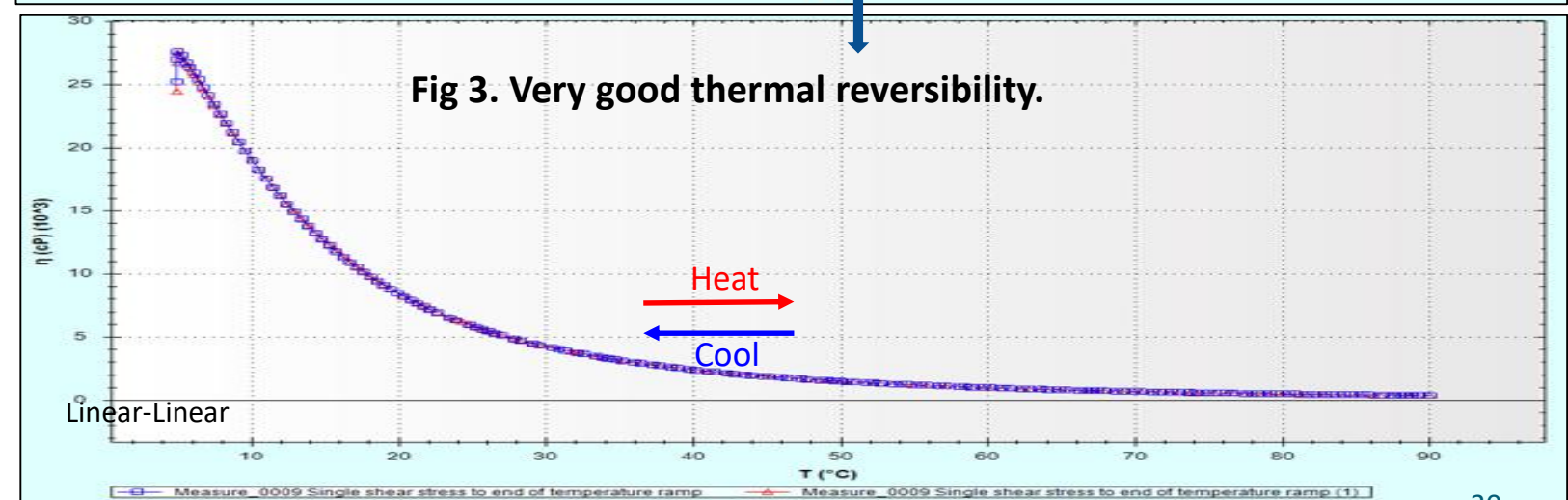
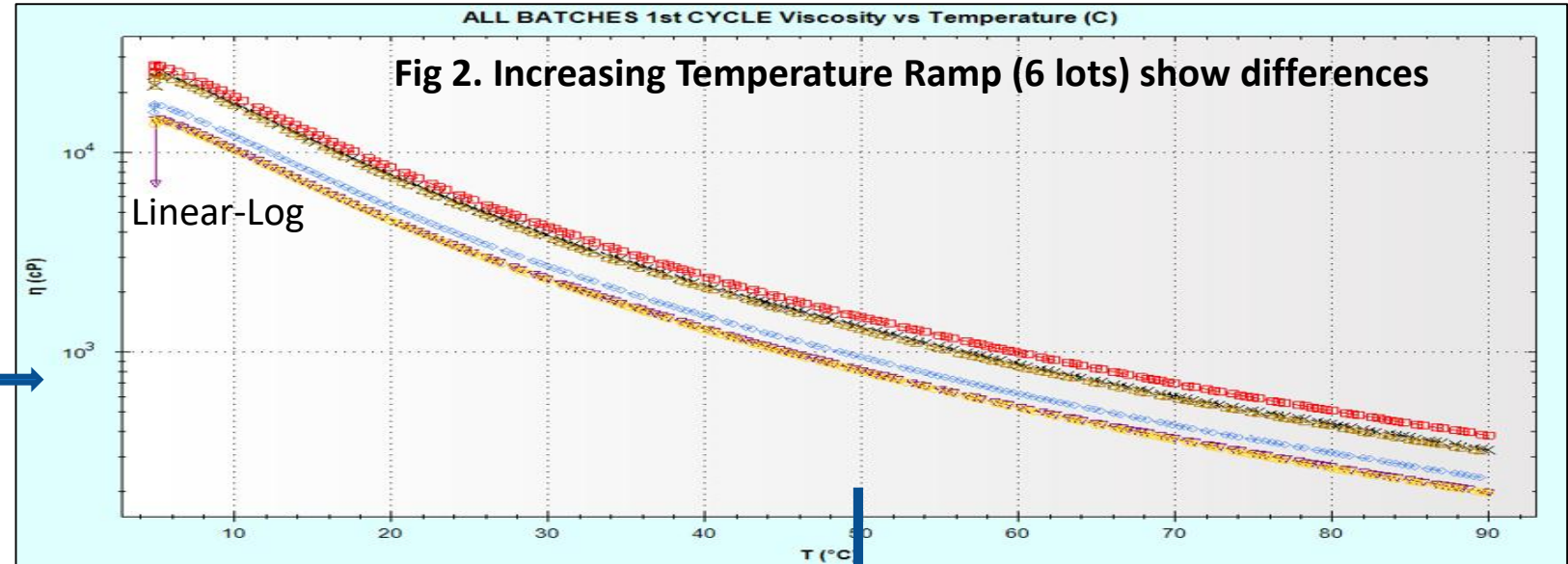
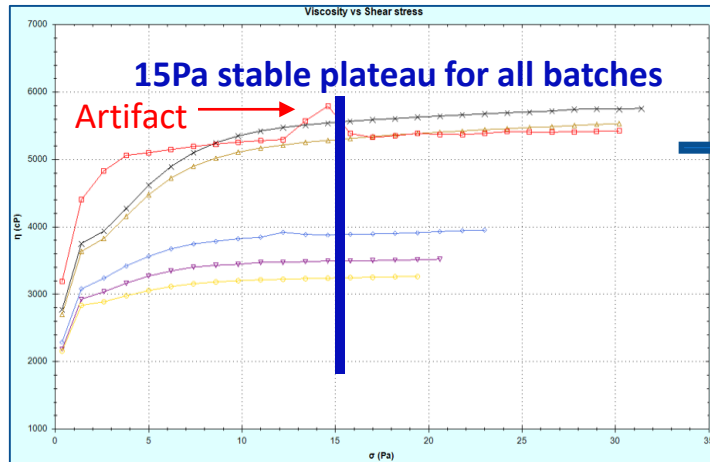




# Application: Temperature Ramp with Single Shear STRESS - 6 dispersed polymers

- **Purpose:** Client requested screen for rheological differences & stability with brief exposure to at 90°C.
- **Result:** Batches differed (Fig 2). All appeared to be rheologically stable with brief heating (Fig 3).
- **Experimental:** 25mm rough parallel plate, 0.2mm gap, 15Pa over 5 → 90 → 5°C (5°C/min)

Fig 1. Preliminary yield stress screen at 25°C  
Identified stable stress input (15Pa) for  
subsequent temperature ramps (Figs 2-3)



# Creep-Recovery for Yield Stress & Elasticity

## Response to applied stress and release

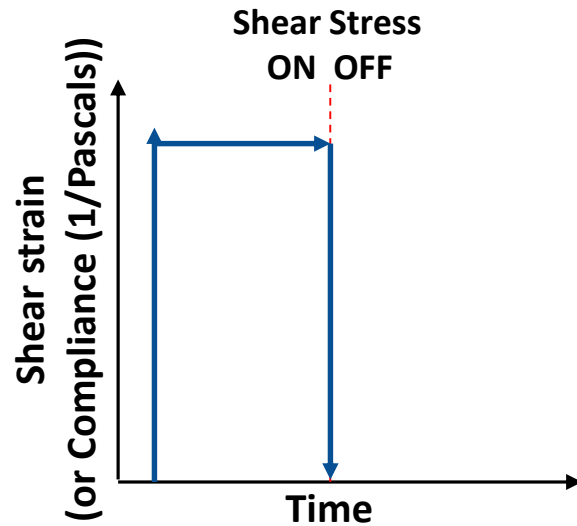
- ⇒ Quantitate net loss of elasticity (fatigue) following stress or strain
- ⇒ Used to determine zero-shear viscosity and evaluate suspension stability



*Squeeze/twist and release.  
Quantify responses.*

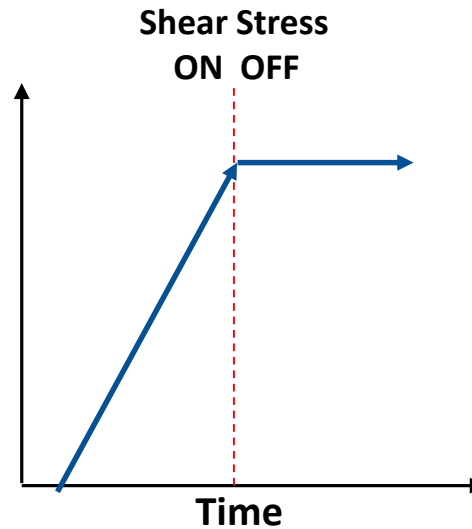
### Pure Elastic

Most stable  
Bounces 100% of initial height



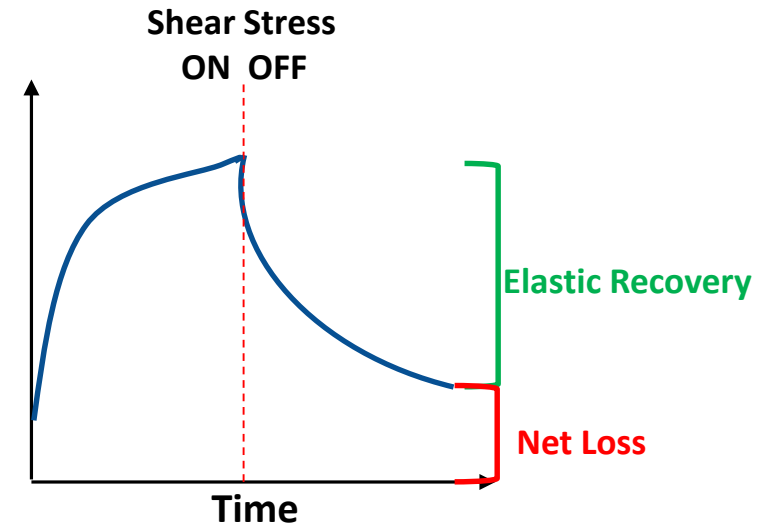
### Pure Viscous

Least stable  
No bounce



### Viscoelastic

Mix of Viscous & Elastic

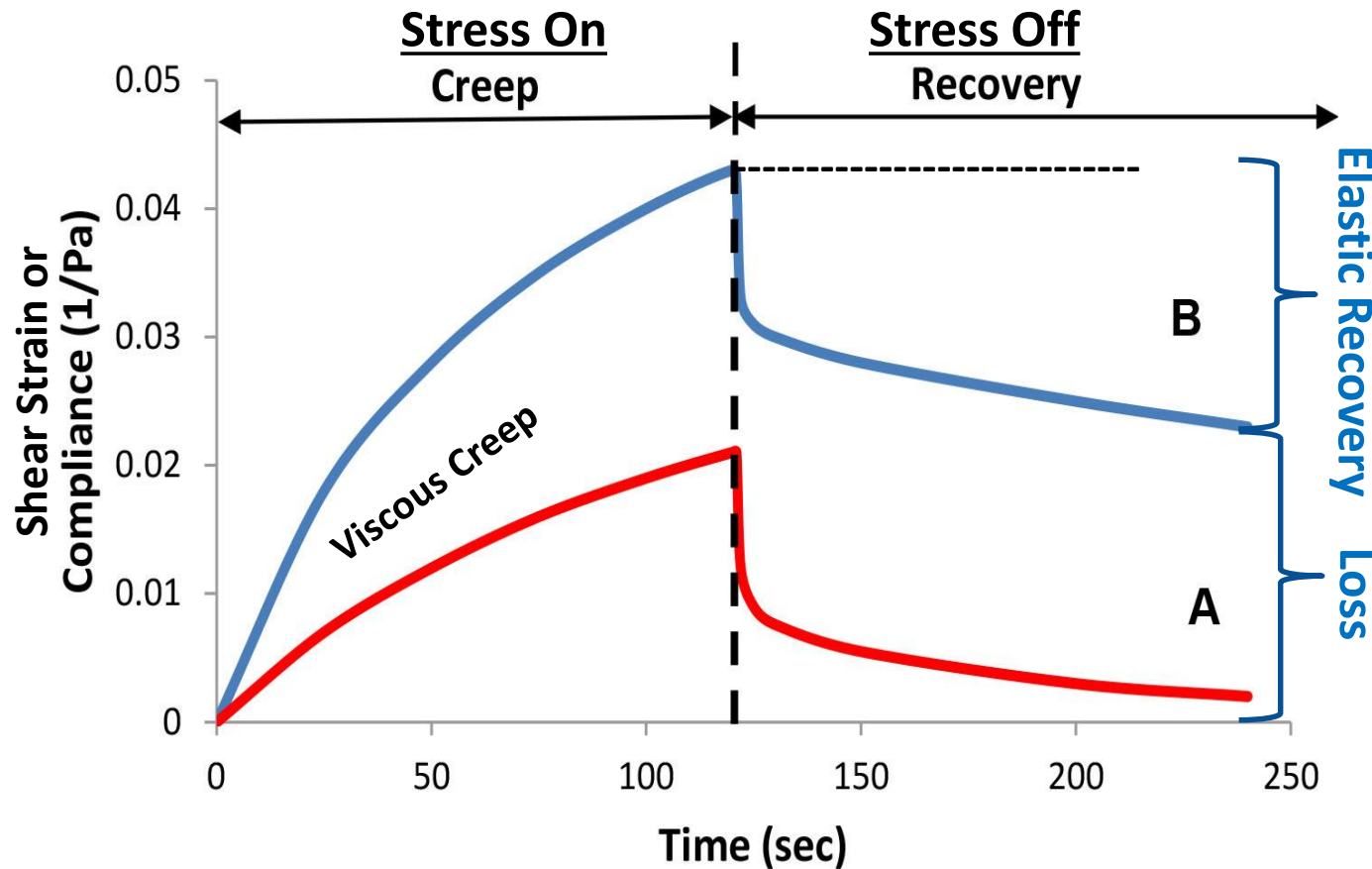


# Creep-Recovery

Response to applied stress and release

⇒ Quantitate net loss of elasticity following stress

## Viscoelastic Material



*Squeeze/twist and release.  
Quantify responses.*

# Application: Tribology (friction) of 4 common 5W-30 motor oils at 15, 25 & 125°C

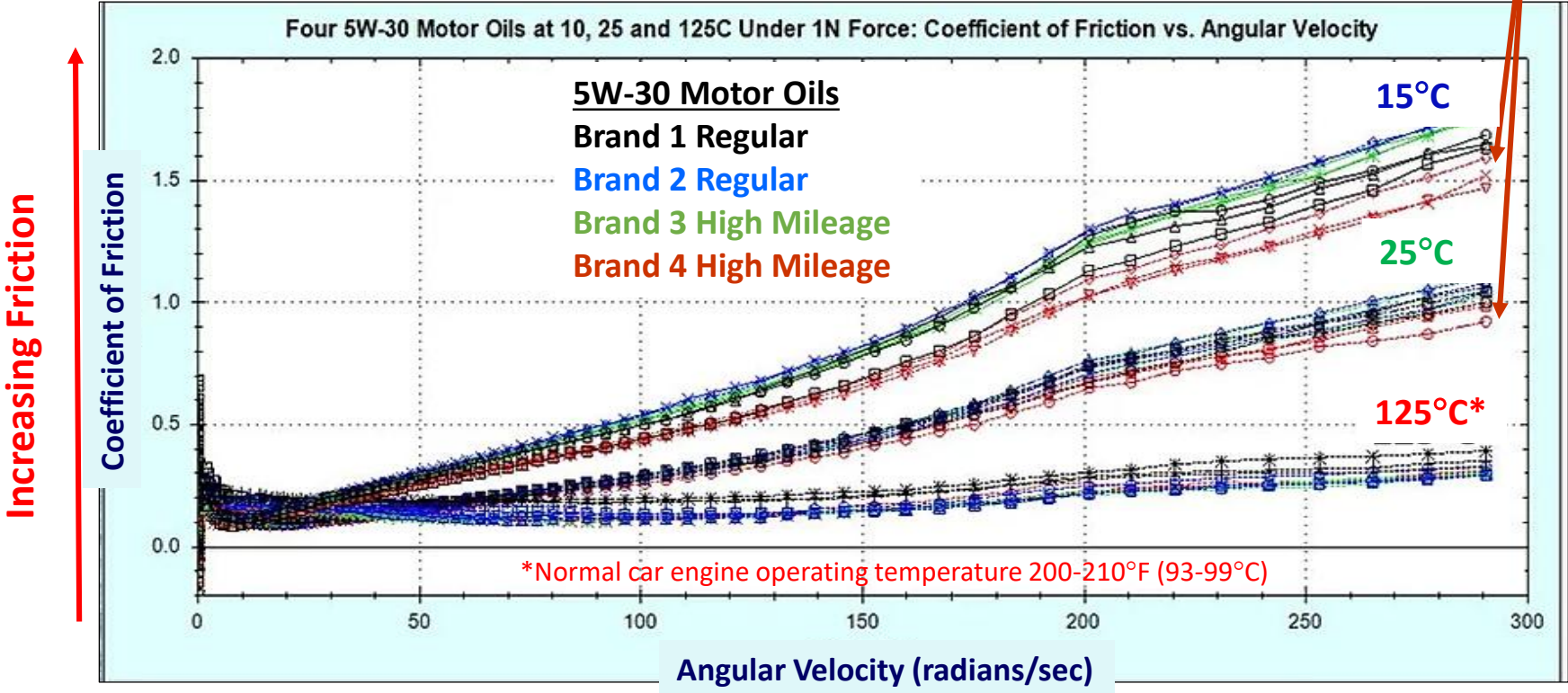
► **Result:** Differences among oils decrease with increasing temperature and decreasing shear  
⇒ food and cosmetics applications



**Brand 4 (high mileage oil)** has lowest friction (CoF) at lower temperatures as ↑ shear.

## Stribeck Curves

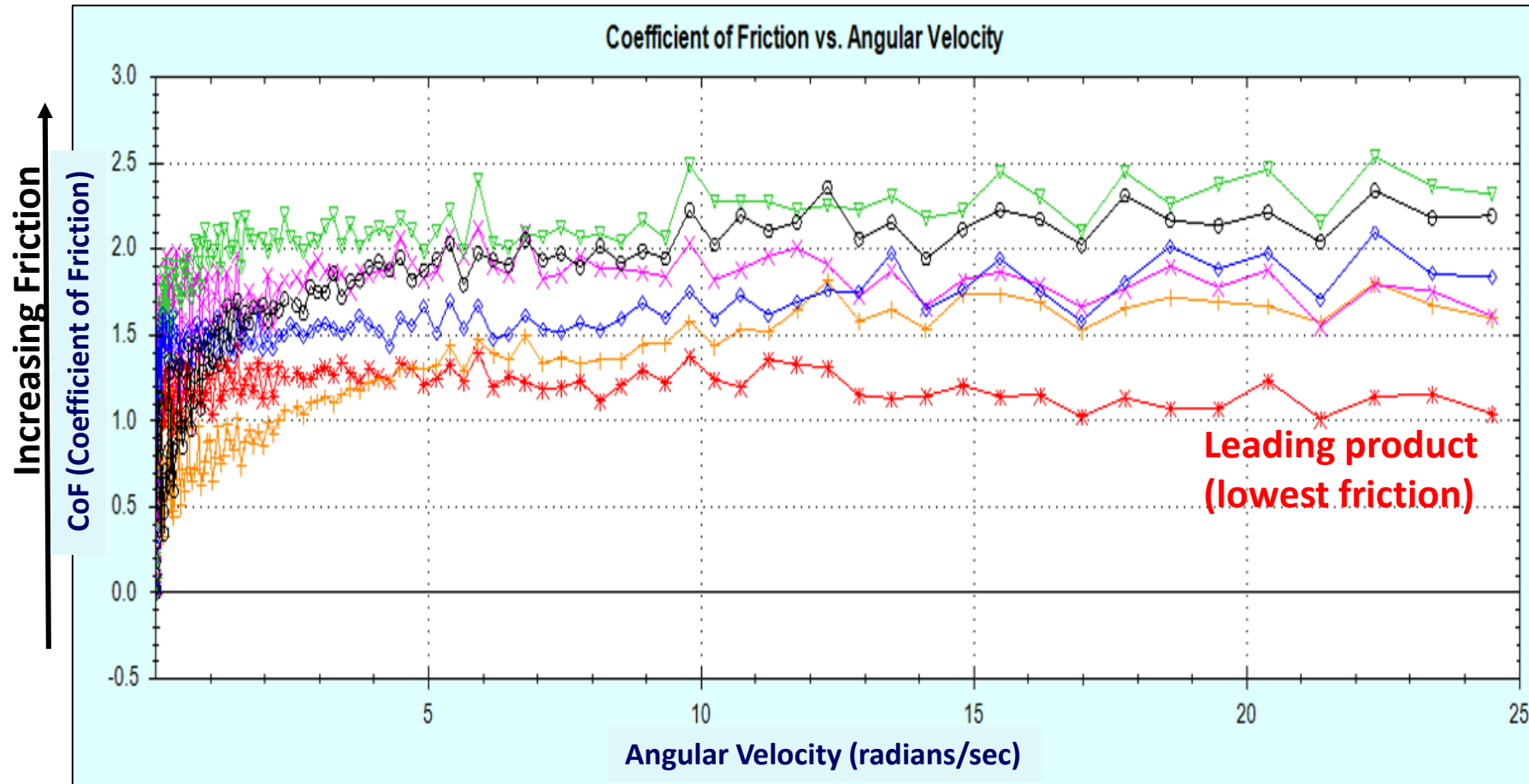
per ISO7148





# Application: Tribology (friction) for arthritis products

- **Purpose:** Client wanted to compare friction properties across 6 products
- **Result:** Observed  $\approx 2$ -fold difference among samples with leading product having least friction (lowest CoF).
- **Experimental:**  $36^{\circ}\text{C}$ , 0.2N downward force over 0.0001 to 100 radians/sec. Requires  $\approx 300\mu\text{L}$  sample.





Now that we've looked at some examples,  
some experimental considerations....

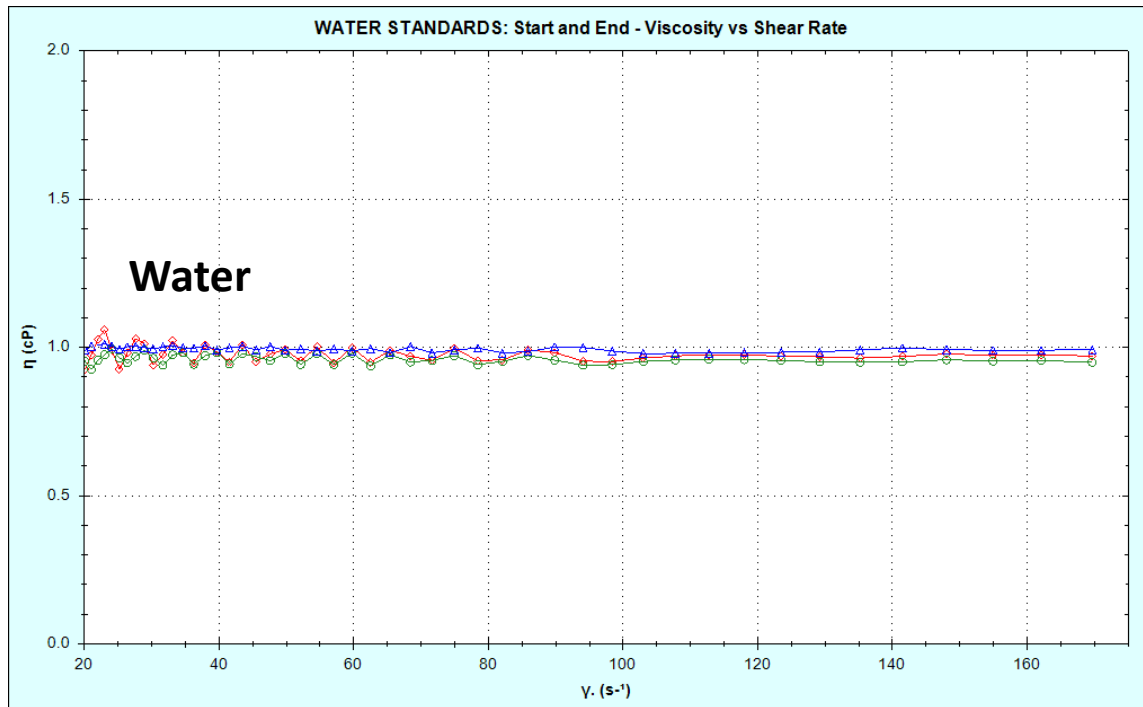


# Preliminaries to Ensure & Confirm Rheometer Performance

- Motor Warmup, Torque Mapping, Geometry Inertia
- Performance standards: start & end bracketing water or silicone oil for rotational assays and PDMS for oscillatory assays

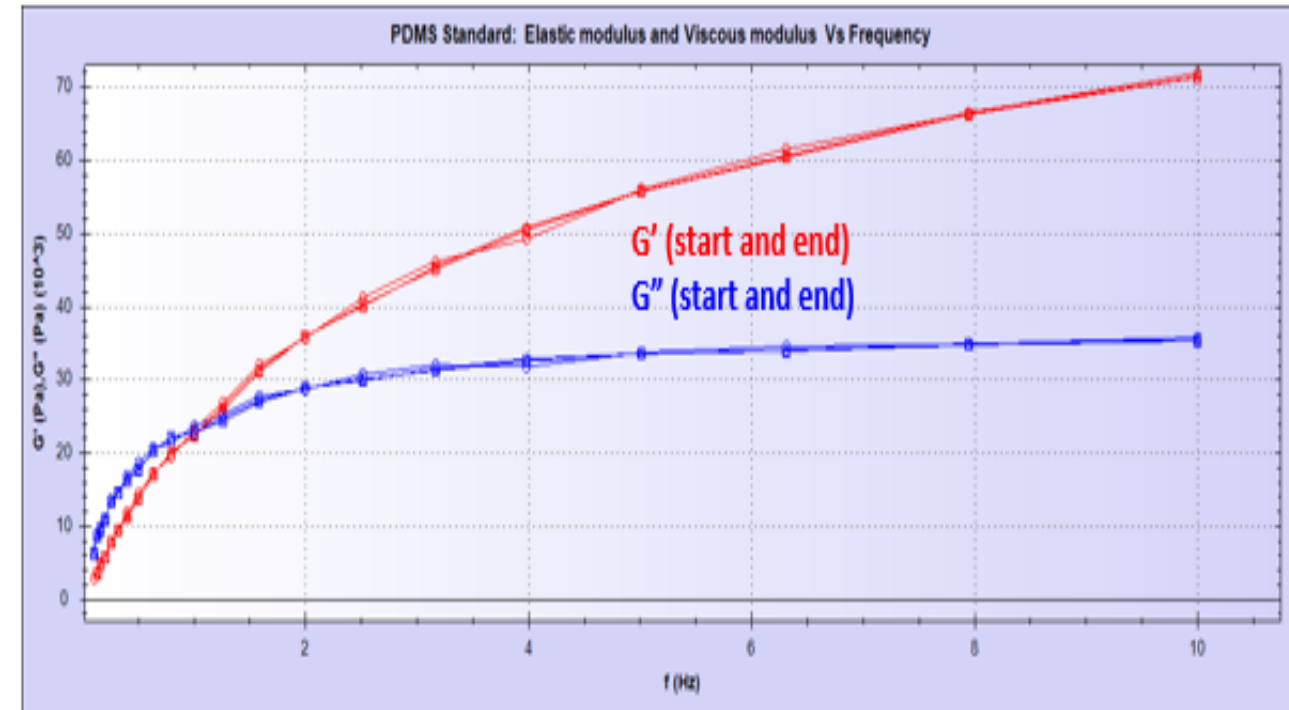
## For Rotational Assays: Shear Rate Ramp (same used for samples)

- Water for highly aqueous, low viscosity samples
- Certified silicone oil standards for higher viscosity samples



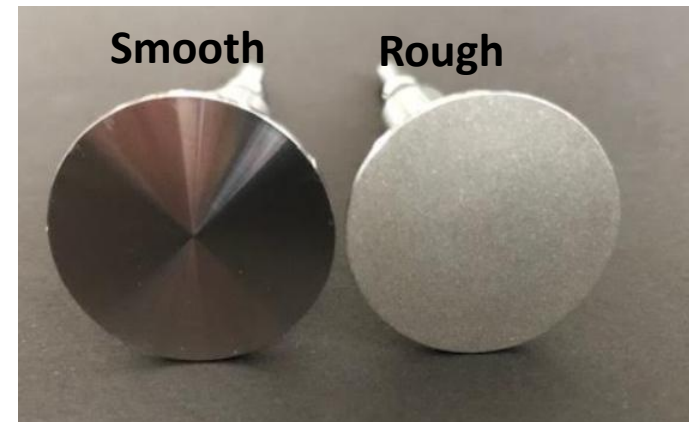
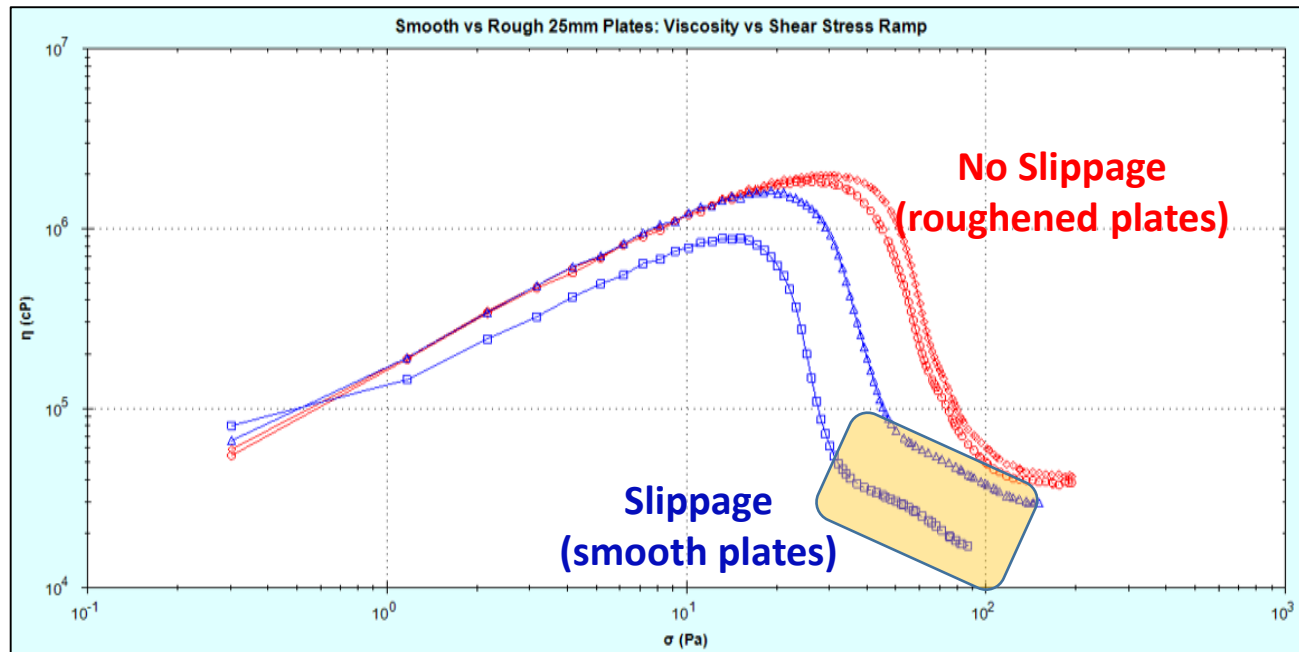
## For Oscillatory Assays: Frequency Sweep

- PDMS Std  
(10 $\rightarrow$ 0.1Hz at 25°C, 0.5% strain, 0.5mm gap with 25mm rough plate vs label claim)



# Mindful about slippage at plate-sample interface

- Plate must impart force through sample, not just at plate-sample interface
  - **Slippage leads to experimental error, variability and conclusions**
  - **If sample not prone to slippage, results should be similar with different gaps (i.e. sample height)**
- Use roughened or serrated plates to reduce potential for slippage



Example of “Slippage” at of top cards→  
Top 2 cards “slip” further than others



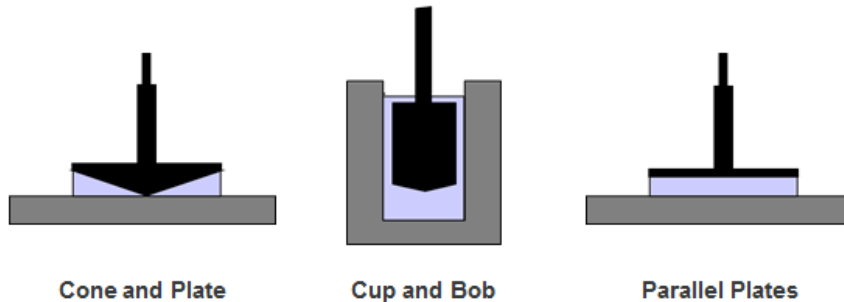
# Other Experimental Considerations

- **Consistency is critical!**

- Handling during loading (minimize shear, bubbles, volatiles loss (more later))
- Trim to remove excess sample

- **Geometry: Cone, Plate or Cup & Bob, vane, many options**

- Cone gives more consistent shear across sample vs parallel plate.
- Cone not recommended for temperature sweeps if not compensate for thermal expansion.
- Plate allows flexible and smaller gap to assay with higher shear rate without losing sample. Cone has default gap.



- **Plate/Cone Size**

- Larger diameter provides more sample contact to provide more torque, hence more sensitivity; but requires more sample.
- Larger diameter is more sensitive for less viscous samples and achieves smaller strain amplitudes for oscillatory assays.
- Larger diameter can generate higher shear rate
- Larger diameter, having more oscillating mass gives “inertia flag” at higher frequency, esp for lower viscosity samples.
- Smaller diameter better for more viscous and viscoelastic samples. Also uses less sample.
- Smaller cone angles achieve higher shear rates.

# Other Experimental Considerations (continued)

- Consistency is critical! ...repeating

$$\text{Shear rate} = \text{strain/time}$$
$$(\text{Strain} = \text{displacement/height})$$

- Gap (sample height)

- Typically 0.2-1mm. Depends on sample and assay parameters. (human hair  $\approx 70 \pm 20 \mu\text{m}$ )
  - Smaller gap requires less sample (100ul for 25mm plate with 200um gap)
  - Smaller gap:
    - Generates higher shear rate.
    - Reduces potential to lose sample from gap at high shear rate. Observe stress  $\downarrow\downarrow$  with  $\uparrow$  shear rate if sample displaced.
    - Small gap inaccuracies may lead to modest % assay error.
  - Larger gap facilitates smaller strain amplitude
  - 1/10 rule: plate-plate or plate cone gap  $\geq 10 \times$  largest particle or droplet. Cones have fixed default gaps.
  - Gap setting options to provide consistent sample loading:
    - height controlled  $\rightarrow$  For most samples. Typically 200-1,000um.
    - force controlled  $\rightarrow$  For samples with inconsistent thickness (i.e. cheese), rigid & difficult to compress (polymer films). Rheometer software accounts for sample height throughout assay to calc outputs.
- $\Rightarrow$  Kinexus rheometer tracks both gap height and force for each datapoint throughout assay.



# Other Experimental Considerations (continued)

- **Pre-Shear or not to pre-shear.....**

- Depends on question to be answered

- Any sample movement (loading) may irreversibly shear thin sample, maybe not!?! Screen with thixotropy assay (later)

- Can apply very low pre-shear to “normalize” for handling effects

- BUT...** pre-shear can “erase” other rheological properties especially if sample easily shear thins with poor rebuilding.*

- **Sample change during handling and analysis**

- Curing, degradation, rebuilding, cross-linking, volatiles loss, etc

- Rotational: Screen with single shear rate or shear stress vs time at assay temperature(s) and monitor viscosity

- Oscillatory: Screen with single frequency vs time & monitor  $G'$ ,  $G''$ ,  $\delta$ ,  $G^*$  changes.

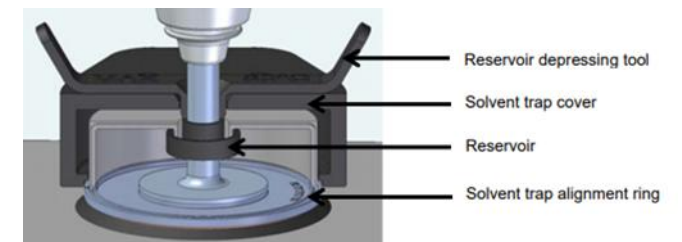
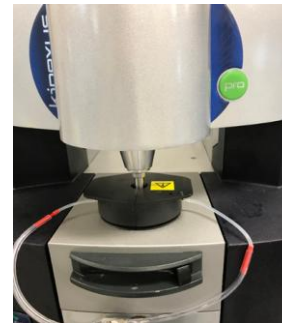
- What are  $G'$ ,  $G''$ ,  $\delta$ ,  $G^*$  ? Stay tuned.....*



- Got volatiles? Use a solvent trap

- Maintain sample in enclosed volatiles saturated environment (i.e. humidity)

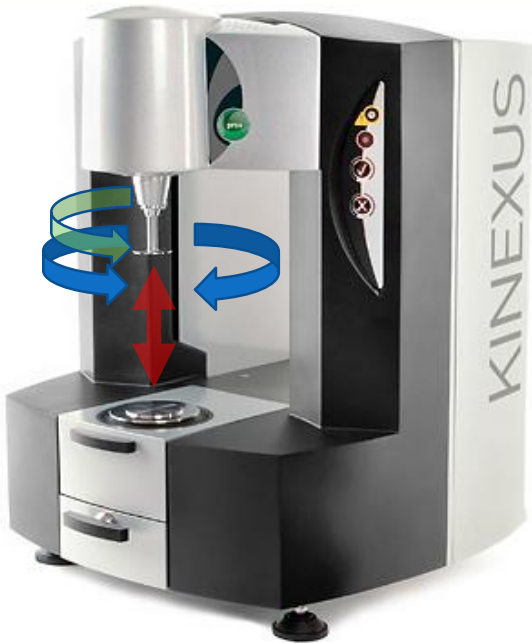
- Sensitivity to oxidation at elevated temperature → enclosed, low  $N_2$  flow



# Switching gears from rotational to oscillatory assays → DEFORMATION

## Movements → torque

- Rotational (1 direction)
- Oscillatory (bi-directional)
- Vertical



# Oscillation $\approx$ washing machine agitator...sort of

## 2 Ways to Modulate Oscillation:

### 1. Amplitude (destructive)

- Determine Linear Viscoelastic Region (LVER)  
 $\Rightarrow$  “Breaking point” of structure  $\propto$  stability
- Quantify textural properties: stiffness, springiness, structural strength, brittleness

### 2. Frequency (non-destructive)

- Measure response to event time  $= 1/\text{freq}$ 
  - Probe structural properties within LVER to maintain rheological integrity during assay

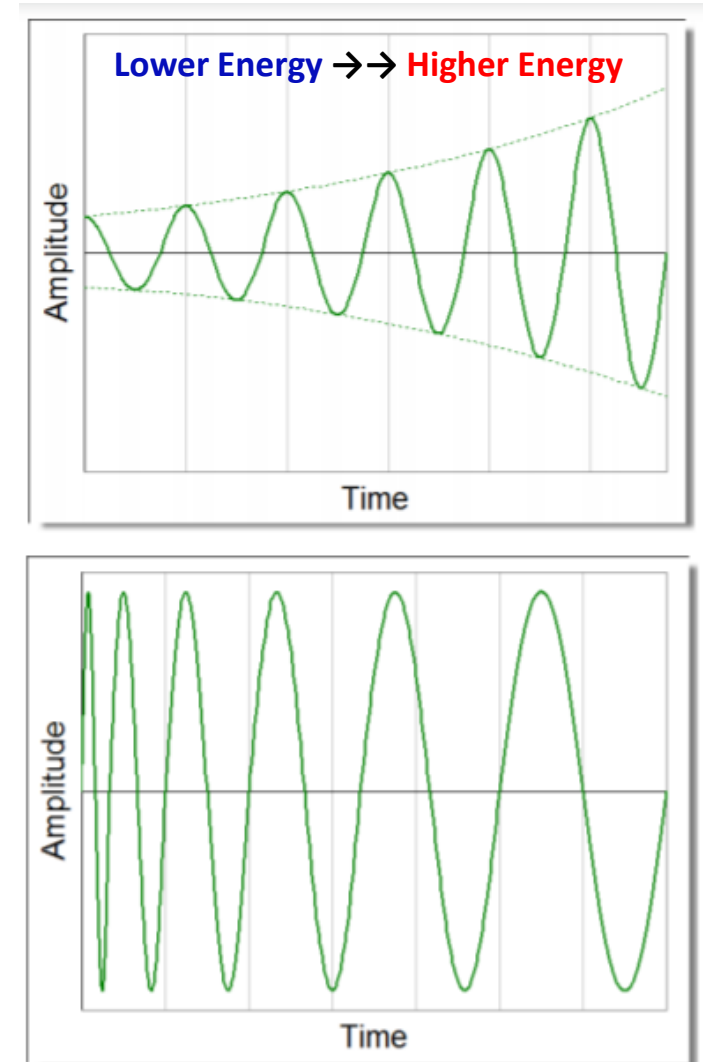


Image from Netzsch

# Oscillation - Amplitude Sweep

- ⇒ Increase amplitude (back-forth movement) until “break” macrostructure
- ⇒ **Preliminary assay to determine LVER before perform frequency modulated assays to ensure sample integrity.**
- ⇒ LVER can decrease with increasing frequency. Typically perform assays at 1Hz.
- ⇒  $G'$  (elastic modulus; solid-nature) tends to increase with increasing frequency
- ⇒ LVER tends to decrease with increasing solid form (i.e. temperature dependence).  $LVER_{\text{melted}} > LVER_{\text{not melted}}$

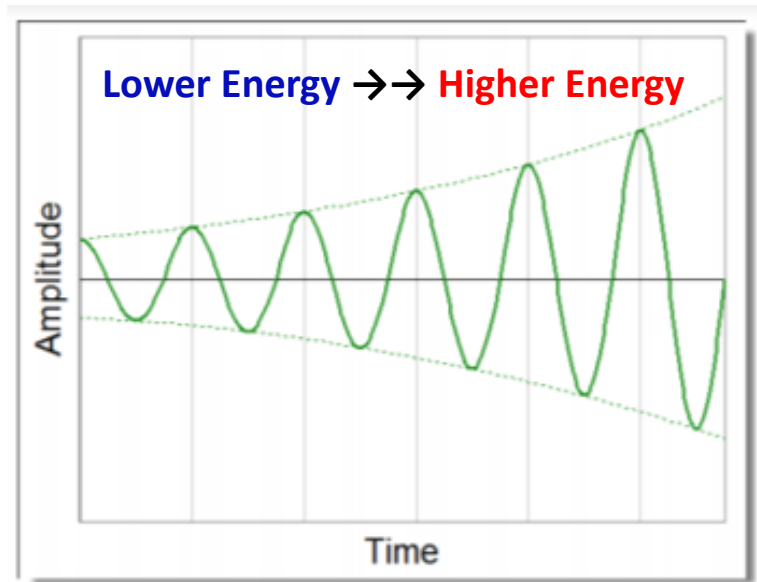
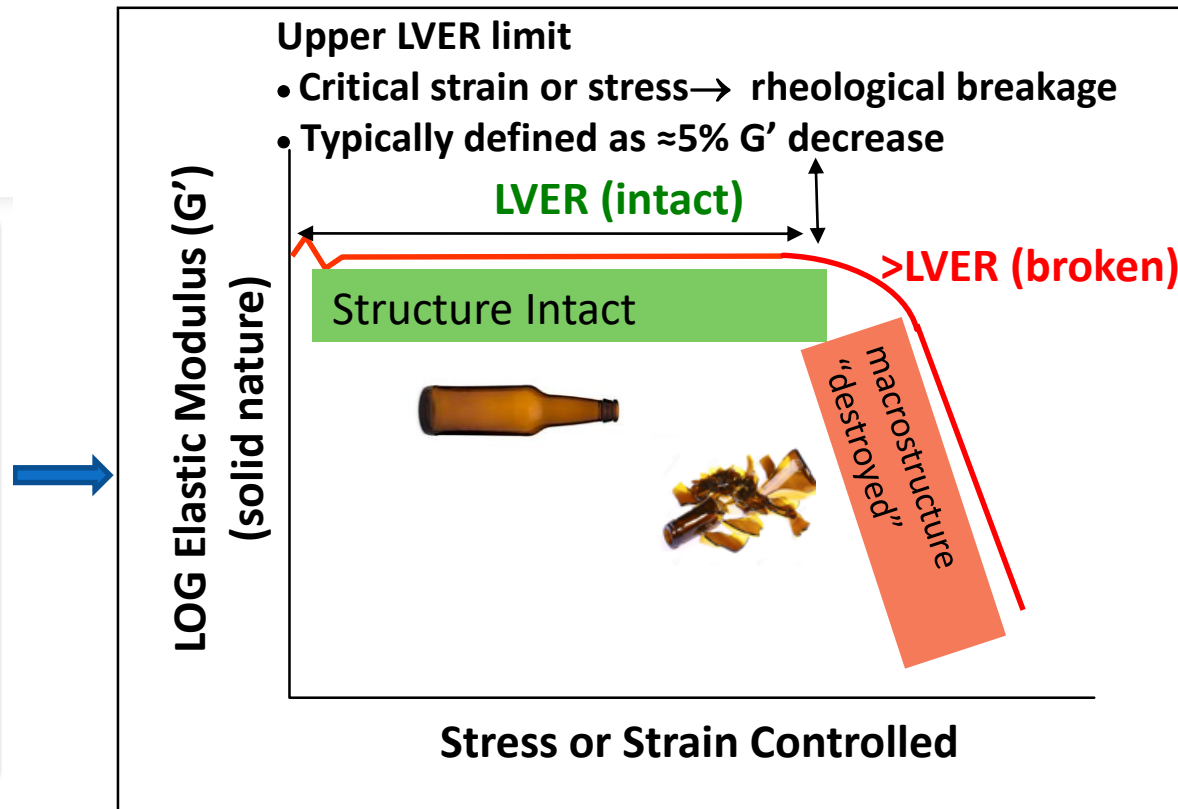
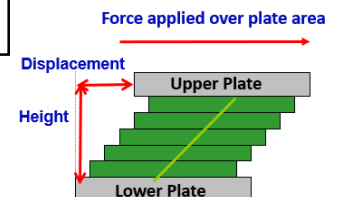


Image from Netzsch



**Stress controlled:** Measure sample movement from defined applied force (stress= $F/A$ ).  
**Strain controlled:** Measure torque required to move sample defined displacement.

Rheology Testing Services



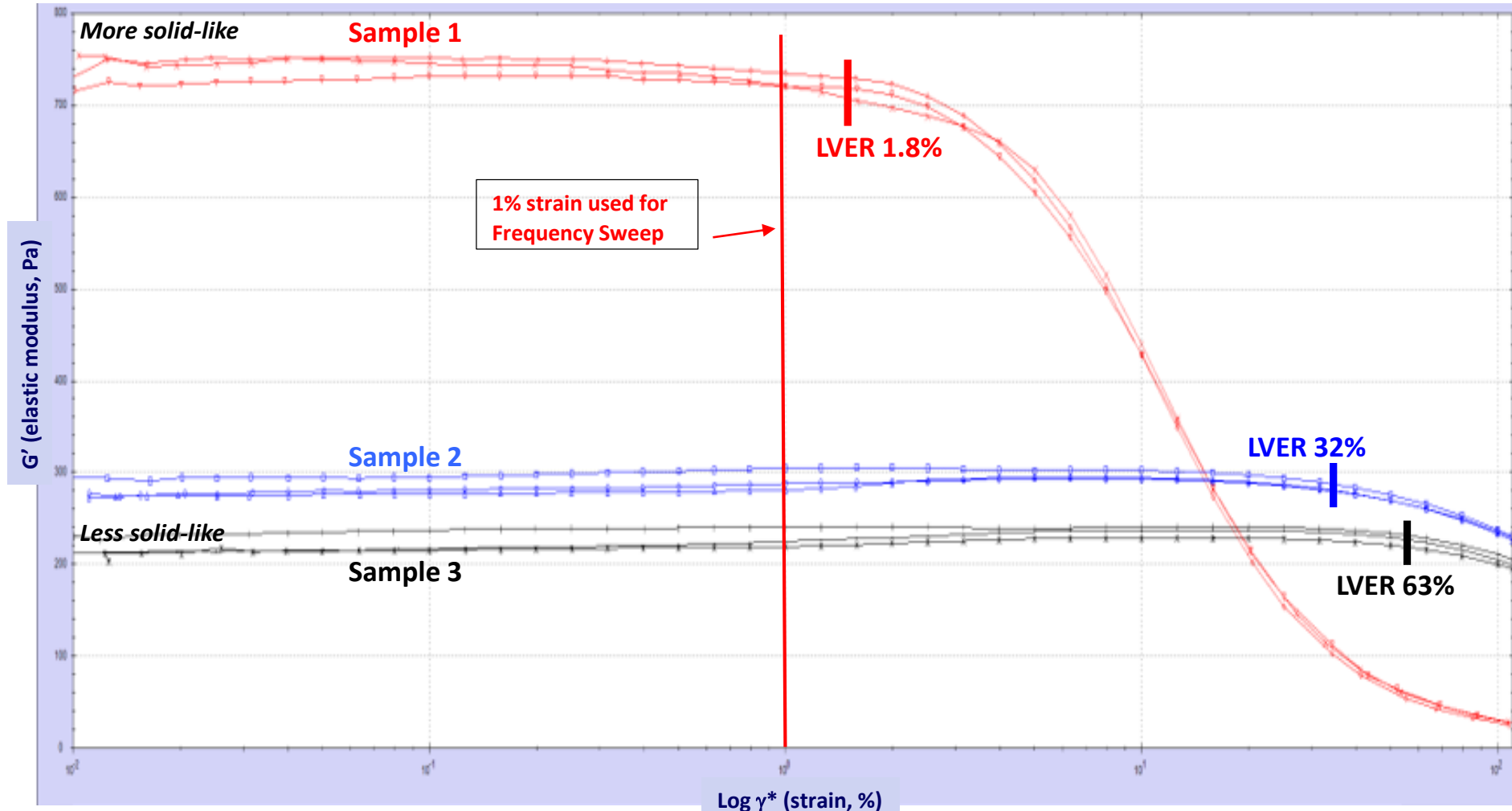
# Application: Amplitude Sweep: $G'$ vs % strain to determine LVER for gels containing hyaluronic acid

→ strain = extent of sample deformation relative to sample height

► **Purpose:** Compare properties. ALSO need LVER from this assay to define %strain (within LVER) input for subsequent frequency sweeps.

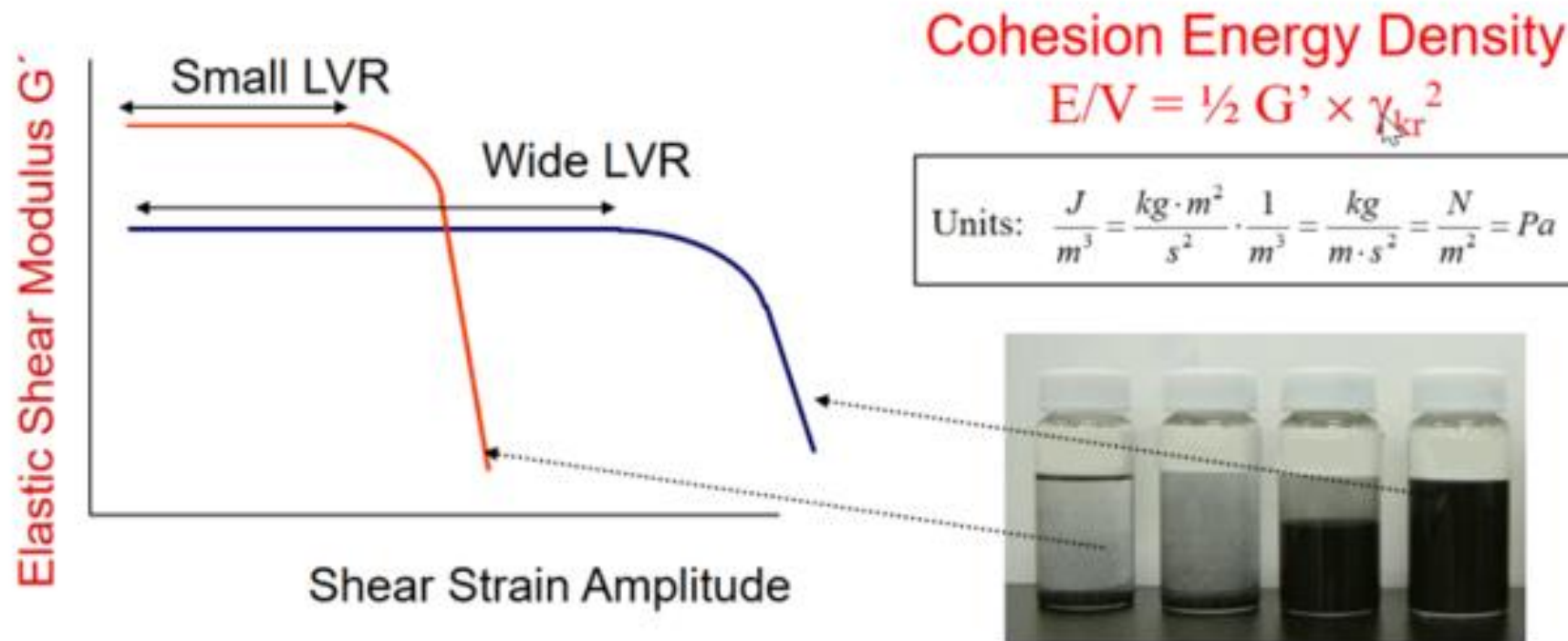
► **Result:** Observed large LVER and  $G'$  differences. Determined input %strain for subsequent frequency sweeps.

**Note:** LVER typically defined as 5%  $G'$  decrease. Determined from data tables, not visually from plots.





Quick Check of Shelf Life without Prediction of Timescale!

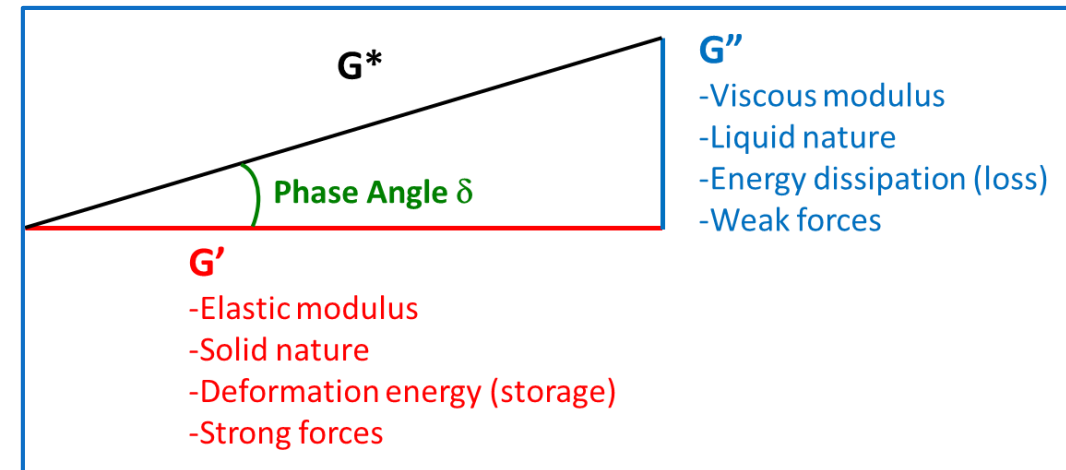
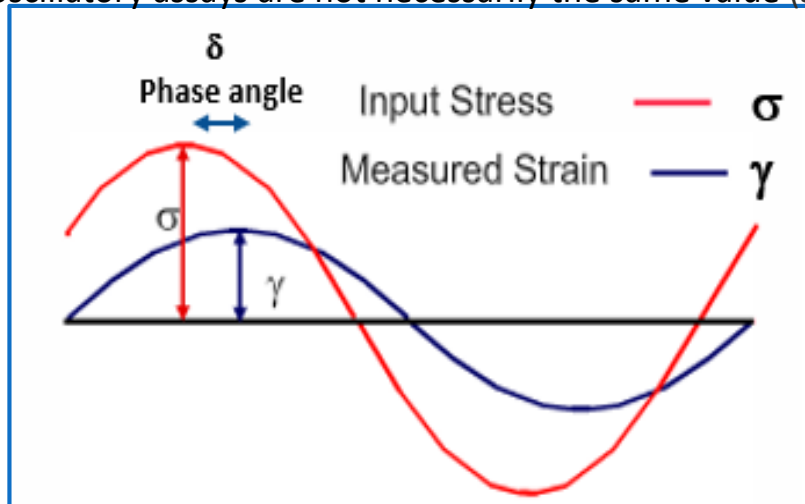


Long-Range Interactions increase the Cohesion Energy by enlarging the LVR.

# Oscillatory Assay Output Summary: $G'$ , $G''$ , $\delta$ , $G^*$ , $\eta^*$ and tan delta to Quantify Viscoelastic Deformation



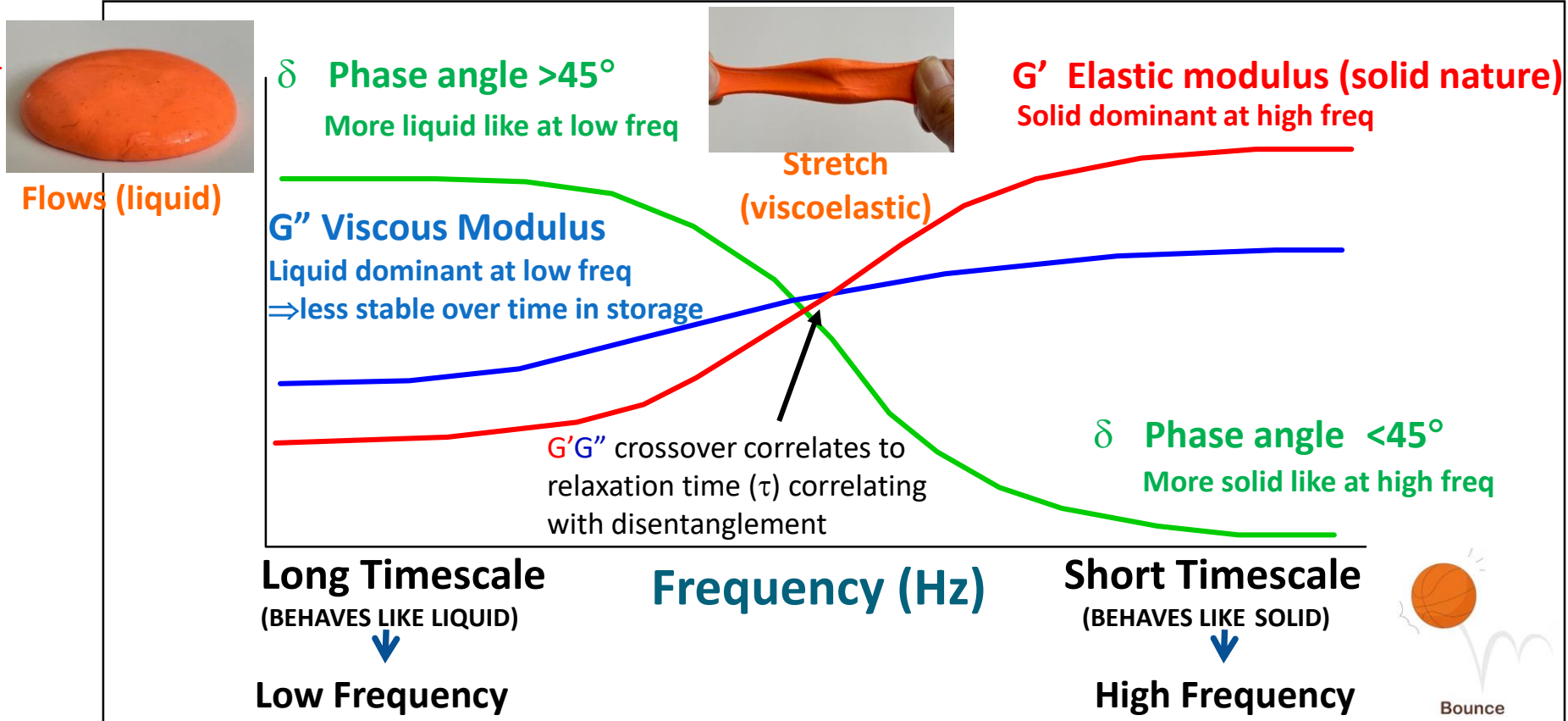
- $G'$  (Pascals; Pa) : Elastic or “storage” modulus  $\propto$  solid nature
- $G''$  (Pascals; Pa) : Viscous or “loss” modulus  $\propto$  liquid nature
- $\delta$  (degrees): Phase angle  $45^\circ \rightarrow 0^\circ$  increasingly solid  
 $45^\circ \rightarrow 90^\circ$  increasingly liquid
- $\tan \delta$  (unitless):  $= G''/G' \propto$  ability to store (solid-like) and release (liquid-like) energy.
  - With decreasing tan delta, particles increasingly associated due to colloidal forces, sedimentation could occur
  - The lower the frequency of  $G'G''$  crossover, the higher the molecular mass.
  - $<1$  increasingly solid-like;  $>1$  increasingly liquid like;  $= 1$  is  $G'G''$  crossover (phase transition, melting pt, gel pt)
- $G^*$  (complex modulus; Pa)  $= \text{Stress}_{(\max)} / \text{Strain}_{(\max)} \propto$  Stiffness
- $\eta^*$  (complex viscosity; cP or Pa-sec)  $= G^* / 2\pi f$  where  $f$  = angular frequency that must be units of radians/second  
 $\Rightarrow$  Depending on sample properties, it is important to note that “ $\eta$  viscosity” obtained with rotational assays and “ $\eta^*$  complex viscosity” determined with oscillatory assays are not necessarily the same value (see references about [Cox-Merz Rule-Netzsch](#) and [Cox-Merz Rule-TA](#)).



# Frequency Sweep: Example Silly Putty → Viscoelastic Liquid or Solid?

- Probe properties across a time domain. Frequency = 1/time (sec)
- Generates rheological “fingerprint” or “spectrum”
- Use % strain as assay input **within LVER** determined with amplitude sweep

At lower Hz, sample molecular relaxation time is shorter than applied test freq, more liquid-like with  $G'' > G'$  ⇒ flows.



At higher Hz, sample molecular relaxation is longer than test freq, more solid-like with  $G' > G''$  ⇒ bounces.

**Bounces (solid)**

# Application: Frequency Sweep - Quantify Texture

Complex modulus ( $G^*$ ) vs Phase Angle ( $\delta$ ) at 1Hz and consistent %strain

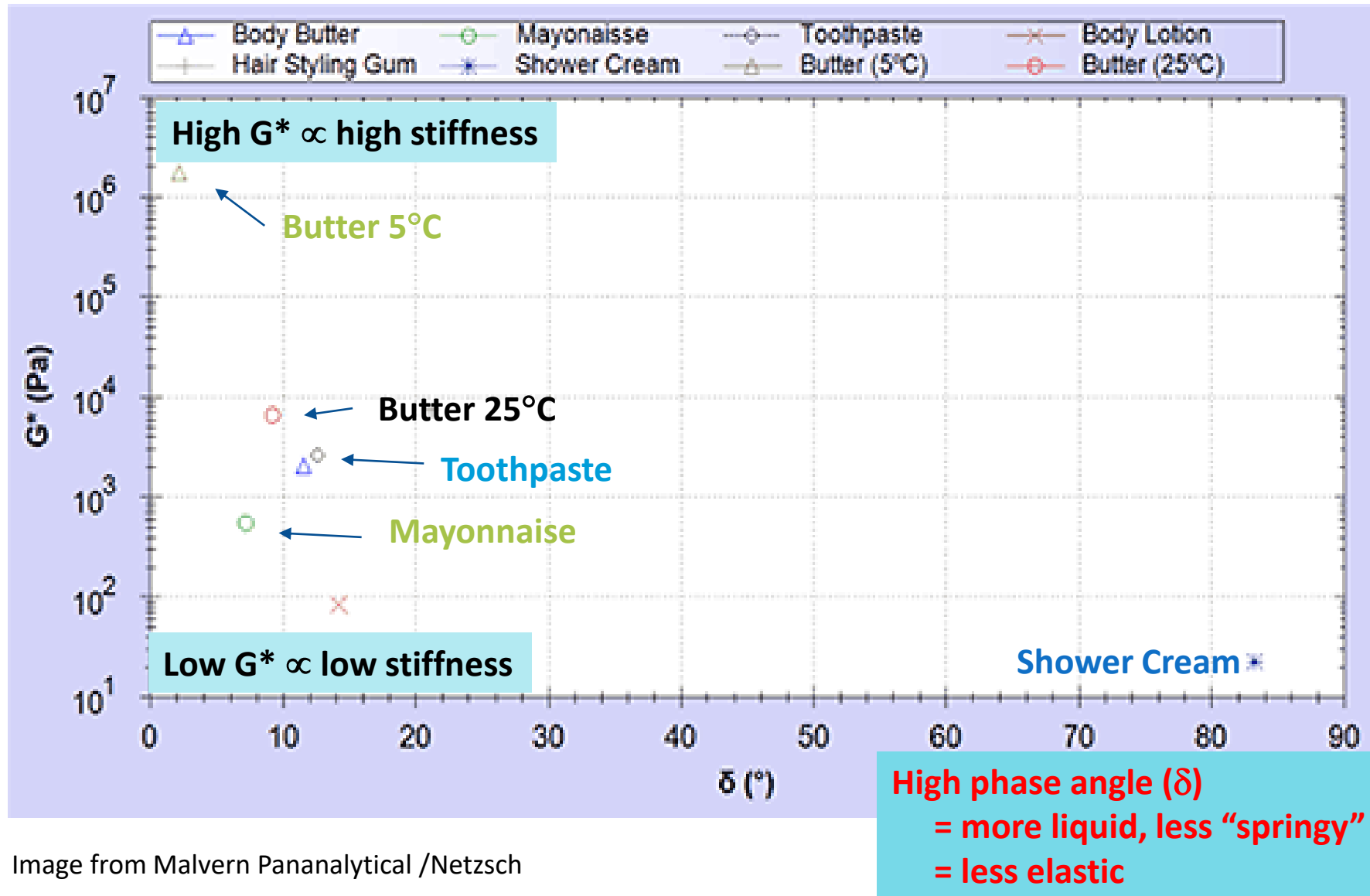
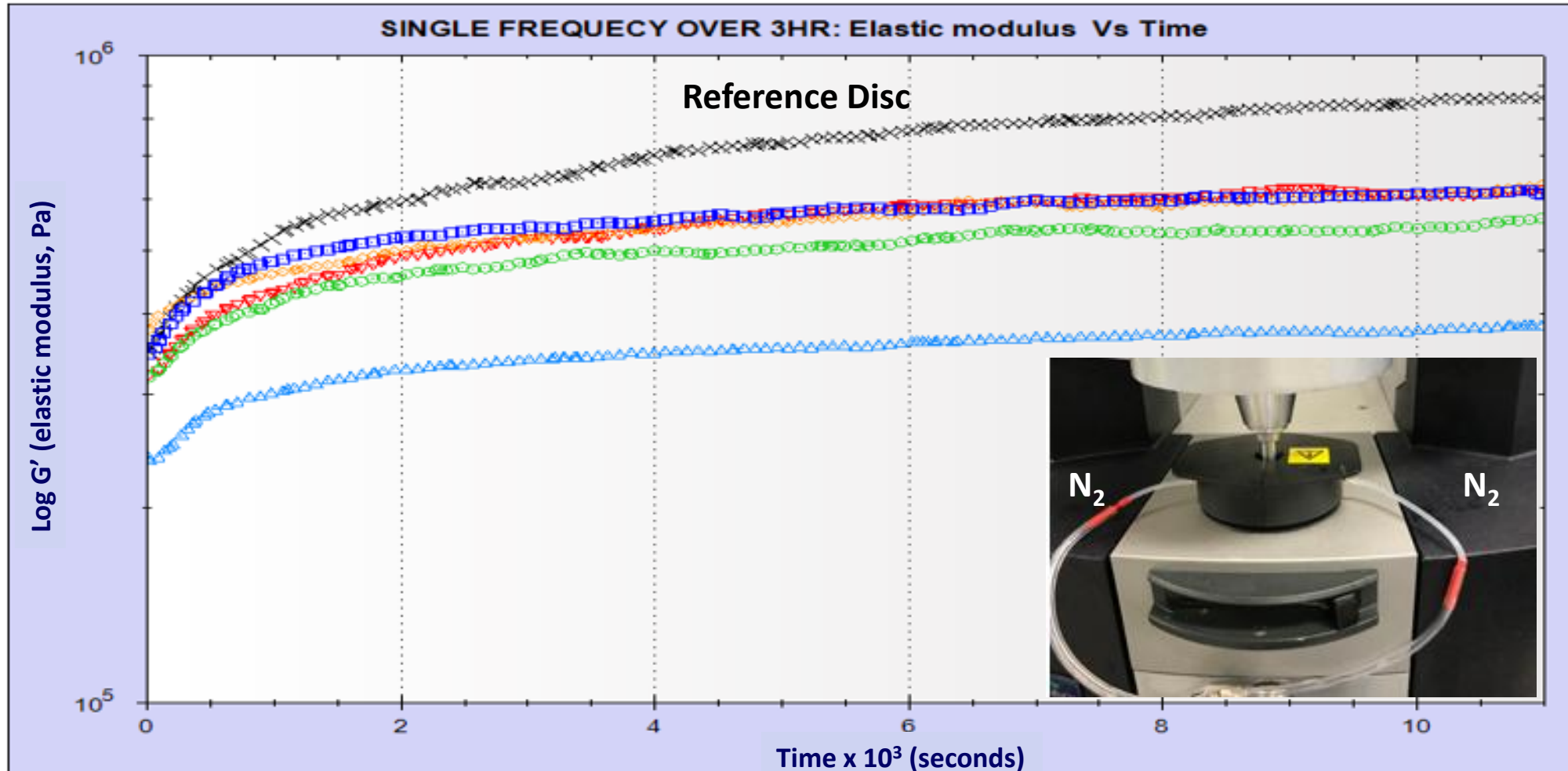


Image from Malvern Pananalytical /Netzsch

# Application: Stability - Single Frequency and %Strain for Polymer Discs

- **Purpose:** Compare thermal stability of discs vs % anti-oxidant relative to Reference Disc
- **Result:** Samples show different  $G'_{\text{(plateau)}}$  and stabilization rate
- **Experimental:** Gap discs with 4N downward force, assayed 3hrs at 180°C under  $N_2$  with 1.59Hz at 0.5% strain

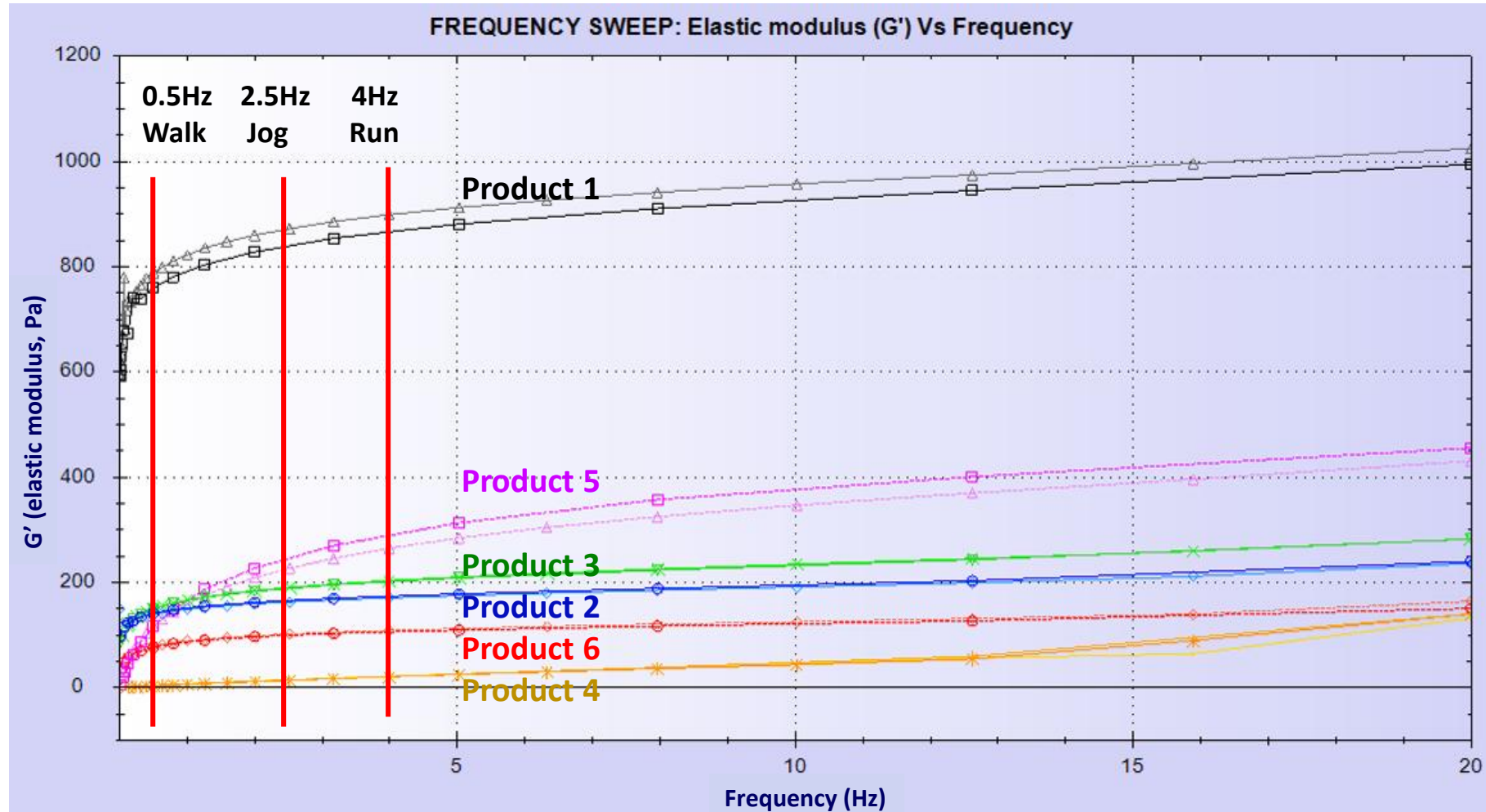




# Application: Frequency sweep $G'$ 20-0.01Hz, 3% strain\* for 6 Arthritis products

⇒ ID products that stiffen more than others with increasing frequency ( $\propto$  exercise) as shown in results

- **Purpose:** Client requested detailed comparison for rheological of 6 products. Assayed in duplicate.
- **Results:** Significant differences. Helpful for Q3 (ANDA) pharma, ID counterfeit and adulterated products



\* 3% strain obtained from literature and also confirmed with amplitude sweep

# Application: FREQUENCY SWEEP – Sensory Screen

- Pull-away assay also correlates well with sensory panel results

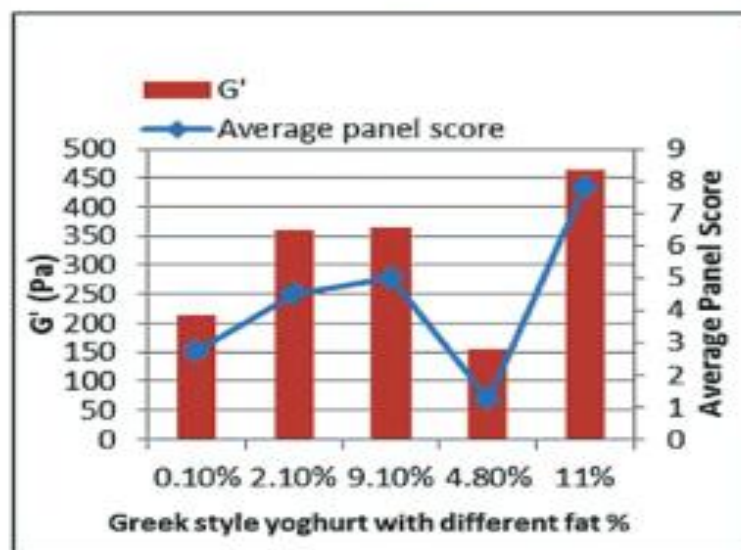
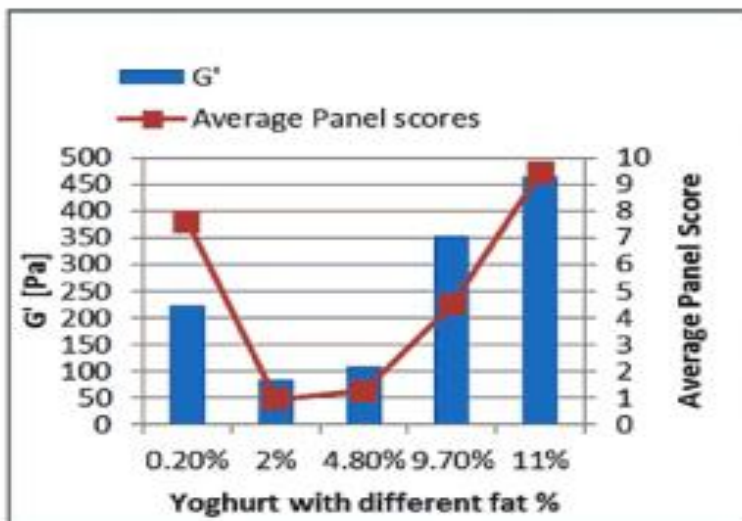
## Yogurt - sensory-rheology

Firmness vs elastic modulus relationship

High fat always scores well.....

**Note  $G'$  here – correlates to panel score....**

Dairy Innovation Australia Sensor  
Analysis Lab



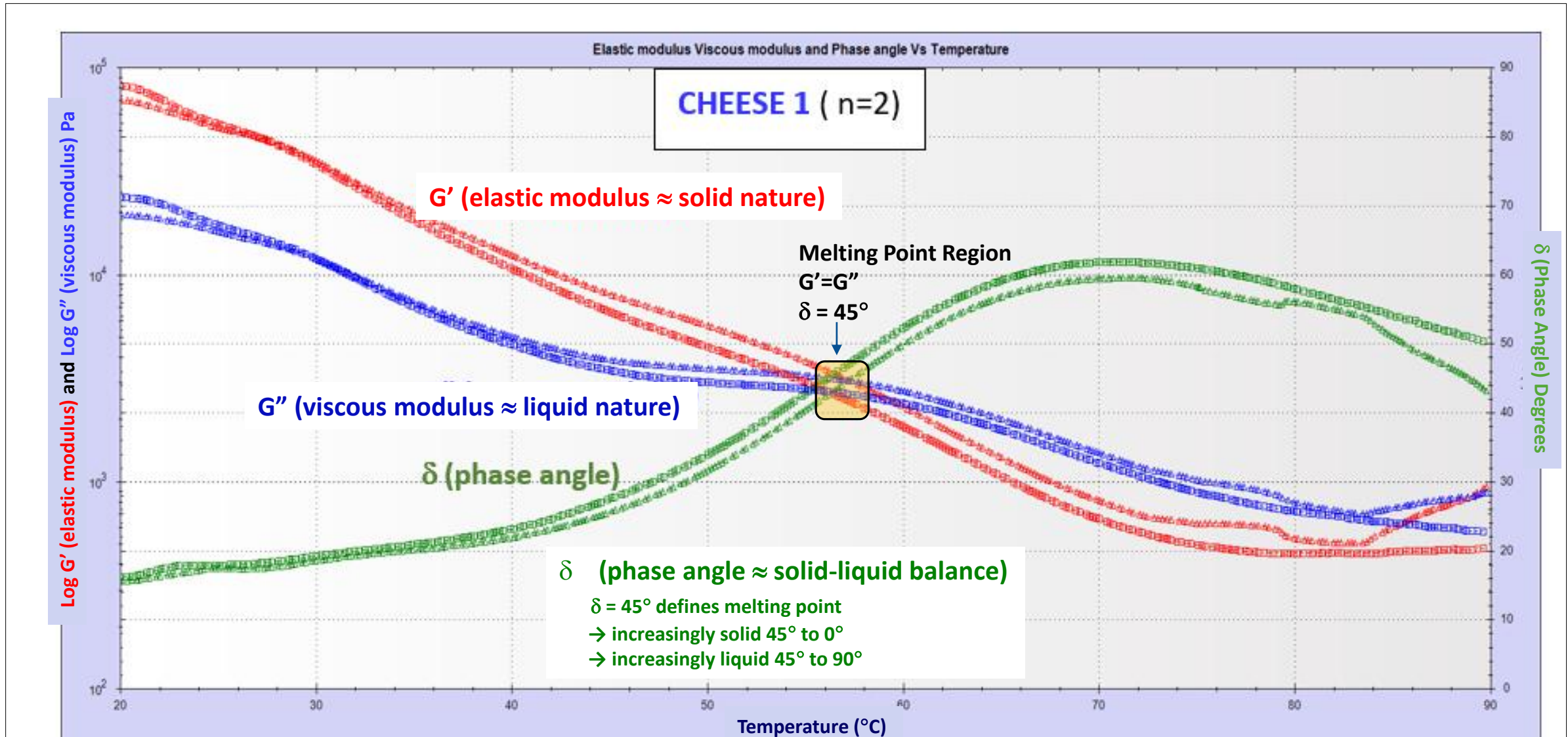
Ranjan Sharma Dairy Australia/NCDEA

“Sensory Quality Aspects of Yoghurt” Webinar - 11 July 2013

Image from Malvern Pananalytical/ Netzsch

# Application: Oscillatory Single Frequency Temperature Sweep - Melting Point of Cheese

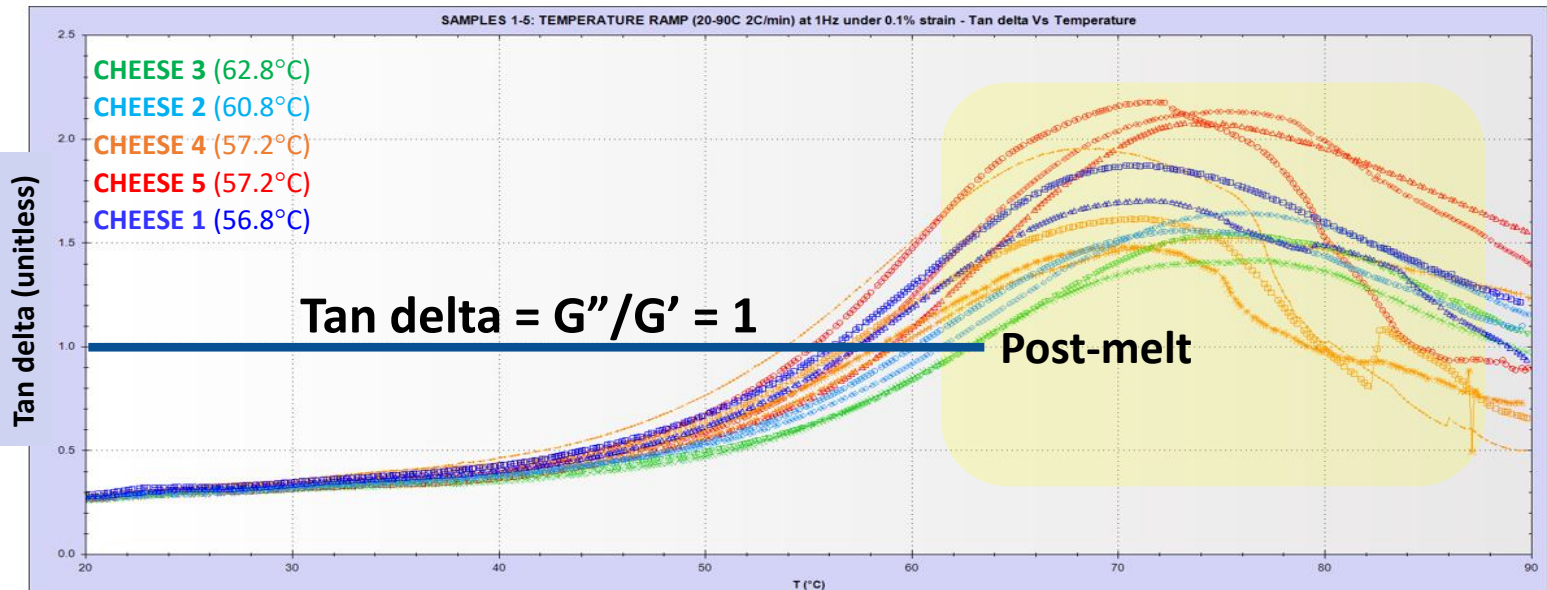
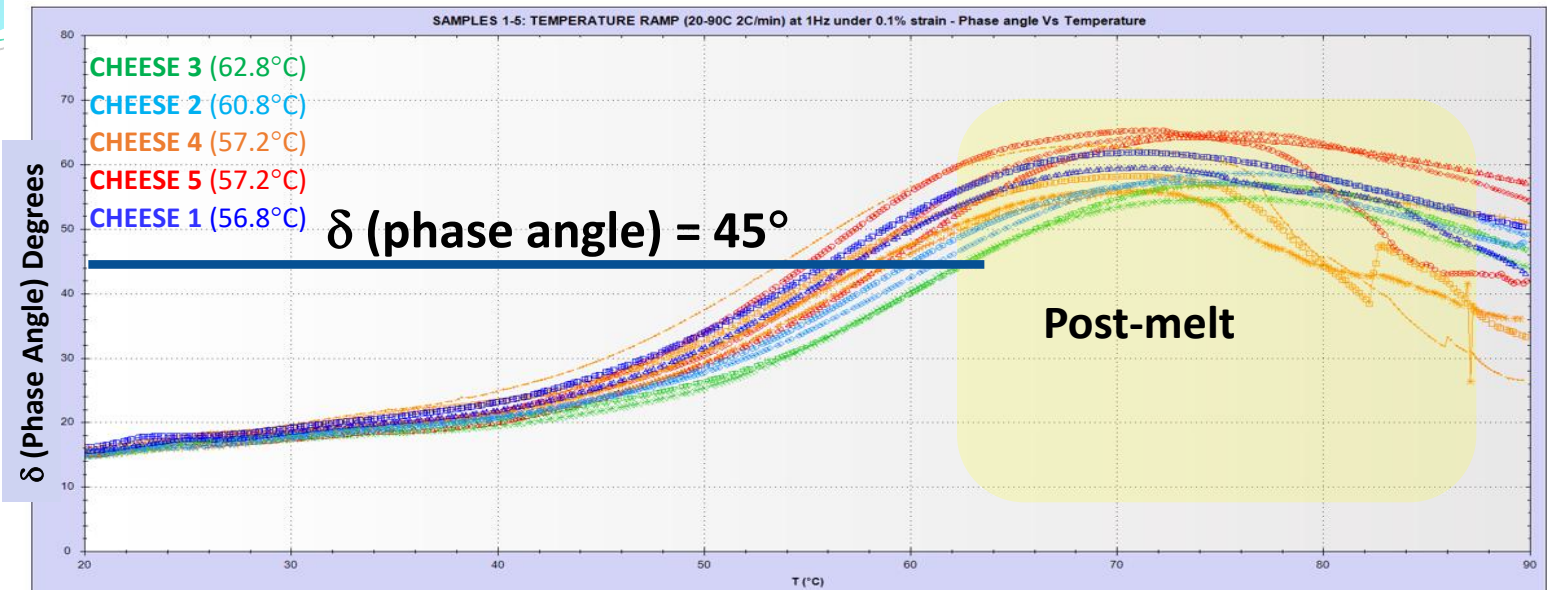
- Quantify melting pt with  $G'G''$ - crossover and phase angle ( $\delta=45^\circ$ )





# Application: Oscillatory Single Frequency Temperature Sweep - Melting Point of Cheese

- Quantify melting pt with phase angle ( $\delta=45^\circ$ ) and Tan delta ( $G''/G'=1$ )



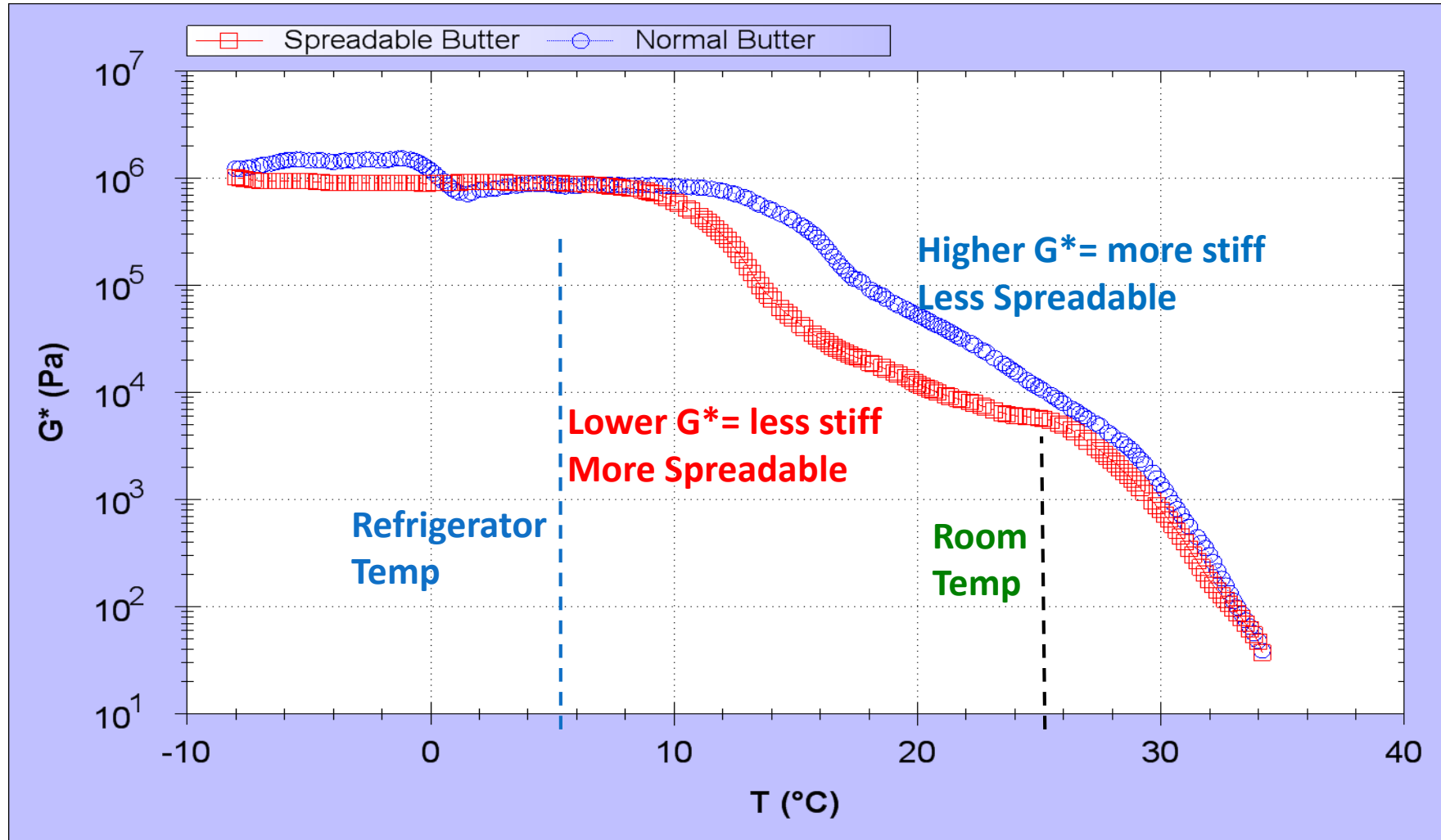
REPRODUCIBILITY*	
Sample	Melt Point °C
CHEESE 1	56.28
	57.35
AVG	56.8
CHEESE 2	60.21
	61.41
AVG	60.8
CHEESE 3	62.93
	62.69
AVG	62.8
CHEESE 4	59.39
	58.46
	53.95
	56.96
AVG	57.2
CHEESE 5	58.93
	55.32
	57.49
AVG	57.2

\*Values determined directly from data files not from figures.

Apparent outlier

# Application: Oscillatory Single Frequency Temperature Sweep – Butter Spreadability

- $G^* \propto$  stiffness
- Spreadable butter contains fats & oils that melt and more spreadable at lower temperatures.

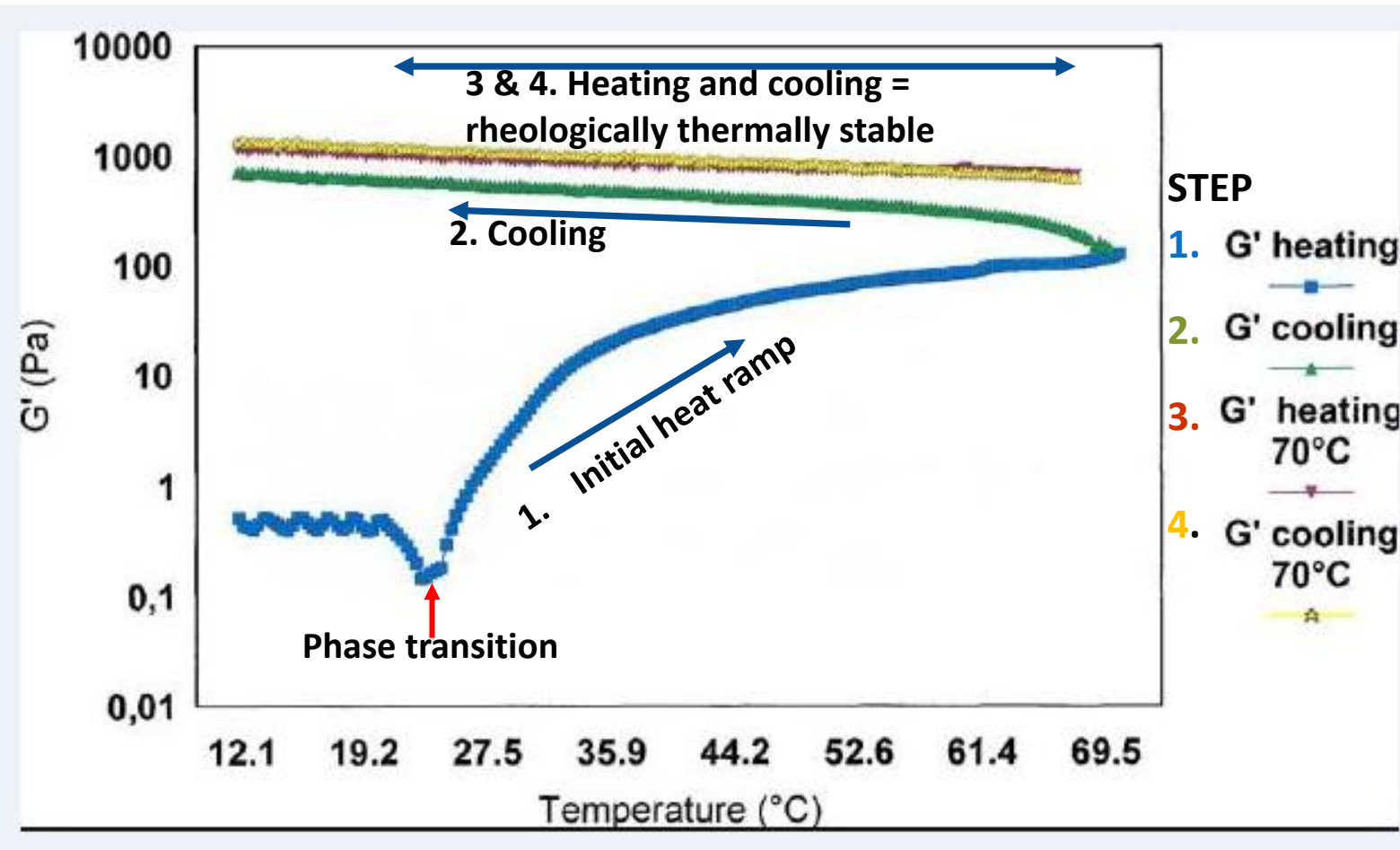




# TEMPERATURE SWEEP TO PROBE THERMAL (IR)REVERSIBILITY

- Can do in either rotational or oscillatory mode
- Probe properties with multiple temperature up/down ramps
- Important for manufacturing and low/high temperature exposure (winter/summer)

Example showing irreversible rheological change to more thermally stable material



# Switching gears to vertical assays

- Pull away
- Model chewing
- Surface tension

## Movements → torque

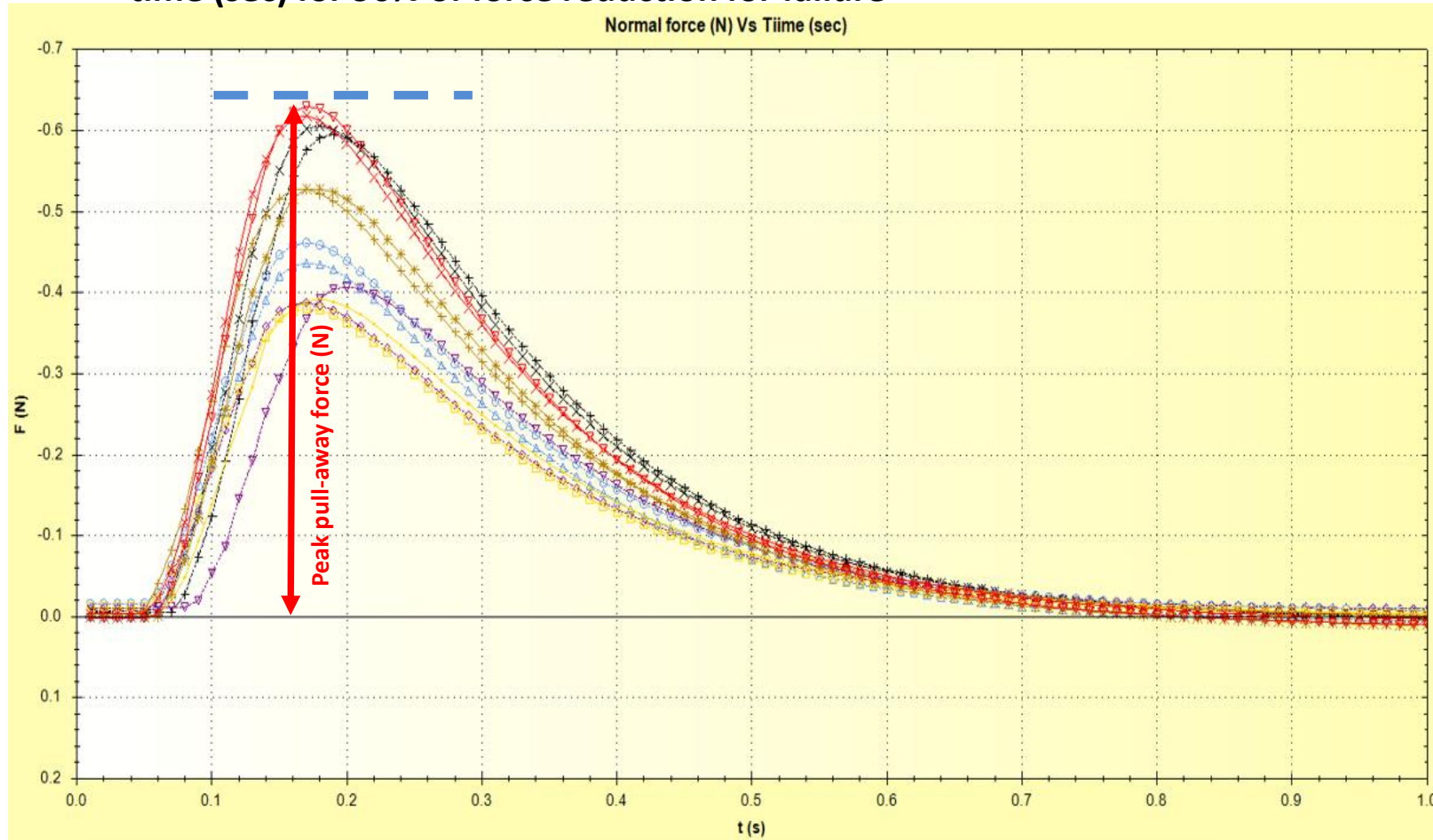
- Rotational (1 direction)
- Oscillational (bi-directional)
- **Vertical**



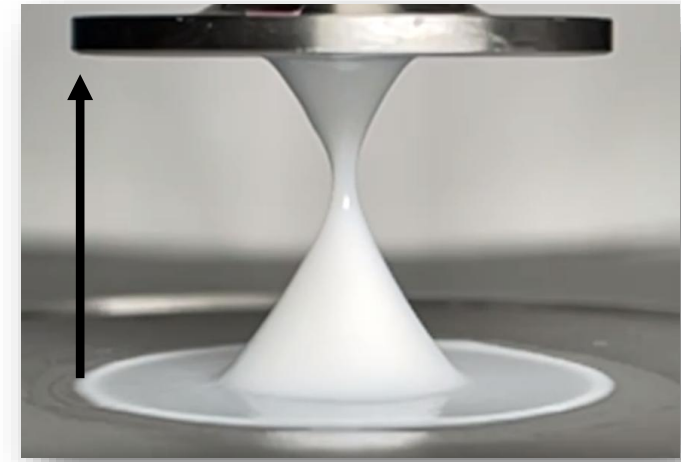
# Squeeze-Pull Away for Several Manufacturing Sources

Model adhesion/cohesion, stickiness, mastication (chewing)

- peak pull-away force (N; Newtons) for tack
- area under the curve (N-sec) for adhesion/cohesion strength
- time (sec) for 90% of force reduction for failure



Tack test method: ASTM D2979





# Application: Axial Testing to Quantify Texture with Heating- Chocolate

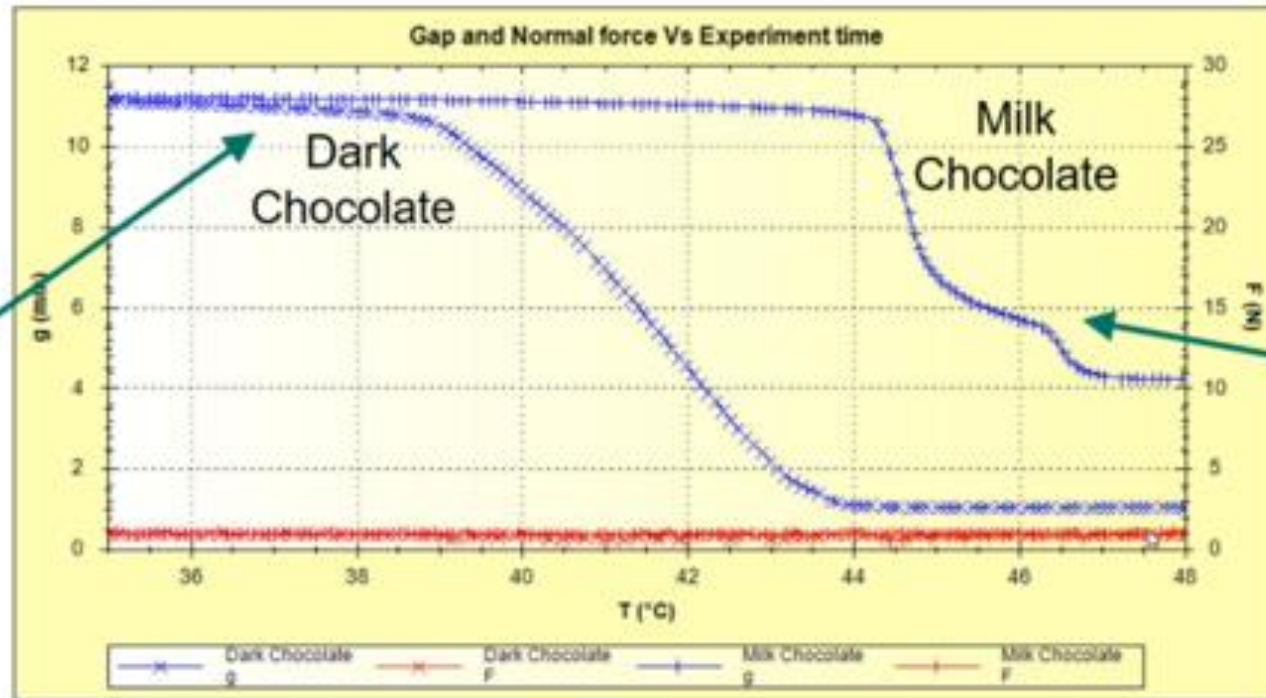
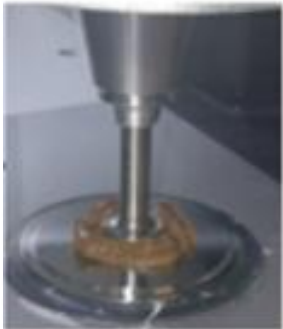
## Chocolate

### Rheometry Axial Testing Results

NETZSCH

- These relative tests allow for a close correlation, under more scientific control, of properties that we “feel” and know

Softening at 42°C



Still solid at 42°C



# Application: Squeeze-Pull Away Cycling to Model Chewing

Food Research International 49 (2012) 161–169



Contents lists available at SciVerse ScienceDirect

Food Research International

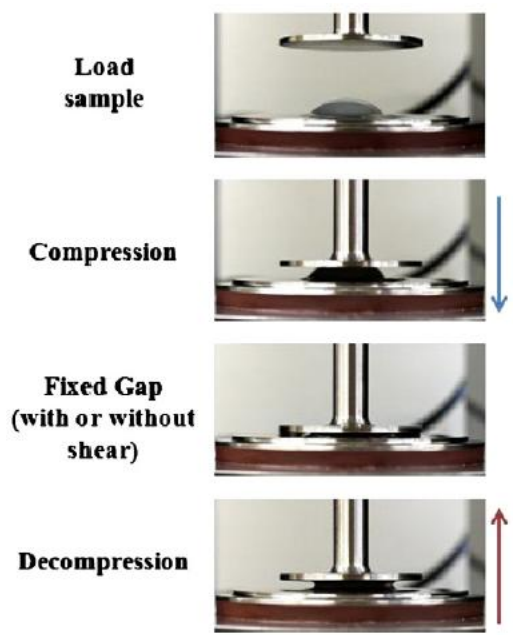
journal homepage: [www.elsevier.com/locate/foodres](http://www.elsevier.com/locate/foodres)



Instrumental mastication assay for texture assessment of semi-solid foods:  
Combined cyclic squeezing flow and shear viscometry

Cheryl Chung <sup>a</sup>, Brian Degner <sup>b</sup>, David Julian McClements <sup>a,\*</sup>

<sup>a</sup> Department of Food Science, University of Massachusetts, Amherst, MA 01003, United States  
<sup>b</sup> ConAgra Foods, Six ConAgra Drive, Omaha, NE 68102, United States

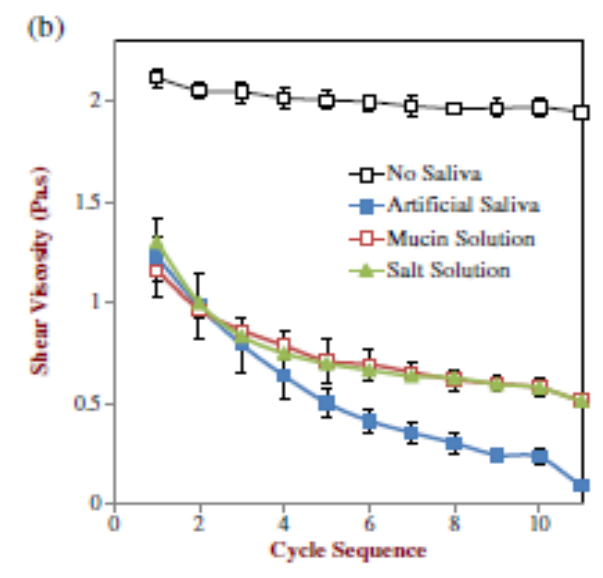
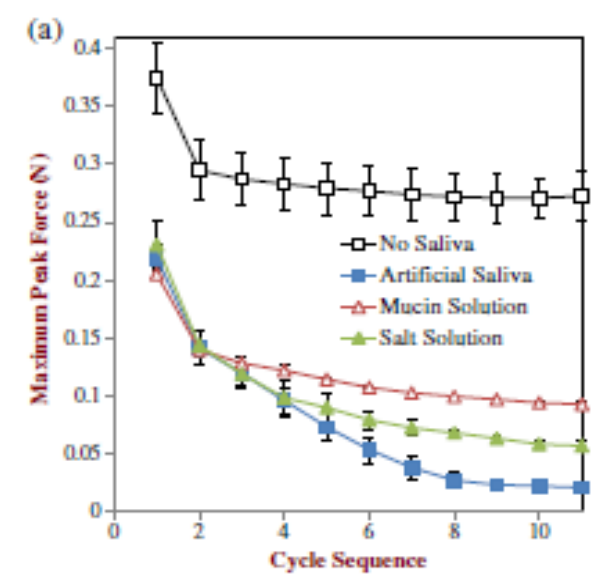
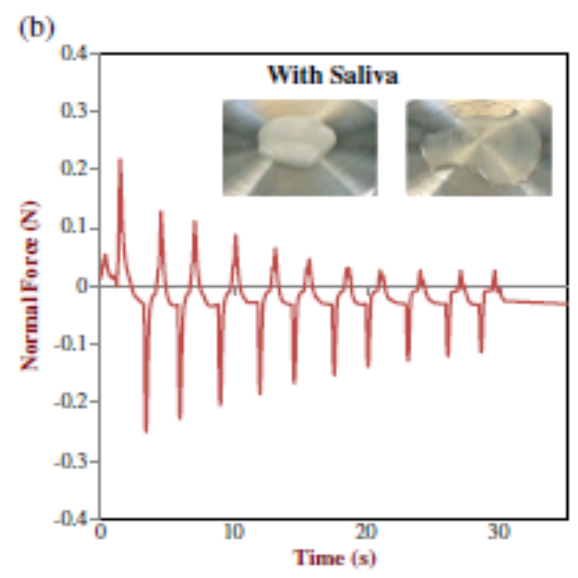
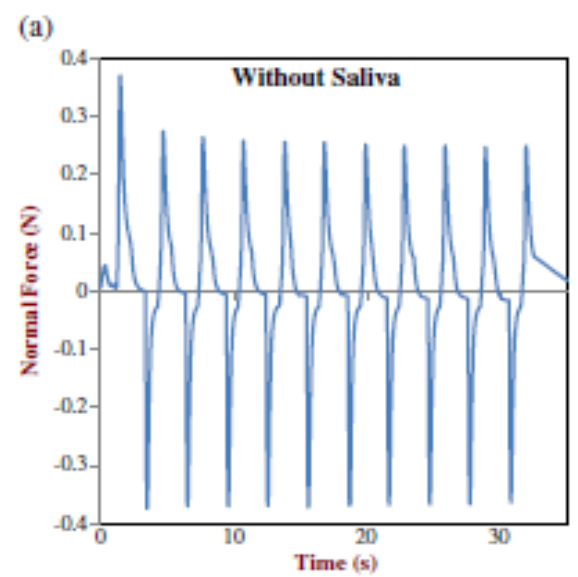


**Table 1**  
Chemical composition of artificial saliva (Mandel et al., 2010; Sarkar et al., 2009).

Chemical type	Concentration (g/L) or activity (units/mL)
Sodium chloride	1.594
Ammonium nitrate	0.328
Potassium phosphate	0.636
Potassium chloride	0.202
Potassium citrate	0.308
Uric acid sodium salt	0.021
Urea	0.198
Sodium $\alpha$ -lactate/lactic acid sodium salt	0.146
Mucin from porcine stomach, type II	30
Alpha amylase activity	93 units/mL

168

C. Chung et al. / Food Research International 49 (2012) 161–169



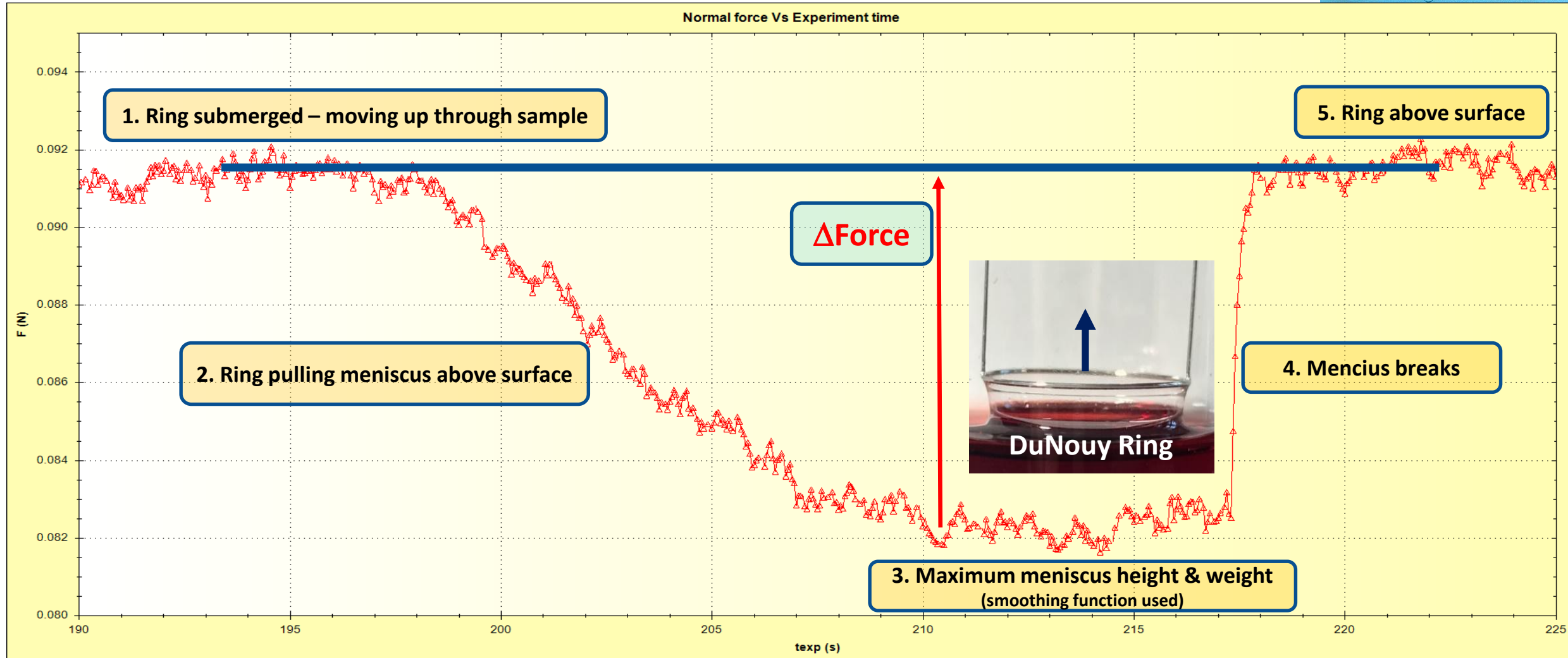


# Application: Interfacial surface tension (liquid-air, liquid-liquid)

- Applications in pharmaceutical, cosmetics, paint, food industries

- Surface Tension (milliNewton/meter) =  $\Delta\text{Force} \times \text{Ring factor}$

Ring factor is normalized to bracketing water standards 71.99mN/meter for assays at 25°C. Adjust for assays at other temperatures.



# Application: Interfacial surface tension (liquid-air, liquid-liquid)

- Applications in pharmaceutical, cosmetics, paint, food industries
- Surface Tension =  $\Delta\text{Force} \times \text{Ring factor}$

Ring factor is normalized to bracketing water standards 71.99mN/meter for assays at 25°C. Adjust for assays at other temperatures.

## Example Results

Sample Description	# Pulls	Average Surface Tension (milliNewton/meter)	%RSD
HPLC grade water START	12	71.99	5.3
1mg/mL SET 1	6	72.99	4.4
1mg/mL SET 2	6	72.90	3.6
HPLC grade water INTERIM 2	6	71.99	4.6
10mg/mL SET 1	6	63.84	3.4
10mg/mL SET 2	6	63.89	5.1
HPLC grade water END	6	71.99	1.8

# CONCLUSIONS

- ✓ Rheology is much more than viscosity!
- ✓ Many approaches to characterize materials. Depends on the questions to be answered.
- ✓ Viscosity will often decrease with increasing shear rate → shear thinning (non-Newtonian).  
→ Very important to report viscosity with associated shear rate.
- ✓ Regulatory considerations! Q3
- ✓ Numerous experimental considerations

## ⇒ ROTATION

- Shear stress ramp and stepwise: “Flow curve”. Model delivery, performance & processes.
- Shear rate ramp and stepwise: Compare products. Shear thinning profile.
- Thixotropy: Extent & rate of rebuild after shear thinning. Ketchup, paint, toothpaste
- Single shear rate or stress over time: Stability
- Temperature sweep: Change with temperature, model processes
- Creep-Recovery
- Tribology (friction, lubricity): motor oil, arthritis products

## ⇒ OSCILLATORY

- Amplitude sweep: Define LVER  $\propto$  breaking point  $\propto$  rheological stability. Critical input for frequency assays.
- Frequency sweep: Rheological fingerprint across frequency (1/time) domain. Silly putty example. Model arthritis products. Texture.
- Temperature sweep and cycling: Thermal (ir)reversibility, melting point. Cheese melting point, polymer disc examples.

## ⇒ VERTICAL

- Squeeze - Pull Away: stickiness, model chewing, texture
- Surface Tension



# Backup Slides

## Plate & Cone Considerations

Geometry Size	Advantages	Disadvantages
Larger surface area	-Use for lower viscosity samples	-Requires more sample
Smaller surface area	-Use for higher viscosity samples -Requires less sample	-May not provide adequate response since less sample area

Geometry Surface	Advantages	Disadvantages
Smooth	-Easy to clean	-May give slippage
Roughened	-Easy to clean -May reduce potential for slippage	-May still give slippage
Serrated	-Most aggressive to reduce slippage	-May need brush to clean -May “gouge” sample surface

Geometry Type	Advantages	Disadvantages
Flat (parallel)	-Good for high viscosity fluids	-Variable shear rate across radius. Sample may yield at edge before center.
Cone (2 & 4°)	-Good for low viscosity fluids -Constant shear rate in gap	Don't use for temperature sweeps unless rheometer compensates for thermal expansion



# Optimizing Dispersion, Colloidal and Emulsion Stability

(dispersed phase <1mm)

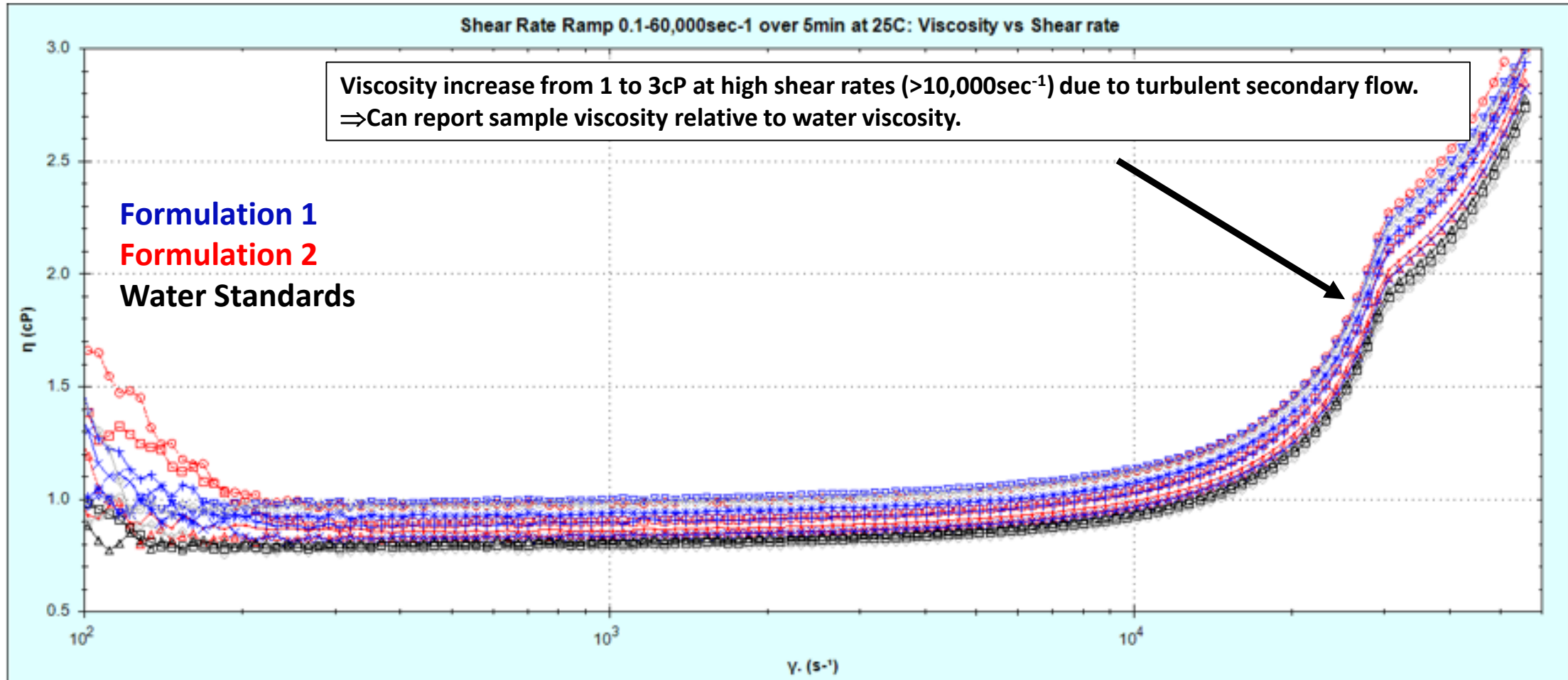
Property	To Improve Stability	How
Zero Shear Viscosity ( $\eta_0$ )	↑	Add thickeners to prevent particles from settling
Yield Stress	↑	Provides high resistance to sedimentation.
Thixotropy	↓	Decrease rebuild time to near pre-shear value
Cohesive Energy	↑	Determine with strain controlled amplitude sweep ( $CE = 1/2G' \times \gamma^2$ )
Viscoelasticity	↓ $\delta$	-Viscoelastic liquids with high phase angle ( $\delta$ ) at low freq are less stable -Use structured gel having $\delta < 45^\circ$ and independent of freq -If heavy or large particles, decrease $\delta < 45^\circ$ at low freq

- Larger particles increase viscosity
- Irregular particles increase viscosity

<https://www.azom.com/article.aspx?ArticleID=11442>

# Shear Rate Ramp: Low viscosity formulations with high shear rate

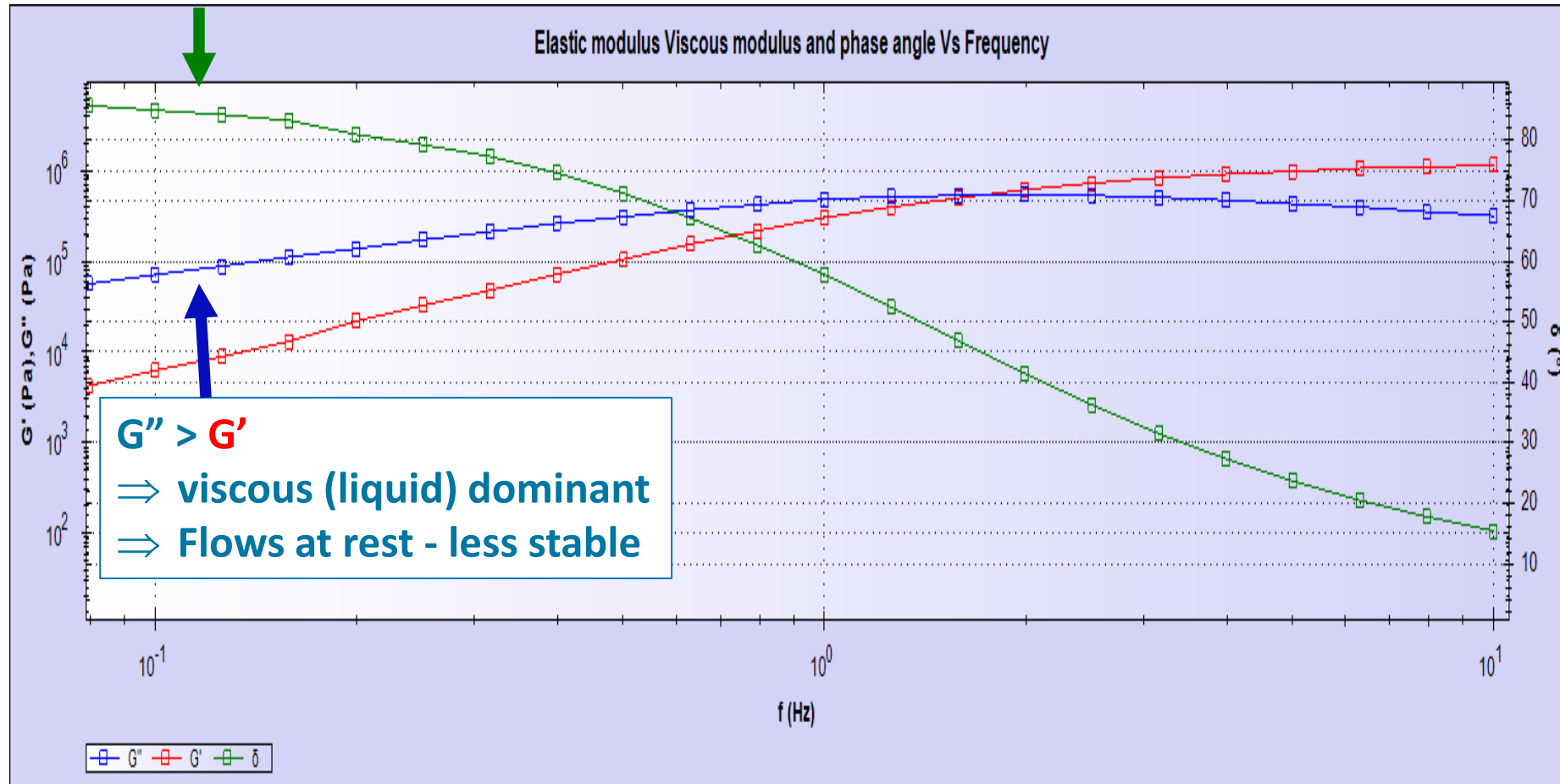
- Experimental: 40mm smooth parallel plate, 100uL gap\* (130uL sample), 25°C, 0.1-60,000sec<sup>-1</sup> over 5min



\* Small gap (100um) is required to retain sample within plates at high shear. Human hair is 70+/-20um.

# Is Silly Putty a viscoelastic solid or liquid at rest?

phase angle starts  $>45^\circ$   
 $\Rightarrow$  liquid dominant



# PROCESSING OF A PROTEIN-STABILIZED EMULSION

## Influence of Processing Variables on Rheological & Textural Properties of Lupin

### Protein-Stabilized Emulsions

J. M. Franco, A. Raymundo, I. Sousa, and C. Gallegos J. Agric. Food Chem. 1998, 46, 3109–3115



### PURPOSE

- Mayonnaise and salad dressing-type emulsions are stabilized by an adsorbed layer of protein at the oil-water interface.
- Previous studies show poorer gelation and thickening properties of lupin protein compared to commercially used soy protein.

### EXPERIMENTAL (rheology only)

- **Steady-state flow curves (rotational):** Serrated plate (20 mm) to prevent wall-slip.
- **Frequency Sweep (oscillational):** Within LVER, using a cone/plate (35 mm, 2°) across 0.05-200 rad/s (0.01-31.8Hz).

### CONCLUSION:

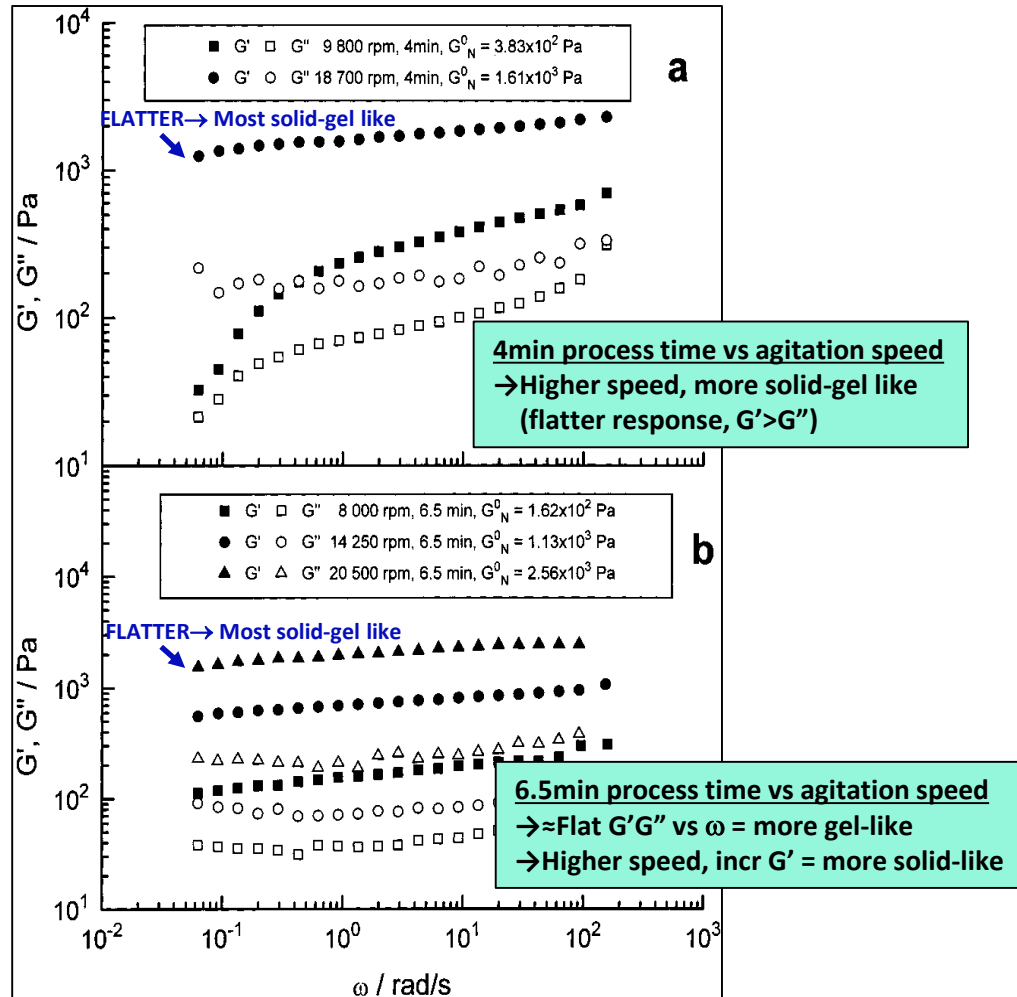
- Emulsion stability and physical properties improved by heating lupin solution prior to the addition of the oil phase or inducing a chemical or enzymatic reaction that increases the entanglement protein molecules along with hydrophobicity.
- Processing variables (temp, time, impeller/stir type & speed) affect viscous and viscoelastic behavior by droplet size distribution, interdroplet interactions and entanglement.

# PROCESSING OF A PROTEIN-STABILIZED EMULSION

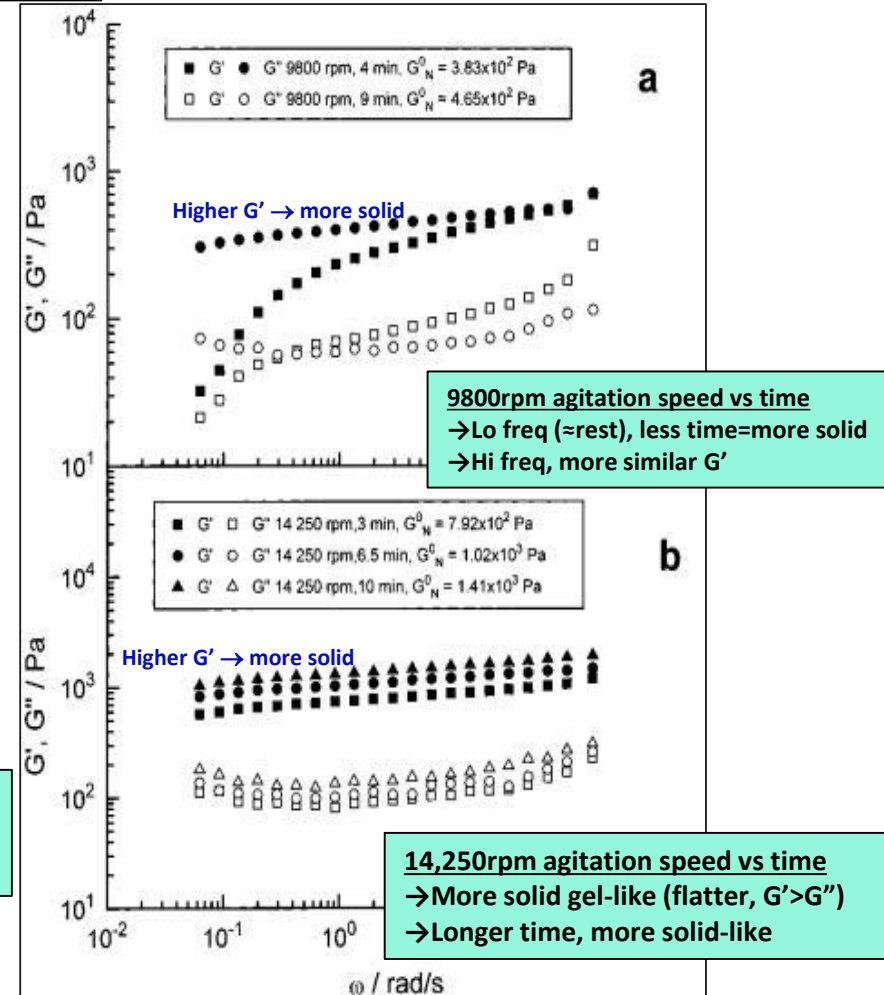
## Influence of Processing Variables on Rheological & Textural Properties of Lupin Protein-Stabilized Emulsions

J. M. Franco, A. Raymundo, I. Sousa, and C. Gallegos

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**Freq Sweep:**  $G'$  and  $G''$  of lupin protein-stabilized emulsions vs agitation speeds.



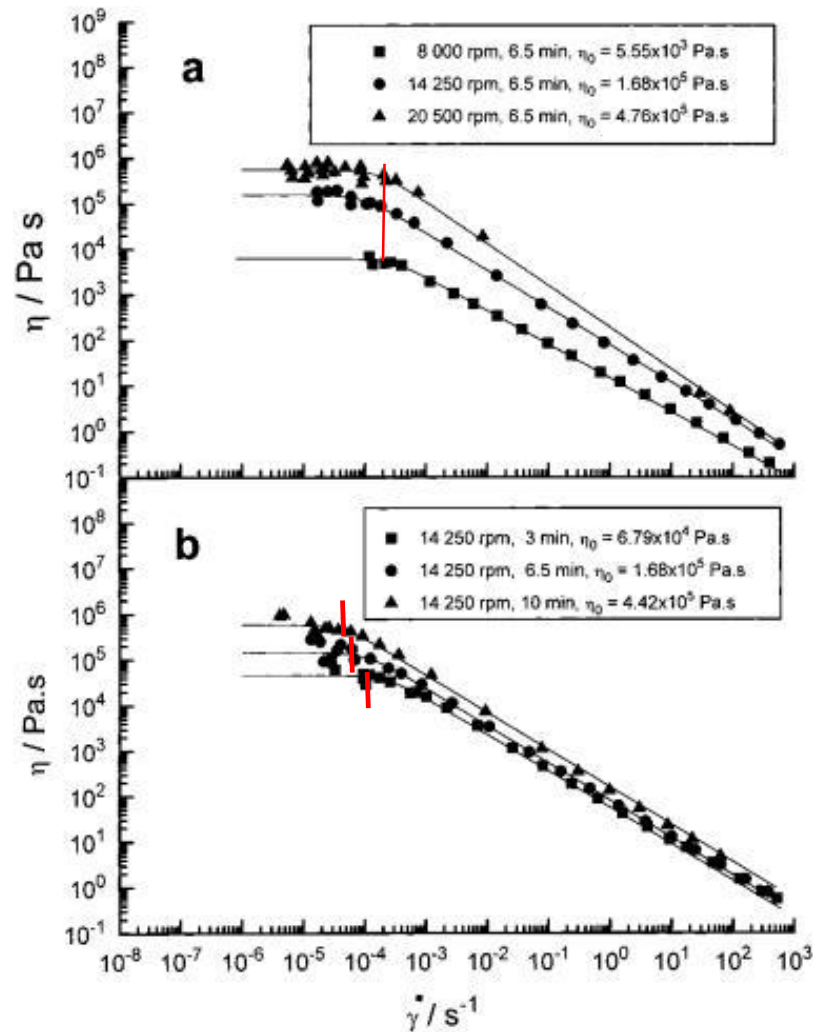
**Freq Sweep:**  $G'$  and  $G''$  for lupin protein-stabilized emulsions prepared vs emulsification times



# PROCESSING OF A PROTEIN-STABILIZED EMULSION (con't)

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## 6.5min process time vs agitation speed

→ Higher speed, more viscous

→ All shear thin, with 20,500rpm more rapidly

→ Generally, similar breakpoint

## Agitation speed (14,250rpm) vs time

→ Longer time, more viscous

→ Shorter time, later breakpoint

**Steady-state flow curves:** (a) agitation speed and (b) emulsification time for lupin protein stabilized emulsions.